

Company Name -

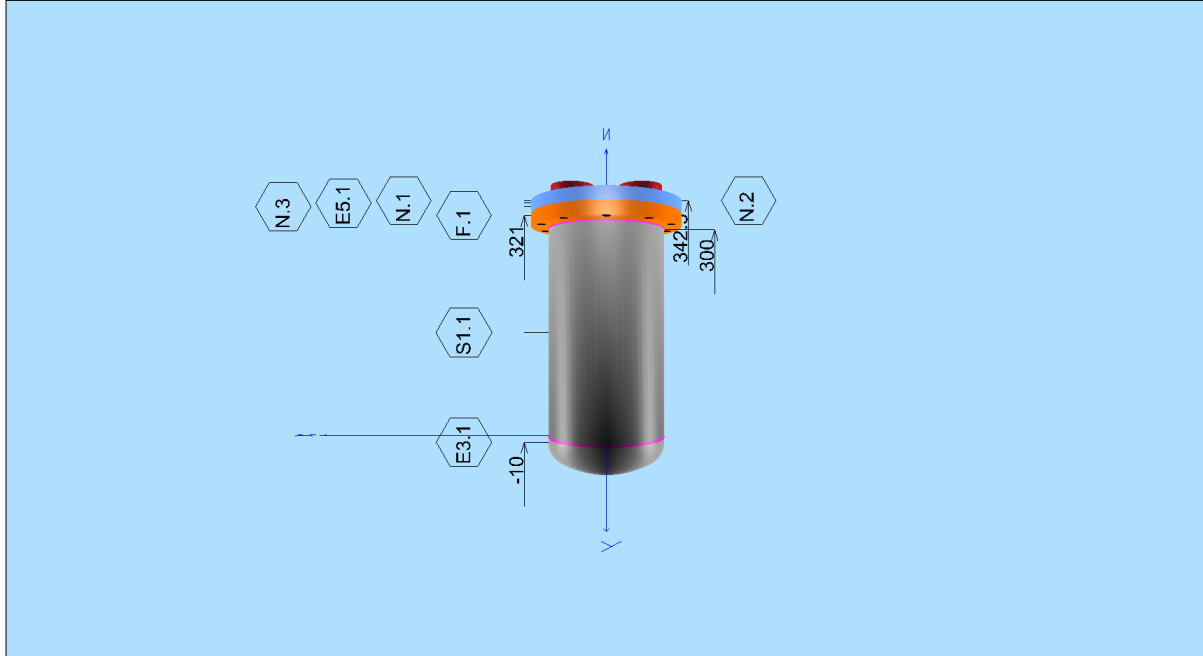
Client :GÜVEN SOGUTMA

Vessel Tag No.:OS.F.33B.54.1

Visual Vessel Design by Hexagon PPM,Ver:20.0 Operator : Rev.:A

(0) Drawing

3D View of Vessel (alter by using the Save User Specified View command)



Design Data & Process Information

Description	Units	Design Data
Process Card		General Design Data
Design Code & Specifications		EN13445 TG = 3b
Internal Design Pressure (MPa)	MPa	3.3
External Design Pressure (MPa)	MPa	
Hydrotest Pressure (MPa)	MPa	
Maximum Design Temperature (°C)	°C	130
Minimum Design Temperature (°C)	°C	-20
Operating Temperature (°C)	°C	
Corrosion Allowance (mm)	mm	0
Content of Vessel		
Specific Density of Oper.Liq		
Normal Liquid Level NLL (mm)	mm	

Test Pressure

TEST PRESSURE OF VESSEL - NEW & COLD - VERTICAL

Design Pressure..... : 3.300 MPa

Design Temperature..... : 130.0 C

ID	Description	Pdesign	PtMax	PtMin	Wat.Head	PtTop	PtTopMax
E3.1	Torispherical End-End	3.300	6.710	4.386	0.004	4.386	6.706
E5.1	Bolted Flat End-Cover Flange	3.300	8.405	4.187	0.000	4.187	8.405
F.1	RT - Flange-Shell Flange	3.300	5.887	4.187	0.001	4.187	5.886
N.1	Nozzle,Seamless Pipe-Inlet	3.300	6.511	NA	0.000	NA	6.511
N.2	Nozzle,Seamless Pipe-Outlet	3.300	6.511	NA	0.000	NA	6.511
N.3	Nozzle,Seamless Pipe-Sae 3/8"	3.300	7.617	NA	0.000	NA	7.617
S1.1	Cylindrical Shell-Shell	3.300	10.012	4.297	0.004	4.297	10.009

PtReq = MAX(MIN(PtTop), 1.43*p) = 4.7190 MPa (EN13445-5, 10.2.3.3.1-1 & 2)

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HYDRO-TEST

REQUIRED TEST PRESSURE AT TOP OF VESSEL PtReq(Hydro Test): 4.7190 MPa
MAXIMUM TEST PRESSURE AT TOP OF VESSEL PtLim(Hydro Test): 5.8864 MPa

PNEUMATIC TEST

REQUIRED TEST PRESSURE AT TOP OF VESSEL PtReq(Pneumatic Test) ...: 4.7190 MPa
MAXIMUM TEST PRESSURE AT TOP OF VESSEL PtLim(Pneumatic Test) ...: 5.8870 MPa

Note : Other components may limit Ptlim than the ones checked above.

TEST PRESSURE OF VESSEL - NEW & COLD - HORIZONTAL

Design Pressure.....: 3.300 MPa

Design Temperature.....: 130.0 C

ID	Description	Pdesign	PtMax	PtMin	Wat.Head	PtTop	PtTopMax
E3.1	Torispherical End-End	3.300	6.710	4.386	0.001	4.386	6.709
E5.1	Bolted Flat End-Cover Flange	3.300	8.405	4.187	0.002	4.187	8.403
F.1	RT - Flange-Shell Flange	3.300	5.887	4.187	0.002	4.187	5.885
N.1	Nozzle,Seamless Pipe-Inlet	3.300	6.511	NA	0.001	NA	6.511
N.2	Nozzle,Seamless Pipe-Outlet	3.300	6.511	NA	0.002	NA	6.510
N.3	Nozzle,Seamless Pipe-Sae 3/8"	3.300	7.617	NA	0.002	NA	7.616
S1.1	Cylindrical Shell-Shell	3.300	10.012	4.297	0.002	4.297	10.010

PtReq = MAX(MIN(PtTop), 1.43*p)= 4.7190 MPa (EN13445-5, 10.2.3.3.1-1 & 2)

HYDRO-TEST

REQUIRED TEST PRESSURE AT TOP OF VESSEL PtReq(Hydro Test): 4.7190 MPa
MAXIMUM TEST PRESSURE AT TOP OF VESSEL PtLim(Hydro Test): 5.8849 MPa

PNEUMATIC TEST

REQUIRED TEST PRESSURE AT TOP OF VESSEL PtReq(Pneumatic Test) ...: 4.7190 MPa
MAXIMUM TEST PRESSURE AT TOP OF VESSEL PtLim(Pneumatic Test) ...: 5.8870 MPa

Note : Other components may limit Ptlim than the ones checked above.

NOMENCLATURE:

Pdesign- is the design pressure including liquid head at the part under consideration.

PtMax - is the maximum allowed test pressure determined at the part under consideration.

PtMin - is the required test pressure determined at the part under consideration.

Wat.Head - is the water head during hydrotesting at the part under consideration.

PtBot - is the required test pressure at bottom of the vessel, for the part under consideration.

PtTop - is the required test pressure at top of the vessel, for the part under consideration.

PtTopMax - is the maximum test pressure allowed at top of the vessel, for the part under consideration.

PtReq - is the required minimum test pressure (minimum value of PtTop) at top of vessel for the listed components.

PtLim - is the maximum allowed test pressure (minimum value for PtTopMax) at top of vessel for the listed components.

EN13445-5 10.2.3.3.8 Pressure of vessels under test shall be gradually increased to a value of approximately 50 % of the specified test pressure, thereafter the pressure shall be increased in stages of approximately 10 % of the specified test pressure until this is reached. The required test pressure shall be maintained for not less than 30 min. At no stage shall the vessel be approached for close examination until the pressure has been positively reduced by at least 10 % to a level lower than that previously attained. The pressure shall be maintained at the specified close examination level for a sufficient length of time to permit a visual inspection to be made of all surfaces and joints.

Utilization Chart

Utilization Chart

Company Name -

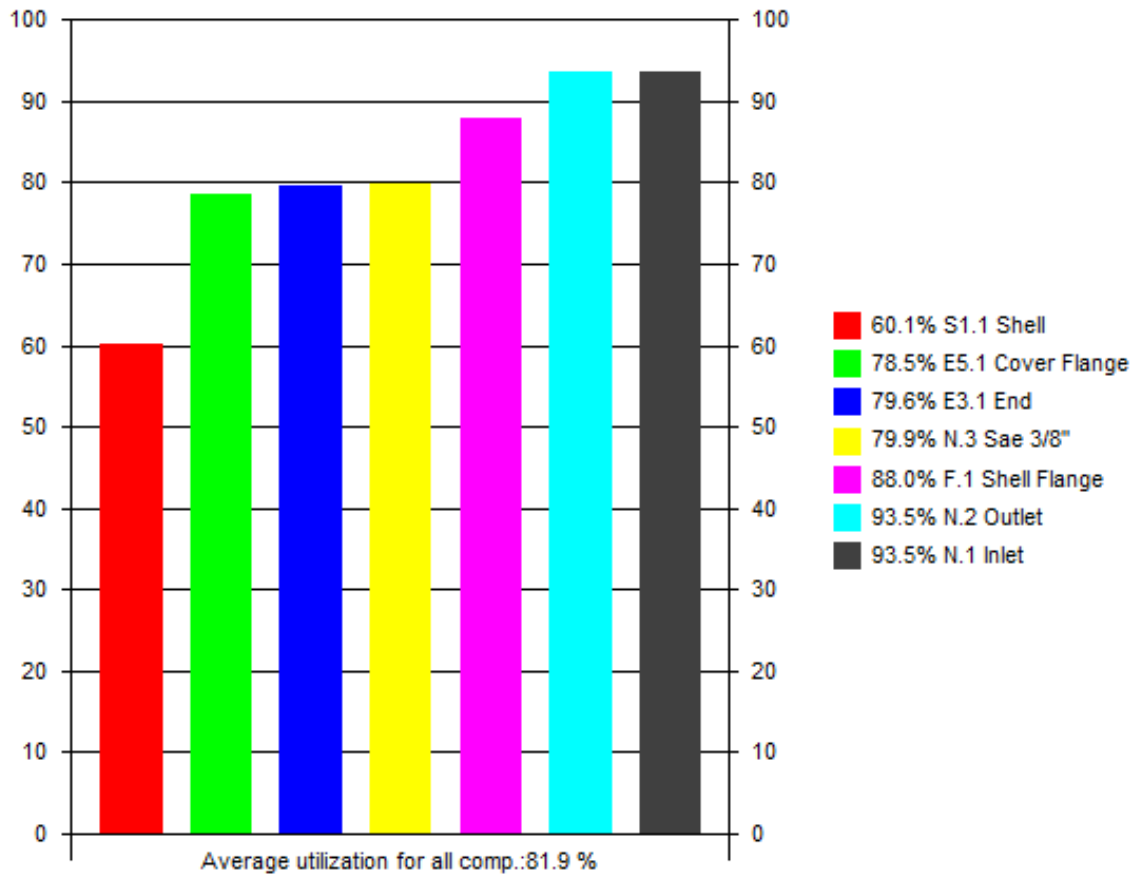
Client :GÜVEN SOGUTMA

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Visual Vessel Design by Hexagon PPM,Ver:20.0 Operator :

Rev.:A

COMPONENTS UTILIZATION CHART - Client :GÜVEN SOGUTMA Vessel Tag No.:OS.F.33B.54



Maximum Utilization of 93.5% for Component N.2 Outlet - VVD by Hexagon PPM, Ver:20.0

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Vessel Tag No.:OS.F.33B.54.1

Visual Vessel Design by Hexagon AB,Ver:19.0- Operator : Rev.:A

EN13445:2014 Issue 5:2018+A5 - 7.4.2 CYLINDRICAL SHELL

S1.1 Shell

19 Feb. 2020 17:25

INPUT DATA

COMPONENT ATTACHMENT/LOCATION

GENERAL DESIGN DATA

PRESSURE LOADING: Design Component for Internal Pressure Only

PROCESS CARD:

General Design Data : Temp= 100°C, P=3.3000 MPa, c=0.0 mm, Pext=0.0000 MPa

SPECIFIC DENSITY OF OPERATING LIQUID.....:SG 0.00

LIQUID HEAD.....:LH 0.00 mm

SHELL DATA

CYLINDER FABRICATION: Welded Pipe

WELD JOINT COEFFICIENT: Testing Group 1 (z=1.0)

NEGATIVE TOLERANCE: Negative tolerance specified in mm

EN 10216-3:2013, 1.0565 P355NH seamless tube, HT:N THK<=50mm 100'C

Rm=490 Rp=335 Rpt=294 f=196 f20=204.17 ftest=319.05 E=206067(N/mm²) ro=7.85

OUTSIDE DIAMETER OF SHELL.....:De 168.30 mm

LENGTH OF CYLINDRICAL PART OF SHELL.....:Lcyl 300.00 mm

NOMINAL WALL THICKNESS (uncorroded).....:en 3.0000 mm

NEGATIVE TOLERANCE/THINNING ALLOWANCE.....:th 0.4000 mm

Split shell into several shell courses and include welding information: NO

WELDING REQUIREMENTS TO EN 1708-1:2010

Comment(Optional):

Type of welded connection: Not Applicable

CALCULATION DATA

7.4.2 - CYLINDRICAL SHELLS UNDER INTERNAL PRESSURE

Required Minimum Shell Thickness Excl.Allow. emin :

$$emin = De * P / (2 * f * z + P) \quad (7.4-2)$$
$$=168.3*3.3/(2*196*1+3.3)= \underline{1.4050 \text{ mm}}$$

Required Minimum Shell Thickness Incl.Allow. :

$$emina = emin + c + NegDev =1.4+0+0.4= \underline{\underline{1.8050 \text{ mm}}}$$

Analysis Thickness

$$ea = en - c - NegDev =3-0-0.4= \underline{\underline{2.6000 \text{ mm}}}$$

»7.4.1 Cond.of Applicability $emin/De=0.0083 \leq 0.16$ « » OK«

Internal Pressure $emina=1.8 \leq en=3$ [mm]	60.1%	OK
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MAXIMUM ALLOWABLE WORKING PRESSURE MAWP :

Inside Diameter of Shell

$$Di = De - 2 * ea =168.3-2*2.6= 163.10 \text{ mm}$$

Mean Diameter of Shell

$$Dm = (De + Di) / 2 =(168.3+163.1)/2= 165.70 \text{ mm}$$

MAWP HOT & CORR. (Corroded condition at design temp.)

$$MAWPHC = 2 * f * z * ea / Dm =2*196*1*2.6/165.7= \underline{\underline{6.1509 \text{ MPa}}}$$

MAWP NEW & COLD (Uncorroded condition at ambient temp.)

$$MAWPNC = 2 * f20 * z * (ea + c) / Dm$$
$$=2*204.17*1*(2.6+0)/165.7= \underline{\underline{6.4073 \text{ MPa}}}$$

MAX TEST PRESSURE (Uncorroded cond.at ambient temp.)

Ptmax = 2 * ftest * ztest * (ea + c) / Dm

$$=2*319.05*1*(2.6+0)/165.7= \underline{\underline{10.01 \text{ MPa}}}$$

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EN13445:2014 Issue 5:2018+A5 - 7.4.2 CYLINDRICAL SHELL

S1.1 Shell 19 Feb. 2020 17:25

EN13445-5;10.2.3.3 REQUIRED MIN.HYDROSTATIC TEST PRESSURE:Ptmin

NEW AT AMBIENT TEMP. FOR TEST GROUPS 1, 2 and 3

$$Ptmin = 1.25 * Pd * f_{20} / f = 1.25 * 3.3 * 204.17 / 196 = 4.2969 \text{ MPa}$$

$$Ptmin = 1.43 * Pd = 1.43 * 3.3 = 4.7190 \text{ MPa}$$

Test Pressure Ptmin=4.72 <= Pmax=10.01[MPa]	47.1%	OK
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MAXIMUM DIAMETER OF UNREINFORCED OPENING IN SHELL

Inside Radius of Shell

$$ris = Di / 2 \text{ (9.5-3)} = 163.1 / 2 = 81.55 \text{ mm}$$

Length of Shell Contributing to Reinforcement

$$Is = \text{Sqr}((2 * ris + ea) * ea) \text{ (9.5-2)}$$

$$= \text{Sqr}((2 * 81.55 + 2.6) * 2.6) = 20.76 \text{ mm}$$

Maximum Diameter of Unreinforced Opening in Shell Checked to Rules in Section 9

$$dmax1 = \text{MIN}(0.5 * Di, (ea * Is * (f - 0.5 * P) / P - ris * Is) / (0.5 * ris + 0.5 * ea)) \text{ (9.5-7,22,23)}$$

$$= \text{MIN}(0.5 * 163.1, (2.6 * 20.76 * (196 - 0.5 * 3.3) / 3.3 - 81.55 * 20.76) / (0.5 * 81.55 + 0.5 * 2.6)) = 35.31 \text{ mm}$$

Maximum diameter of Opening Not Requiring Reinforcement Check

$$dmax2 = 0.15 * \text{Sqr}((2 * ris + ea) * ea) \text{ (9.5-18)}$$

$$= 0.15 * \text{Sqr}((2 * 81.55 + 2.6) * 2.6) = 3.1134 \text{ mm}$$

Maximum Diameter of Unreinforced Opening

$$dmax = \text{MAX}(dmax1, dmax2) = \text{MAX}(35.31, 3.11) = 35.31 \text{ mm}$$

CALCULATION SUMMARY**7.4.2 - CYLINDRICAL SHELLS UNDER INTERNAL PRESSURE**

Required Minimum Shell Thickness Excl.Allow. emin :

$$emin = De * P / (2 * f * z + P) \text{ (7.4-2)}$$

$$= 168.3 * 3.3 / (2 * 196 * 1 + 3.3) = 1.4050 \text{ mm}$$

Required Minimum Shell Thickness Incl.Allow. :

$$emina = emin + c + \text{NegDev} = 1.4 + 0 + 0.4 = 1.8050 \text{ mm}$$

Internal Pressure emina=1.8 <= en=3[mm]	60.1%	OK
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MAX TEST PRESSURE (Uncorroded cond.at ambient temp.)

$$Ptmax = 2 * f_{test} * z_{test} * (ea + c) / Dm$$

$$= 2 * 319.05 * 1 * (2.6 + 0) / 165.7 = 10.01 \text{ MPa}$$

EN13445-5;10.2.3.3 REQUIRED MIN.HYDROSTATIC TEST PRESSURE:Ptmin

NEW AT AMBIENT TEMP. FOR TEST GROUPS 1, 2 and 3

$$Ptmin = 1.25 * Pd * f_{20} / f = 1.25 * 3.3 * 204.17 / 196 = 4.2969 \text{ MPa}$$

$$Ptmin = 1.43 * Pd = 1.43 * 3.3 = 4.7190 \text{ MPa}$$

Test Pressure Ptmin=4.72 <= Pmax=10.01[MPa]	47.1%	OK
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MAXIMUM DIAMETER OF UNREINFORCED OPENING IN SHELL

Maximum Diameter of Unreinforced Opening

$$dmax = \text{MAX}(dmax1, dmax2) = \text{MAX}(35.31, 3.11) = 35.31 \text{ mm}$$

Volume:0.0063 m3 Weight:3.7 kg (SG= 7.85)

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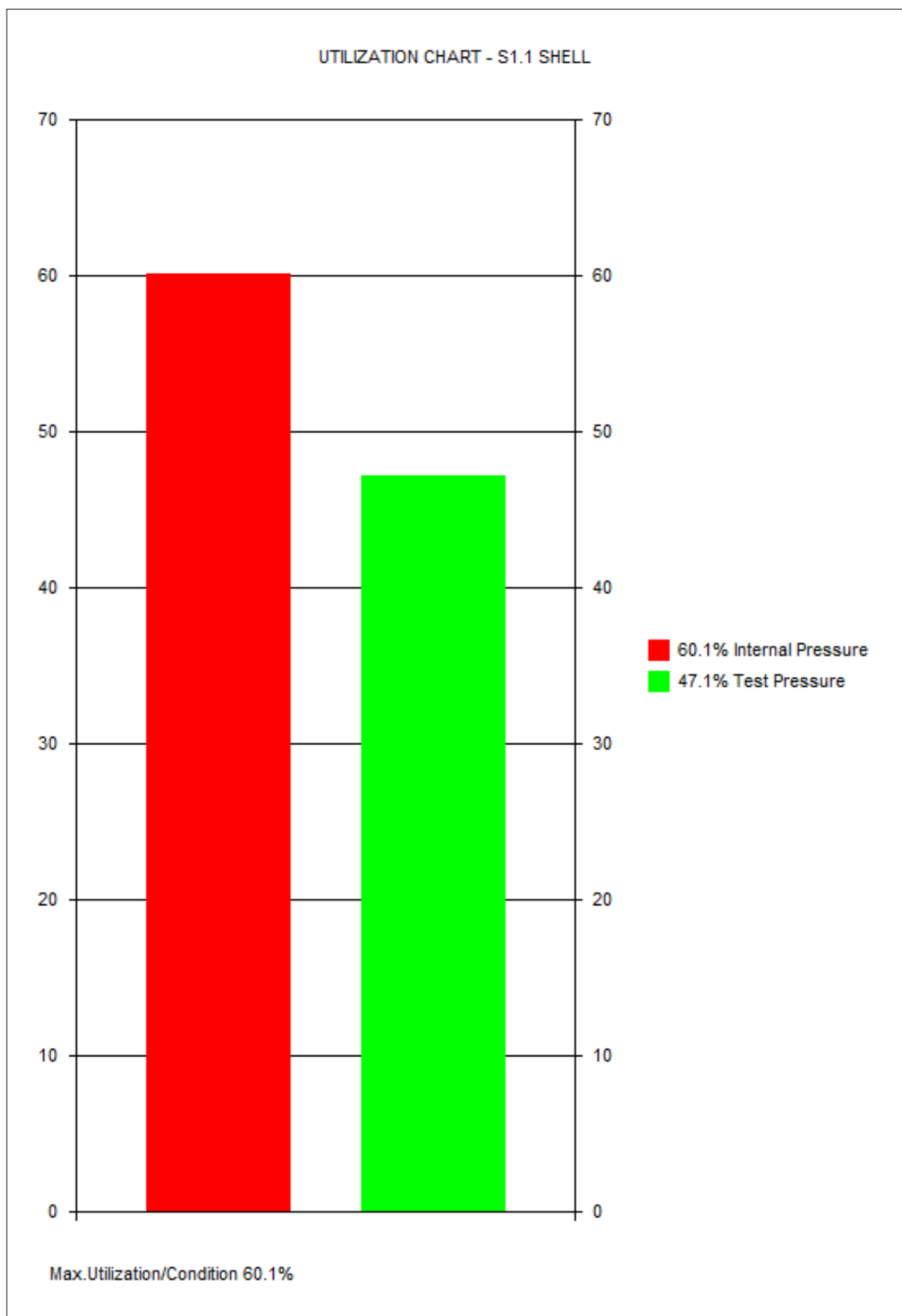
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EN13445:2014 Issue 5:2018+A5 - 7.4.2 CYLINDRICAL SHELL

S1.1 Shell

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Visual Vessel Design by Hexagon AB,Ver:19.0- Operator : Rev.:A

EN13445:2014 Issue 5:2018+A5 - 7.5 DOMED ENDS

E3.1 End 19 Feb. 2020 17:26 ConnID:S1.1

INPUT DATA

COMPONENT ATTACHMENT/LOCATION

Attachment: S1.1 Cylindrical Shell Shell
Location: Along z-axis zo= 0

GENERAL DESIGN DATA

PRESSURE LOADING: Design Component for Internal Pressure Only

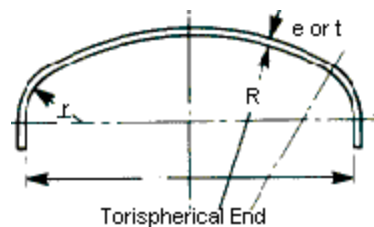
PROCESS CARD:

General Design Data : Temp= 100°C, P=3.3000 MPa, c=0.0 mm, Pext=0.0000 MPa

SPECIFIC DENSITY OF OPERATING LIQUID.....:SG 0.00

LIQUID HEAD.....:LH 0.00 mm

DIMENSIONS OF END



Type of Torispherical End: Dished End KORBOGEN DIN 28013-28014/SMS 482

WELD JOINT COEFFICIENT: Unwelded Component(z=1.0)

OUTSIDE DIAMETER OF CYLINDRICAL FLANGE OF END.....:De 168.30 mm

LENGTH OF CYLINDRICAL FLANGE OF END.....:Lcyl 10.00 mm

NEGATIVE TOLERANCE/THINNING ALLOWANCE.....:th 0.3000 mm

NOMINAL THICKNESS OF HEAD/END (uncorroded).....:en 2.5000 mm

Include calculation of forming during fabrication to EN13445-4 Section 9.: NO

MATERIAL DATA FOR END

EN 10028-2:2017, 1.0425 P265GH plate and strip, HT:N THK<=16mm 100'C

Rm=410 Rp=265 Rpt=241 f=160.67 f20=170.83 ftest=252.38 E=206067(N/mm2) ro=7.85

Material & Delivery Form: Cold Spun Seamless Austenitic Stainless Steel

NOZZLES IN KNUCKLE REGION TO SECTION 7.7

Nozzles In Knuckle Region: NO

WELDING REQUIREMENTS TO EN 1708-1:2010

Comment(Optional):

Type of welded connection: Not Applicable

CALCULATION DATA

7.5.3 - TORISPHERICAL ENDS UNDER INTERNAL PRESSURE

7.5.3.2 Required Minimum End Thickness

Required Thickness of End to Limit Membrane Stress in Central Part

$$e_s = P * R / (2 * f * z - 0.5 * P) \quad (7.5-1)$$

$$= 3.3 * 134.64 / (2 * 160.67 * 1 - 0.5 * 3.3) = 1.3898 \text{ mm}$$

$$f_b = R_{pt} / 1.5 * 1.6 \quad (7.5-5) = 241 / 1.5 * 1.6 = 257.07 \text{ N/mm}^2$$

Required Thickness of Knuckle to Avoid Plastic Buckling

$$e_b = (0.75 * R + 0.2 * D_i) * ((P / (111 * f_b)) * (D_i / r)^{0.825})^{(0.667)} \quad (7.5-3)$$

$$= (0.75 * 134.64 + 0.2 * 163.3) * ((3.3 / (111 * 257.07)) * (163.3 / 25.92)^{0.825})^{(0.667)}$$
$$= 0.8708 \text{ mm}$$

7.5.3.5 Formulas for Calculation of Factor Beta

$$Y = \text{MIN}(e_{min} / R, 0.04) \quad (7.5-9) = \text{MIN}(1.68 / 134.64, 0.04) = 0.0125$$

$$Z = \text{LOG}(1 / Y) \quad (7.5-10) = \text{LOG}(1 / 0.0125) = 1.9031$$

$$X = r / D_i \quad (7.5-11) = 25.92 / 164.93 = 0.1571$$

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$$N = 1.006 - 1 / (6.2 + (90 * Y) ^ 4) \quad (7.5-12)$$

$$= 1.006 - 1 / (6.2 + (90 * 0.0125) ^ 4) = 0.8778$$

$$\text{Beta01} = N * (-0.1833 * Z^3 + 1.0383 * Z^2 - 1.2943 * Z + 0.837) \quad (7.5-15)$$

$$= 0.8778 * (-0.1833 * 1.9^3 + 1.0383 * 1.9^2 - 1.2943 * 1.9 + 0.837) = 0.7645$$

$$\text{Beta02} = \text{MAX}(0.5, 0.95 * (0.56 - 1.94 * Y - 82.5 * Y ^ 2)) \quad (7.5-17)$$

$$= \text{MAX}(0.5, 0.95 * (0.56 - 1.94 * 0.0125 - 82.5 * 0.0125^2)) = 0.5000$$

$$\text{beta} = 10 * ((0.2 - X) * \text{Beta01} + (X - 0.1) * \text{Beta02}) \quad (7.5-16)$$

$$= 10 * ((0.2 - 0.1571) * 0.7645 + (0.1571 - 0.1) * 0.5) = 0.6134$$

Required Thickness of Knuckle to Avoid Axisymmetric Yielding

$$e_y = \text{beta} * P * (0.75 * R + 0.2 * D_i) / f \quad (7.5-2)$$

$$= 0.6134 * 3.3 * (0.75 * 134.64 + 0.2 * 164.93) / 160.67 = 1.6877 \text{ mm}$$

NOTE 3, since $e_y(1.7) > 0.005 * D_i(0.8)$ it is NOT necessary to calculate/consider eb.

Required Minimum End Thickness Excl.Allow. e_{min} :

$$e_{min} = e_{min} = 1.69 = \underline{\underline{1.6877 \text{ mm}}}$$

Required Minimum End Thickness Incl.Allow. :

$$e_{minA} = e_{min} + c + t_h = 1.69 + 0 + 0.3 = \underline{\underline{1.9900 \text{ mm}}}$$

Internal Pressure $e_{minA}=1.99 \leq e_n=2.5$[mm]	79.6%	OK
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Analysis Thickness

$$e_a = e_n - c - t_h = 2.5 - 0 - 0.3 = 2.2000 \text{ mm}$$

Inside Diameter of Shell

$$D_i = D_e - 2 * (e_n - c) = 168.3 - 2 * (2.5 - 0) = 163.30 \text{ mm}$$

Mean Diameter of Shell

$$D_m = (D_e + D_i) / 2 = (168.3 + 163.3) / 2 = 165.80 \text{ mm}$$

7.5.3.4 - Required Minimum Thickness of Straight Cylindrical Flange

$$L_{lim} = 0.2 * \text{SQRT}(D_i * e_{min}) = 0.2 * \text{SQRT}(163.3 * 1.69) = 3.3202 \text{ mm}$$

Since $L_{cyl} > L_{lim}$, Required Thickness of Straight Cylindrical Flange to 7.4.2

Minimum Thickness of Straight Flange Excl. Allow.

$$e_{cyl} = P * D_i / (2 * f * z - P) \quad (7.4-1)$$

$$= 3.3 * 163.3 / (2 * 160.67 * 1 - 3.3) = \underline{\underline{1.6944 \text{ mm}}}$$

Minimum Thickness of Straight Flange Incl.Corr. :

$$e_{cylA} = e_{cyl} + c = 1.69 + 0 = \underline{\underline{1.6900 \text{ mm}}}$$

7.5.3.1 Conditions of Applicability - Torispherical Ends

»Geometry Check $r=25.92 \leq 0.2 * D_i=32.66$ [mm] « » OK«

»Geometry Check $r=25.92 \geq 0.06 * D_i=9.8$ [mm] « » OK«

»Geometry Check $r=25.92 \geq 2 * e=3.38$ [mm] « » OK«

»Geometry Check $e=1.69 \leq 0.08 * D_e=13.46$ [mm] « » OK«

»Geometry Check $e_a=2.2 \geq 0.001 * D_e=0.1683$ [mm] « » OK«

»Geometry Check $R=134.64 \leq D_e=168.3$ [mm] « » OK«

MAXIMUM ALLOWABLE WORKING PRESSURE MAWP :NEW & COLD

$$P_s = 2 * f * z * e_a / (R + 0.5 * e_a) \quad (7.5-6)$$

$$= 2 * 170.83 * 1 * 2.2 / (134.64 + 0.5 * 2.2) = 5.5374 \text{ MPa}$$

$$P_y = f * e_a / (\text{beta} * (0.75 * R + 0.2 * D_i)) \quad (7.5-7)$$

$$= 170.83 * 2.2 / (0.5931 * (0.75 * 134.64 + 0.2 * 163.3)) = 4.7420 \text{ MPa}$$

$$P_B = 111 * f_b * (e_a / (0.75 * R + 0.2 * D_i)) ^ 1.5 * (r / D_i) ^ 0.825 \quad (7.5-8)$$

$$= 111 * 282.67 * (2.2 / (0.75 * 134.64 + 0.2 * 163.3)) ^ 1.5 * (25.92 / 163.3) ^ 0.825 = 14.52 \text{ MPa}$$

$$P_{cyl} = 2 * e_a * f * z / (D_i + e_a)$$

$$= 2 * 2.2 * 170.83 * 1 / (163.3 + 2.2) = 4.5417 \text{ MPa}$$

P_{max} (is the least of P_s , P_y , P_b and P_{cyl}) = P_{max}

$$= 4.54 = \underline{\underline{4.5417 \text{ MPa}}}$$

MAXIMUM ALLOWABLE WORKING PRESSURE MAWP :HOT & CORR

$$P_s = 2 * f * z * e_a / (R + 0.5 * e_a) \quad (7.5-6)$$

$$= 2 * 160.67 * 1 * 2.2 / (134.64 + 0.5 * 2.2) = 5.2081 \text{ MPa}$$

$$P_y = f * e_a / (\text{beta} * (0.75 * R + 0.2 * D_i)) \quad (7.5-7)$$

$$= 160.67 * 2.2 / (0.5931 * (0.75 * 134.64 + 0.2 * 163.3)) = 4.4599 \text{ MPa}$$

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$$PB = 111 * fb * (ea / (0.75 * R + 0.2 * Di))^{1.5} * (r / Di)^{0.825} \quad (7.5-8)$$
$$= 111 * 257.07 * (2.2 / (0.75 * 134.64 + 0.2 * 163.3))^{1.5} * (25.92 / 163.3)^{0.825} = 13.20 \text{ MPa}$$
$$P_{cyl} = 2 * ea * f * z / (Di + ea)$$
$$= 2 * 2.2 * 160.67 * 1 / (163.3 + 2.2) = 4.2716 \text{ MPa}$$
$$P_{max} \text{ (is the least of } P_s, P_y, P_b \text{ and } P_{cyl}) = P_{max}$$
$$= 4.27 = \underline{\underline{4.2716 \text{ MPa}}}$$

MAX TEST PRESSURE (Uncorroded cond.at ambient temp.)

$$P_s = 2 * f * z * ea / (R + 0.5 * ea) \quad (7.5-6)$$
$$= 2 * 252.38 * 1 * 2.2 / (134.64 + 0.5 * 2.2) = 8.1809 \text{ MPa}$$
$$P_y = f * ea / (\beta * (0.75 * R + 0.2 * Di)) \quad (7.5-7)$$
$$= 252.38 * 2.2 / (0.5931 * (0.75 * 134.64 + 0.2 * 163.3)) = 7.0057 \text{ MPa}$$
$$PB = 111 * fb * (ea / (0.75 * R + 0.2 * Di))^{1.5} * (r / Di)^{0.825} \quad (7.5-8)$$
$$= 111 * 403.81 * (2.2 / (0.75 * 134.64 + 0.2 * 163.3))^{1.5} * (25.92 / 163.3)^{0.825} = 20.74 \text{ MPa}$$
$$P_{cyl} = 2 * ea * f * z / (Di + ea)$$
$$= 2 * 2.2 * 252.38 * 1 / (163.3 + 2.2) = 6.7098 \text{ MPa}$$
$$P_{max} \text{ (is the least of } P_s, P_y, P_b \text{ and } P_{cyl}) = P_{max}$$
$$= 6.71 = \underline{\underline{6.7098 \text{ MPa}}}$$

EN13445-5;10.2.3.3 REQUIRED MIN.HYDROSTATIC TEST PRESSURE:Ptmin

NEW AT AMBIENT TEMP. FOR TEST GROUPS 1, 2 and 3

$$Ptmin = 1.25 * Pd * f_{20} / f = 1.25 * 3.3 * 170.83 / 160.67 = \underline{\underline{4.3858 \text{ MPa}}}$$

$$Ptmin = 1.43 * Pd = 1.43 * 3.3 = \underline{\underline{4.7190 \text{ MPa}}}$$

Test Pressure Ptmin=4.72 <= Pmax=6.71[MPa]**70.3%****OK**

Maximum diameter of Opening Not Requiring Reinforcement Check , dmax

$$r_{is} = R \quad (9.5-4) = 134.64 = 134.64 \text{ mm}$$
$$\text{Length of Shell Contributing to Reinforcement}$$
$$I_s = \text{Sqr}((2 * r_{is} + ea) * ea) \quad (9.5-2)$$
$$= \text{Sqr}((2 * 134.64 + 2.2) * 2.2) = 24.44 \text{ mm}$$
$$\text{Maximum Diameter of Unreinforced Opening in Shell Checked to Rules in Section 9}$$
$$d_{max1} = (ea * I_s * (f - 0.5 * P) / (P - r_{is} * I_s)) / (0.5 * r_{is} + 0.5 * ea) \quad (9.5-7, 22, 23)$$
$$= (2.2 * 24.44 * (160.67 - 0.5 * 3.3) / (3.3 - 134.64 * 24.44)) / (0.5 * 134.64 + 0.5 * 2.2)$$
$$= 0.00 \text{ mm}$$
$$\text{Maximum diameter of Opening Not Requiring Reinforcement Check}$$
$$d_{max2} = 0.15 * \text{Sqr}((2 * r_{is} + ea) * ea) \quad (9.5-18)$$
$$= 0.15 * \text{Sqr}((2 * 134.64 + 2.2) * 2.2) = 3.6658 \text{ mm}$$
$$\text{Maximum Diameter of Unreinforced Opening}$$
$$d_{max} = \text{MAX}(d_{max1}, d_{max2}) = \text{MAX}(0, 3.67) = \underline{\underline{3.6658 \text{ mm}}}$$

CALCULATION SUMMARY

7.5.3 - TORISPHERICAL ENDS UNDER INTERNAL PRESSURE

7.5.3.2 Required Minimum End Thickness

$$\text{Required Minimum End Thickness Excl.Allow. } e_{min} :$$
$$e_{min} = e_{min} = 1.69 = \underline{\underline{1.6877 \text{ mm}}}$$

$$\text{Required Minimum End Thickness Incl.Allow. } :$$
$$e_{min_a} = e_{min} + c + th = 1.69 + 0 + 0.3 = \underline{\underline{1.9900 \text{ mm}}}$$

Internal Pressure e_{min_a}=1.99 <= e_n=2.5[mm]**79.6%****OK**

Minimum Thickness of Straight Flange Incl.Corr. :

$$e_{cyl_a} = e_{cyl} + c = 1.69 + 0 = \underline{\underline{1.6900 \text{ mm}}}$$

MAXIMUM ALLOWABLE WORKING PRESSURE MAWP :NEW & COLD

$$P_{max} \text{ (is the least of } P_s, P_y, P_b \text{ and } P_{cyl}) = P_{max}$$
$$= 4.54 = \underline{\underline{4.5417 \text{ MPa}}}$$

Company Name -

Client :GÜVEN SOGUTMA

Vessel Tag No.:OS.F.33B.54.1

Visual Vessel Design by Hexagon AB,Ver:19.0- Operator : Rev.:A

EN13445:2014 Issue 5:2018+A5 - 7.5 DOMED ENDS

E3.1 End 19 Feb. 2020 17:26 ConnID:S1.1

MAXIMUM ALLOWABLE WORKING PRESSURE MAWP :HOT & CORRPmax (is the least of Ps, Py, Pb and Pcyl) = Pmax
=4.27=4.2716 MPa**MAX TEST PRESSURE (Uncorroded cond.at ambient temp.)**Pmax (is the least of Ps, Py, Pb and Pcyl) = Pmax
=6.71=6.7098 MPa**EN13445-5;10.2.3.3 REQUIRED MIN.HYDROSTATIC TEST PRESSURE:Ptmin**

NEW AT AMBIENT TEMP. FOR TEST GROUPS 1, 2 and 3

Ptmin = 1.25 * Pd * f20 / f =1.25*3.3*170.83/160.67=

4.3858 MPa

Ptmin = 1.43 * Pd =1.43*3.3=

4.7190 MPa**Test Pressure Ptmin=4.72 <= Pmax=6.71[MPa]****70.3%****OK****Maximum diameter of Opening Not Requiring Reinforcement Check , dmax**

Maximum Diameter of Unreinforced Opening

dmax = MAX(dmax1, dmax2) =MAX(0,3.67)=

3.6658 mm

Volume:0.0007900 m3 Weight:0.7 kg (SG= 7.85)

Company Name -

Client :GÜVEN SOGUTMA

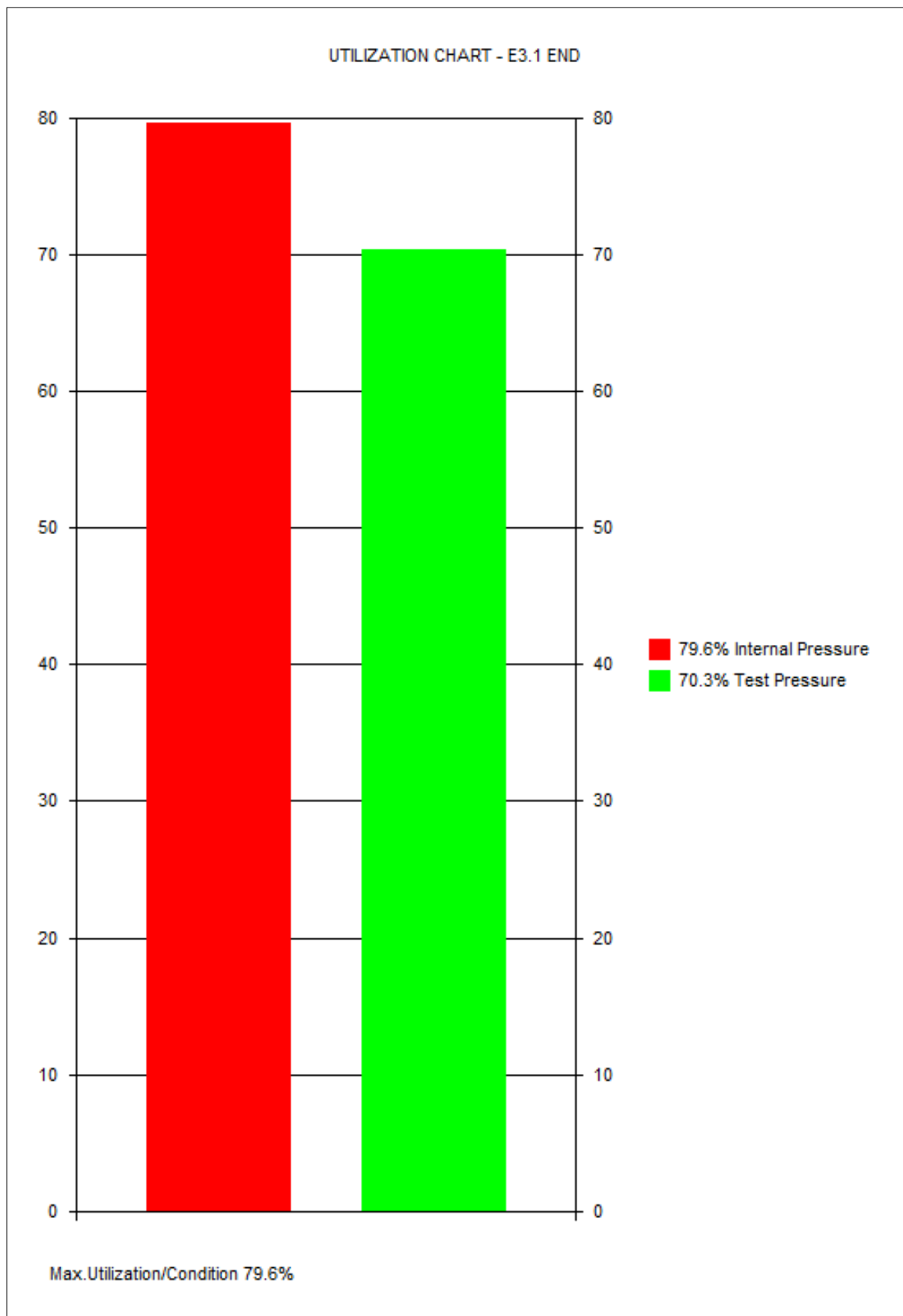
Vessel Tag No.:OS.F.33B.54.1

Visual Vessel Design by Hexagon AB,Ver:19.0- Operator : Rev.:A

EN13445:2014 Issue 5:2018+A5 - 7.5 DOMED ENDS

E3.1 End

19 Feb. 2020 17:26 ConnID:S1.1



Company Name -

Client :GÜVEN SOGUTMA

Vessel Tag No.:OS.F.33B.54.1

Visual Vessel Design by Hexagon AB,Ver:19.0- Operator : Rev.:A

EN13445:2014 Issue 5:2018+A5 - 10.5 BOLTED CIRCULAR FLAT END

E5.1 Cover Flange 23 Feb. 2020 18:42 ConnID:F.1

INPUT DATA

COMPONENT ATTACHMENT/LOCATION

Attachment: F.1 RT - Flange Shell Flange S1.1
Location: Along z-axis z1= 321

GENERAL DESIGN DATA

PROCESS CARD: General Design Data : Temp= 100°C, P=3.3000 MPa, c=0.0 mm
SPECIFIC DENSITY OF OPERATING LIQUID.....:SG 0.00
LIQUID HEAD.....:LH 0.00 mm
Check Deflection of Cover to TEMA RCB-9-21(multipass units): NO
Shape of Cover: Circular
Stayed Flat Plate to section 20.2: NO
Circular flat ends with radial reinforcement ribs to section 21: NO

DATA FOR MATING FLANGE (F.1)

TYPE OF BLIND FLANGE: Blind flange with gasket entirely within the bolt circle.
OUTSIDE DIAMETER OF FLANGE.....:A 218.00 mm
BOLT-CIRCLE DIAMETER.....:C 193.00 mm
NUMBER OF BOLTS.....:n 10.00
DIAMETER OF BOLT HOLES IN FLANGE.....:d 12.00 mm
FLANGE DESIGN BOLT LOAD FOR ASSEMBLY CONDITION.....:W 103.78 kN
DIAMETER AT LOCATION OF GASKET LOAD REACTION.....:G 167.50 mm
GASKET FACTOR.....:m 2.0000
EFFECTIVE GASKET SEATING WIDTH.....:b 2.5000 mm

DATA FOR BLIND FLANGE

NOMINAL THICKNESS OF HEAD/END (uncorroded).....:en 18.00 mm
THICKNESS OF FLANGE(uncorroded).....:e 18.00 mm
EN 10028-2:2017, 1.0473 P355GH plate and strip, HT:N THK<=40mm 100'C
Rm=510 Rp=345 Rpt=314 f=209.33 f20=212.5 ftest=328.57 E=206067(N/mm2) ro=7.85

WELDING REQUIREMENTS TO EN 1708-1:2010

Comment(Optional):
Type of welded connection: Not Applicable

CALCULATION DATA

10.5.2.1 MINIMUM THICKNESS OF BLIND FLANGE WITHIN GASKET e

Mean Bolt Pitch
 $tB = \text{PI} * C / n = 3.14 * 193 / 10 = 60.63 \text{ mm}$
 $Cf = \text{MAX}(\text{Sqr}(tB / (2 * db + 6 * (eb - c) / (0.5 + m))), 1)$ (10.5-4)
 $= \text{MAX}(\text{Sqr}(60.63 / (2 * 10.8 + 6 * (18 - 0) / (0.5 + 2))), 1) = 1.0000$
Bolting Up Conditions
 $ea = \text{Sqr}(Cf * 3 * (C - G) / (\text{PI} * G) * (W / f20))$ (10.5-2)
 $= \text{Sqr}(1 * 3 * (193 - 167.5) / (3.14 * 167.5) * (103.78 / 212.5)) = 8.4261 \text{ mm}$
Operating Conditions
 $eP = \text{Sqr}((0.31 * G^2 + 3 * Cf * (G / 4 + 2 * b * m) * (C - G)) * P / f)$ (10.5-3)
 $= \text{Sqr}((0.31 * 167.5^2 + 3 * 1 * (167.5 / 4 + 2 * 2.5 * 2) * (193 - 167.5)) * 3.3 / 209.33) = 14.13 \text{ mm}$
Minimum thickness excluding corrosion e_{min}
 $e_{min} = \text{Max}(ea, eP)$ (10.5-1) = $\text{Max}(8.43, 14.13) = 14.13 \text{ mm}$
Minimum thickness including allowance e
 $e = e_{min} + c = 14.13 + 0 = 14.13 \text{ mm}$

End Thickness $e_n = 18 \geq e = 14.131 [\text{mm}]$

78.5%

OK

10.5.2.2 MINIMUM THICKNESS OF FLANGED EXTENSION e_1

$e_{P1} = \text{Sqr}(3 * Cf * (G / 4 + 2 * b * m) * (C - G) * P / f)$ (10.5-6)
 $= \text{Sqr}(3 * 1 * (167.5 / 4 + 2 * 2.5 * 2) * (193 - 167.5) * 3.3 / 209.33) = 7.9095 \text{ mm}$
 $e_1 = \text{Max}(ea, e_{P1})$ (10.5-5) = $\text{Max}(8.43, 7.91) = 8.4260 \text{ mm}$

Company Name -

Client :GÜVEN SOGUTMA

Vessel Tag No.:OS.F.33B.54.1

Visual Vessel Design by Hexagon AB,Ver:19.0- Operator : Rev.:A

EN13445:2014 Issue 5:2018+A5 - 10.5 BOLTED CIRCULAR FLAT END

E5.1 Cover Flange 23 Feb. 2020 18:42 ConnID:F.1

Flanged Extension Thk. eb=18 >= e1=8.426[mm]

46.8%

OK

PRESSURE CALCULATIONS

MAXIMUM ALLOWABLE WORKING PRESSURE MAWP :NEW & COLD

$$P_{max1} = e_a^2 * f / (0.31 * G^2 + 3 * C_f * (G/4 + 2 * b * m) * (C - G))$$
$$= 18^2 * 212.5 / (0.31 * 167.5^2 + 3 * 1 * (167.5/4 + 2 * 2.5 * 2) * (193 - 167.5)) = 5.4359 \text{ MPa}$$

$$P_{max2} = e_1^2 * f / (3 * C_f * (G/4 + 2 * b * m) * (C - G))$$
$$= 18^2 * 212.5 / (3 * 1 * (167.5/4 + 2 * 2.5 * 2) * (193 - 167.5)) = 17.35 \text{ MPa}$$

$$P_{max} = \text{MIN}(P_{max1} , P_{max2}) = \text{MIN}(5.44, 17.35) = 5.4359 \text{ MPa}$$

MAXIMUM ALLOWABLE WORKING PRESSURE MAWP :HOT & CORR

$$P_{max1} = e_a^2 * f / (0.31 * G^2 + 3 * C_f * (G/4 + 2 * b * m) * (C - G))$$
$$= 18^2 * 209.33 / (0.31 * 167.5^2 + 3 * 1 * (167.5/4 + 2 * 2.5 * 2) * (193 - 167.5)) = 5.3548 \text{ MPa}$$

$$P_{max2} = e_1^2 * f / (3 * C_f * (G/4 + 2 * b * m) * (C - G))$$
$$= 18^2 * 209.33 / (3 * 1 * (167.5/4 + 2 * 2.5 * 2) * (193 - 167.5)) = 17.09 \text{ MPa}$$

$$P_{max} = \text{MIN}(P_{max1} , P_{max2}) = \text{MIN}(5.35, 17.09) = 5.3548 \text{ MPa}$$

MAX TEST PRESSURE (Uncorroded cond.at ambient temp.)

$$P_{max1} = e_a^2 * f / (0.31 * G^2 + 3 * C_f * (G/4 + 2 * b * m) * (C - G))$$
$$= 18^2 * 328.57 / (0.31 * 167.5^2 + 3 * 1 * (167.5/4 + 2 * 2.5 * 2) * (193 - 167.5)) = 8.4050 \text{ MPa}$$

$$P_{max2} = e_1^2 * f / (3 * C_f * (G/4 + 2 * b * m) * (C - G))$$
$$= 18^2 * 328.57 / (3 * 1 * (167.5/4 + 2 * 2.5 * 2) * (193 - 167.5)) = 26.83 \text{ MPa}$$

$$P_{max} = \text{MIN}(P_{max1} , P_{max2}) = \text{MIN}(8.41, 26.83) = 8.4050 \text{ MPa}$$

EN13445-5;10.2.3.3 REQUIRED MIN.HYDROSTATIC TEST PRESSURE:Ptmin

NEW AT AMBIENT TEMP. FOR TEST GROUPS 1, 2 and 3

$$P_{tmin} = 1.25 * P_d * f_{20} / f = 1.25 * 3.3 * 212.5 / 209.33 = 4.1875 \text{ MPa}$$

$$P_{tmin} = 1.43 * P_d = 1.43 * 3.3 = 4.7190 \text{ MPa}$$

Test Pressure Ptmin=4.72 <= Pmax=8.41[MPa]

56.1%

OK

CALCULATION SUMMARY

10.5.2.1 MINIMUM THICKNESS OF BLIND FLANGE WITHIN GASKET e

Minimum thickness excluding corrosion emin

$$e_{min} = \text{Max}(e_A , e_P) (10.5-1) = \text{Max}(8.43, 14.13) = 14.13 \text{ mm}$$

Minimum thickness including allowance e

$$e = e_{min} + c = 14.13 + 0 = 14.13 \text{ mm}$$

End Thickness en=18 >= e=14.131[mm]

78.5%

OK

10.5.2.2 MINIMUM THICKNESS OF FLANGED EXTENSION e1

$$e_1 = \text{Max}(e_A , e_{P1}) (10.5-5) = \text{Max}(8.43, 7.91) = 8.4260 \text{ mm}$$

Flanged Extension Thk. eb=18 >= e1=8.426[mm]

46.8%

OK

PRESSURE CALCULATIONS

MAXIMUM ALLOWABLE WORKING PRESSURE MAWP :NEW & COLD

$$P_{max} = \text{MIN}(P_{max1} , P_{max2}) = \text{MIN}(5.44, 17.35) = 5.4359 \text{ MPa}$$

Company Name -

Client :GÜVEN SOGUTMA

Vessel Tag No.:OS.F.33B.54.1

Visual Vessel Design by Hexagon AB,Ver:19.0- Operator : Rev.:A

EN13445:2014 Issue 5:2018+A5 - 10.5 BOLTED CIRCULAR FLAT END

E5.1 Cover Flange 23 Feb. 2020 18:42 ConnID:F.1

MAXIMUM ALLOWABLE WORKING PRESSURE MAWP :HOT & CORR $P_{max} = \text{MIN}(P_{max1} , P_{max2}) = \text{MIN}(5.35,17.09) =$ 5.3548 MPa**MAX TEST PRESSURE (Uncorroded cond.at ambient temp.)** $P_{max} = \text{MIN}(P_{max1} , P_{max2}) = \text{MIN}(8.41,26.83) =$ 8.4050 MPa**EN13445-5;10.2.3.3 REQUIRED MIN.HYDROSTATIC TEST PRESSURE:Ptmin**

NEW AT AMBIENT TEMP. FOR TEST GROUPS 1, 2 and 3

 $P_{tmin} = 1.25 * P_d * f_{20} / f = 1.25 * 3.3 * 212.5 / 209.33 =$ 4.1875 MPa $P_{tmin} = 1.43 * P_d = 1.43 * 3.3 =$ 4.7190 MPa**Test Pressure Ptmin=4.72 <= Pmax=8.41[MPa]****56.1%****OK**

Volume:0.00 m3 Weight:5 kg (SG= 7.85)

Company Name -

Client :GÜVEN SOGUTMA

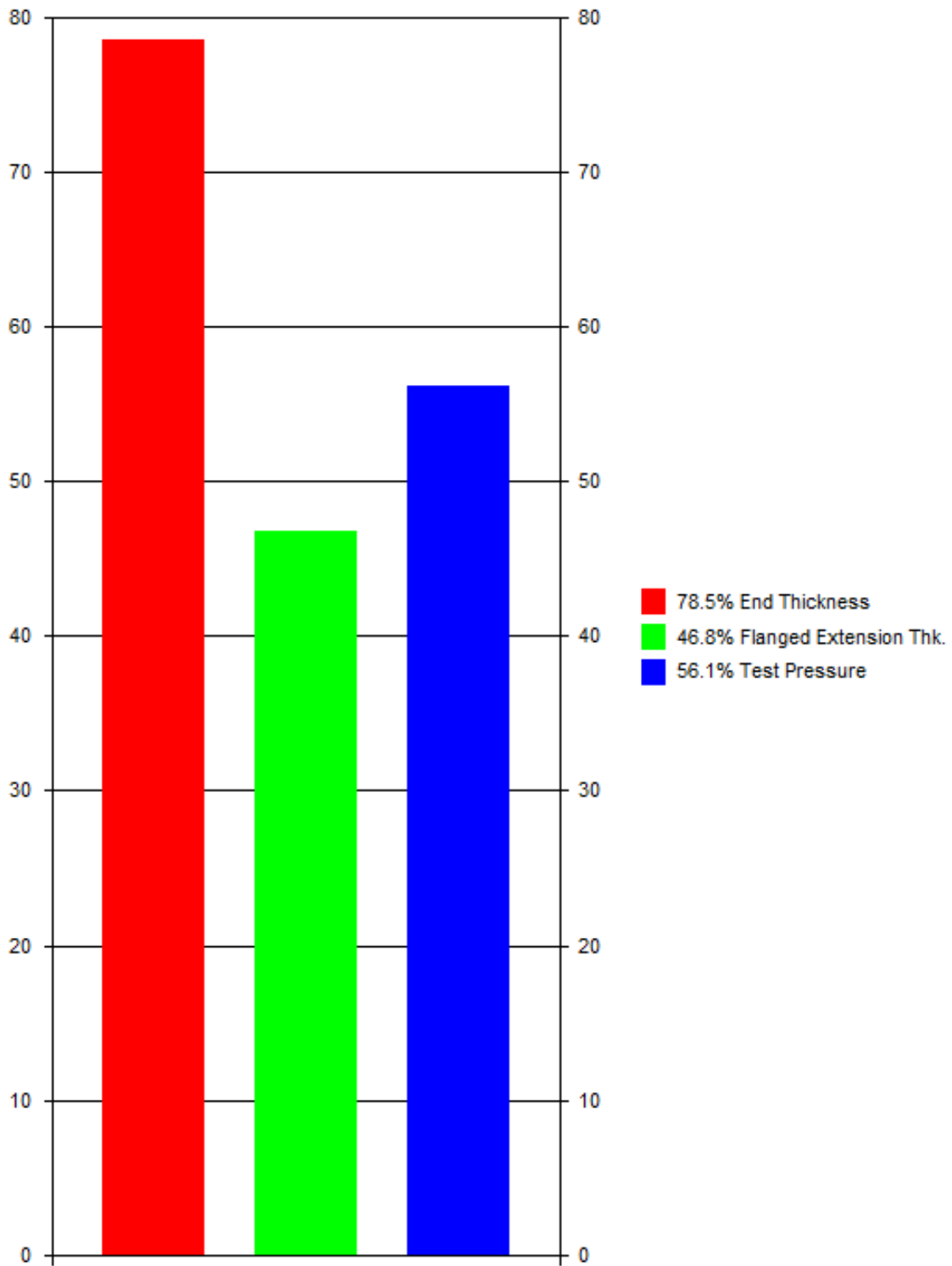
Vessel Tag No.:OS.F.33B.54.1

Visual Vessel Design by Hexagon AB,Ver:19.0- Operator : Rev.:A

EN13445:2014 Issue 5:2018+A5 - 10.5 BOLTED CIRCULAR FLAT END

E5.1 Cover Flange 23 Feb. 2020 18:42 ConnID:F.1

UTILIZATION CHART - E5.1 COVER FLANGE



Max.Utilization/Condition 78.5%

Company Name -

Client :GÜVEN SOGUTMA

Vessel Tag No.:OS.F.33B.54.1

Visual Vessel Design by Hexagon AB,Ver:19.0- Operator : Rev.:A

EN13445:2014 Issue 5:2018+A5 - 9.5 ISOLATED OPENINGS IN SHELLS

N.1 Inlet 23 Feb. 2020 18:42 ConnID:E5.1

INPUT DATA

COMPONENT ATTACHMENT/LOCATION

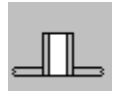
Attachment: E5.1 Bolted Flat End Cover Flange F.1
Connect this nozzle to the nozzle neck of another nozzle: NO



Off Center

Orientation & Location of Nozzle: Radial to End (Off Center)
Angle of Rotation of nozzle axis projected in the x-y plane:Phi 0.00 Degr.
Distance between Center of End and Center of Nozzle.:R 50.00 mm

GENERAL DESIGN DATA



Type of Opening: Nozzle Without Standard ASME or DIN/EN Flange Attachment
PRESSURE LOADING: Design Component for Internal Pressure Only
PROCESS CARD:
General Design Data : Temp= 100°C, P=3.3000 MPa, c=0.0 mm, Pext=0.0000 MPa
SPECIFIC DENSITY OF OPERATING LIQUID.....:SG 0.00
LIQUID HEAD.....:LH 0.00 mm
Apply a different corrosion allowance to nozzle neck than the shell thickness.: NO

SHELL DATA (E5.1)

Shell Type: Bolted Flat End
INSIDE DIAMETER OF SHELL/GASKET LOAD REACTION.....:Di 167.50 mm
NOMINAL WALL THICKNESS (uncorroded).....:en 18.00 mm
REQUIRED THICKNESS OF UNPIERCED END(corroded).....:eo 14.13 mm
EN 10028-2:2017, 1.0473 P355GH plate and strip, HT:N THK<=40mm 100'C
Rm=510 Rp=345 Rpt=314 fs=209.33 f20=212.5 ftest=328.57 E=206067(N/mm2) ro=7.85

NOZZLE MATERIAL DATA



Delivery Form: Seamless Pipe
EN 10217-2:2002/A1:05, 1.0345 P235GH welded tube, HT:N THK<=16mm 100'C
Rm=360 Rp=235 Rpt=198 fb=132 f20=150 ftest=223.81 E=206067(N/mm2) ro=7.85

NOZZLE DIMENSIONAL DATA



Attachment: Set On Nozzle
Application:
9.4.6.3 NOT a critical fatigue area, and calc.temp.is outside creep range.
OUTSIDE NOZZLE DIAMETER.....:deb 62.00 mm
NOMINAL NOZZLE THICKNESS (uncorroded).....:enb 5.0000 mm
Size of Flange and Nozzle:
Comment (Optional):
NEGATIVE TOLERANCE/THINNING ALLOWANCE.....: 10.00 %
NOZZLE STANDOUT MEASURED FROM VESSEL OD.....:ho 25.00 mm

Company Name -

Client :GÜVEN SOGUTMA

Vessel Tag No.:OS.F.33B.54.1

Visual Vessel Design by Hexagon AB,Ver:19.0- Operator : Rev.:A

EN13445:2014 Issue 5:2018+A5 - 9.5 ISOLATED OPENINGS IN SHELLS

N.1 Inlet 23 Feb. 2020 18:42 ConnID:E5.1

WELDING REQUIREMENTS TO EN 1708-1:2010

Comment(Optional):

Type of welded connection: Not Applicable

CALCULATION DATA**PRELIMINARY CALCULATIONS**

Shell Analysis Thickness eas

$$eas = en - c = 18 - 0 = 18.00 \text{ mm}$$

Nozzle Analysis Thickness eab

$$eab = enb - cn - NegDev = 5 - 0 - 0.5 = 4.5000 \text{ mm}$$

$$dib = deb - 2 * eab = 62 - 2 * 4.5 = 53.00 \text{ mm}$$

Min.Nozzle Thk.Based on Internal Pressure ebp

$$ebp = P * deb / (2 * fb * z + P) = 3.3 * 62 / (2 * 132 * 1 + 3.3) = 0.7700 \text{ mm}$$

Min.Nozzle Thk. ebp=0.77 <= eab=4.5[mm]	17.1%	OK
---	--------------	-----------

Limit of Reinforcement Along Nozzle

$$Ibo = \text{MIN}(0.8 * \text{Sqr}((dib + eab) * eab), ho) = \text{MIN}(0.8 * \text{Sqr}((53 + 4.5) * 4.5), 25) = 12.87 \text{ mm} \quad (10.6-8)$$

$$A = Ibo * (eab - ebp) = 12.87 * (4.5 - 0.77) = 48.00 \text{ mm}^2$$

$$A = \text{MIN}(A, A * fb / fs) = \text{MIN}(48., 48. * 132 / 209.33) = 30.27 \text{ mm}^2 \quad (10.6-7)$$

$$deq = dib - 2 * A / eas = 53 - 2 * 30.27 / 18 = 49.64 \text{ mm} \quad (10.6-5)$$

10.6 PIERCED CIRCULAR FLAT ENDS

Calculation Coefficient for Opening Reinforcement Y1 and Y2

$$Y2 = \text{SQR}(G / (G - deq)) = \text{SQR}(167.5 / (167.5 - 49.64)) = 1.1921 \quad (10.6-4)$$

Required Minimum Thickness of End due to Opening emin

$$emin = Y2 * eo + c = 1.19 * 14.13 + 0 = 16.84 \text{ mm} \quad (10.6-2)$$

Req.Unpierced End Thk. emin=16.84 <= en=18[mm]	93.5%	OK
--	--------------	-----------

Weight of Nozzle: .1757kg Pad: 0kg

CALCULATION SUMMARY

Min.Nozzle Thk. ebp=0.77 <= eab=4.5[mm]	17.1%	OK
---	--------------	-----------

Limit of Reinforcement Along Nozzle

$$Ibo = \text{MIN}(0.8 * \text{Sqr}((dib + eab) * eab), ho) = \text{MIN}(0.8 * \text{Sqr}((53 + 4.5) * 4.5), 25) = 12.87 \text{ mm} \quad (10.6-8)$$

$$A = Ibo * (eab - ebp) = 12.87 * (4.5 - 0.77) = 48.00 \text{ mm}^2$$

Required Minimum Thickness of End due to Opening emin

$$emin = Y2 * eo + c = 1.19 * 14.13 + 0 = 16.84 \text{ mm} \quad (10.6-2)$$

Req.Unpierced End Thk. emin=16.84 <= en=18[mm]	93.5%	OK
--	--------------	-----------

Volume:0.0001000 m3 Weight:0.2 kg (SG= 7.85)

Company Name -

Client :GÜVEN SOGUTMA

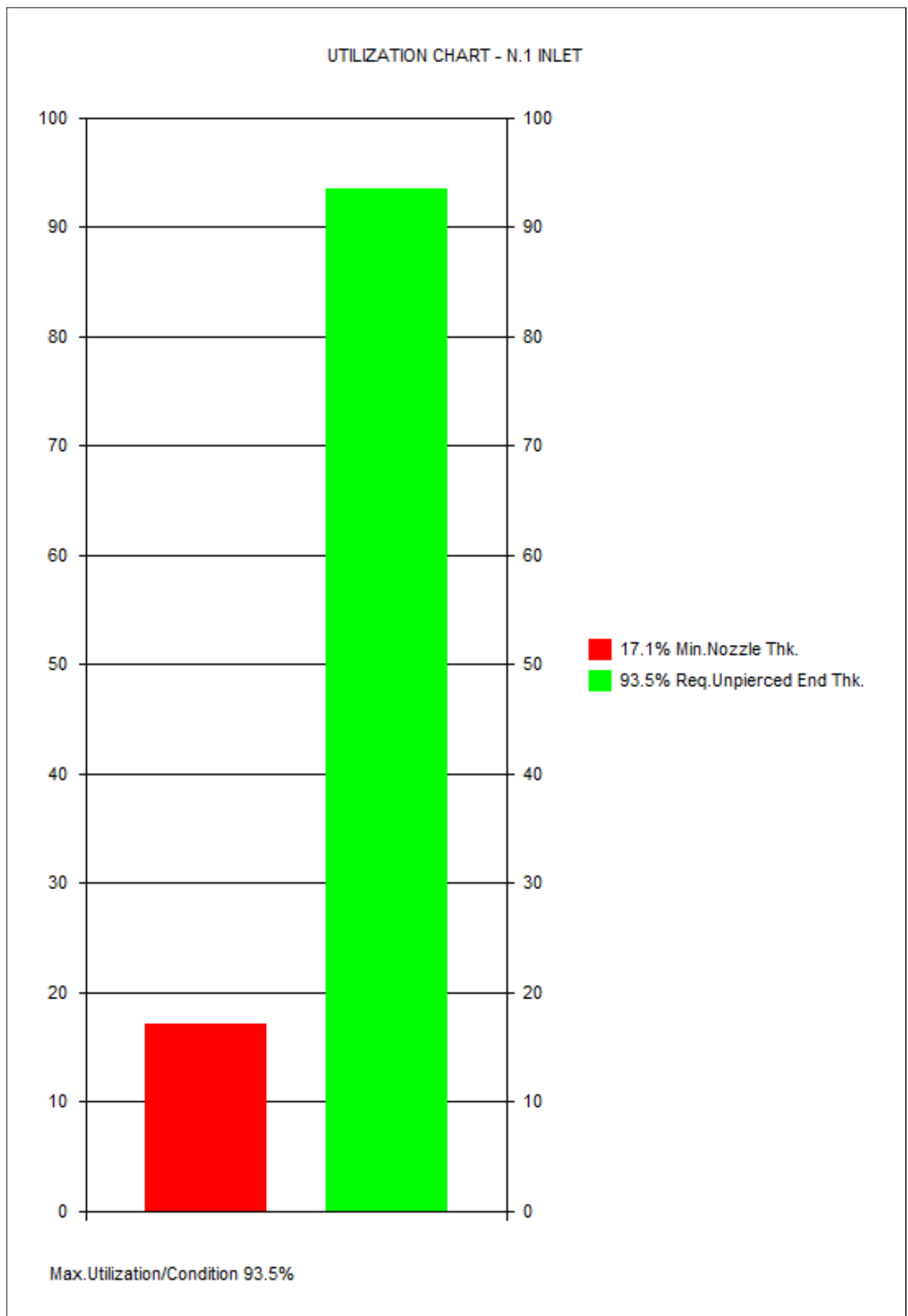
Vessel Tag No.:OS.F.33B.54.1

Visual Vessel Design by Hexagon AB,Ver:19.0- Operator : Rev.:A

EN13445:2014 Issue 5:2018+A5 - 9.5 ISOLATED OPENINGS IN SHELLS

N.1 Inlet

23 Feb. 2020 18:42 ConnID:E5.1



Company Name -

Client :GÜVEN SOGUTMA

Vessel Tag No.:OS.F.33B.54.1

Visual Vessel Design by Hexagon AB,Ver:19.0- Operator : Rev.:A

EN13445:2014 Issue 5:2018+A5 - 9.5 ISOLATED OPENINGS IN SHELLS

N.2 Outlet 23 Feb. 2020 18:42 ConnID:E5.1

INPUT DATA

COMPONENT ATTACHMENT/LOCATION

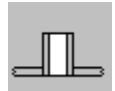
Attachment: E5.1 Bolted Flat End Cover Flange F.1
Connect this nozzle to the nozzle neck of another nozzle: NO



Off Center

Orientation & Location of Nozzle: Radial to End (Off Center)
Angle of Rotation of nozzle axis projected in the x-y plane:Phi 180.00 Degr.
Distance between Center of End and Center of Nozzle.:R 50.00 mm

GENERAL DESIGN DATA



Type of Opening: Nozzle Without Standard ASME or DIN/EN Flange Attachment
PRESSURE LOADING: Design Component for Internal Pressure Only
PROCESS CARD:
General Design Data : Temp= 100°C, P=3.3000 MPa, c=0.0 mm, Pext=0.0000 MPa
SPECIFIC DENSITY OF OPERATING LIQUID.....:SG 0.00
LIQUID HEAD.....:LH 0.00 mm
Apply a different corrosion allowance to nozzle neck than the shell thickness.: NO

SHELL DATA (E5.1)

Shell Type: Bolted Flat End
INSIDE DIAMETER OF SHELL/GASKET LOAD REACTION.....:Di 167.50 mm
NOMINAL WALL THICKNESS (uncorroded).....:en 18.00 mm
REQUIRED THICKNESS OF UNPIERCED END(corroded).....:eo 14.13 mm
EN 10028-2:2017, 1.0473 P355GH plate and strip, HT:N THK<=40mm 100'C
Rm=510 Rp=345 Rpt=314 fs=209.33 f20=212.5 ftest=328.57 E=206067(N/mm2) ro=7.85

NOZZLE MATERIAL DATA



Delivery Form: Seamless Pipe
EN 10217-2:2002/A1:05, 1.0345 P235GH welded tube, HT:N THK<=16mm 100'C
Rm=360 Rp=235 Rpt=198 fb=132 f20=150 ftest=223.81 E=206067(N/mm2) ro=7.85

NOZZLE DIMENSIONAL DATA



Attachment: Set On Nozzle
Application:
9.4.6.3 NOT a critical fatigue area, and calc.temp.is outside creep range.
OUTSIDE NOZZLE DIAMETER.....:deb 62.00 mm
NOMINAL NOZZLE THICKNESS (uncorroded).....:enb 5.0000 mm
Size of Flange and Nozzle:
Comment (Optional):
NEGATIVE TOLERANCE/THINNING ALLOWANCE.....: 10.00 %
NOZZLE STANDOUT MEASURED FROM VESSEL OD.....:ho 25.00 mm

Company Name -

Client :GÜVEN SOGUTMA

Vessel Tag No.:OS.F.33B.54.1

Visual Vessel Design by Hexagon AB,Ver:19.0- Operator : Rev.:A

EN13445:2014 Issue 5:2018+A5 - 9.5 ISOLATED OPENINGS IN SHELLS

N.2 Outlet 23 Feb. 2020 18:42 ConnID:E5.1

WELDING REQUIREMENTS TO EN 1708-1:2010

Comment(Optional):

Type of welded connection: Not Applicable

CALCULATION DATA**PRELIMINARY CALCULATIONS**

Shell Analysis Thickness eas

$$eas = en - c = 18 - 0 = 18.00 \text{ mm}$$

Nozzle Analysis Thickness eab

$$eab = enb - cn - NegDev = 5 - 0 - 0.5 = 4.5000 \text{ mm}$$

$$dib = deb - 2 * eab = 62 - 2 * 4.5 = 53.00 \text{ mm}$$

Min.Nozzle Thk.Based on Internal Pressure ebp

$$ebp = P * deb / (2 * fb * z + P) = 3.3 * 62 / (2 * 132 * 1 + 3.3) = 0.7700 \text{ mm}$$

Min.Nozzle Thk. ebp=0.77 <= eab=4.5[mm]	17.1%	OK
---	--------------	-----------

Limit of Reinforcement Along Nozzle

$$Ibo = \text{MIN}(0.8 * \text{Sqr}((dib + eab) * eab), ho) = \text{MIN}(0.8 * \text{Sqr}((53 + 4.5) * 4.5), 25) = 12.87 \text{ mm} \quad (10.6-8)$$

$$A = Ibo * (eab - ebp) = 12.87 * (4.5 - 0.77) = 48.00 \text{ mm}^2$$

$$A = \text{MIN}(A, A * fb / fs) = \text{MIN}(48., 48. * 132 / 209.33) = 30.27 \text{ mm}^2 \quad (10.6-7)$$

$$deq = dib - 2 * A / eas = 53 - 2 * 30.27 / 18 = 49.64 \text{ mm} \quad (10.6-5)$$

10.6 PIERCED CIRCULAR FLAT ENDS

Calculation Coefficient for Opening Reinforcement Y1 and Y2

$$Y2 = \text{SQR}(G / (G - deq)) = \text{SQR}(167.5 / (167.5 - 49.64)) = 1.1921 \quad (10.6-4)$$

Required Minimum Thickness of End due to Opening emin

$$emin = Y2 * eo + c = 1.19 * 14.13 + 0 = 16.84 \text{ mm} \quad (10.6-2)$$

Req.Unpierced End Thk. emin=16.84 <= en=18[mm]	93.5%	OK
--	--------------	-----------

Weight of Nozzle: .1757kg Pad: 0kg

CALCULATION SUMMARY

Min.Nozzle Thk. ebp=0.77 <= eab=4.5[mm]	17.1%	OK
---	--------------	-----------

Limit of Reinforcement Along Nozzle

$$Ibo = \text{MIN}(0.8 * \text{Sqr}((dib + eab) * eab), ho) = \text{MIN}(0.8 * \text{Sqr}((53 + 4.5) * 4.5), 25) = 12.87 \text{ mm} \quad (10.6-8)$$

$$A = Ibo * (eab - ebp) = 12.87 * (4.5 - 0.77) = 48.00 \text{ mm}^2$$

Required Minimum Thickness of End due to Opening emin

$$emin = Y2 * eo + c = 1.19 * 14.13 + 0 = 16.84 \text{ mm} \quad (10.6-2)$$

Req.Unpierced End Thk. emin=16.84 <= en=18[mm]	93.5%	OK
--	--------------	-----------

Volume:0.0001000 m3 Weight:0.2 kg (SG= 7.85)

Company Name -

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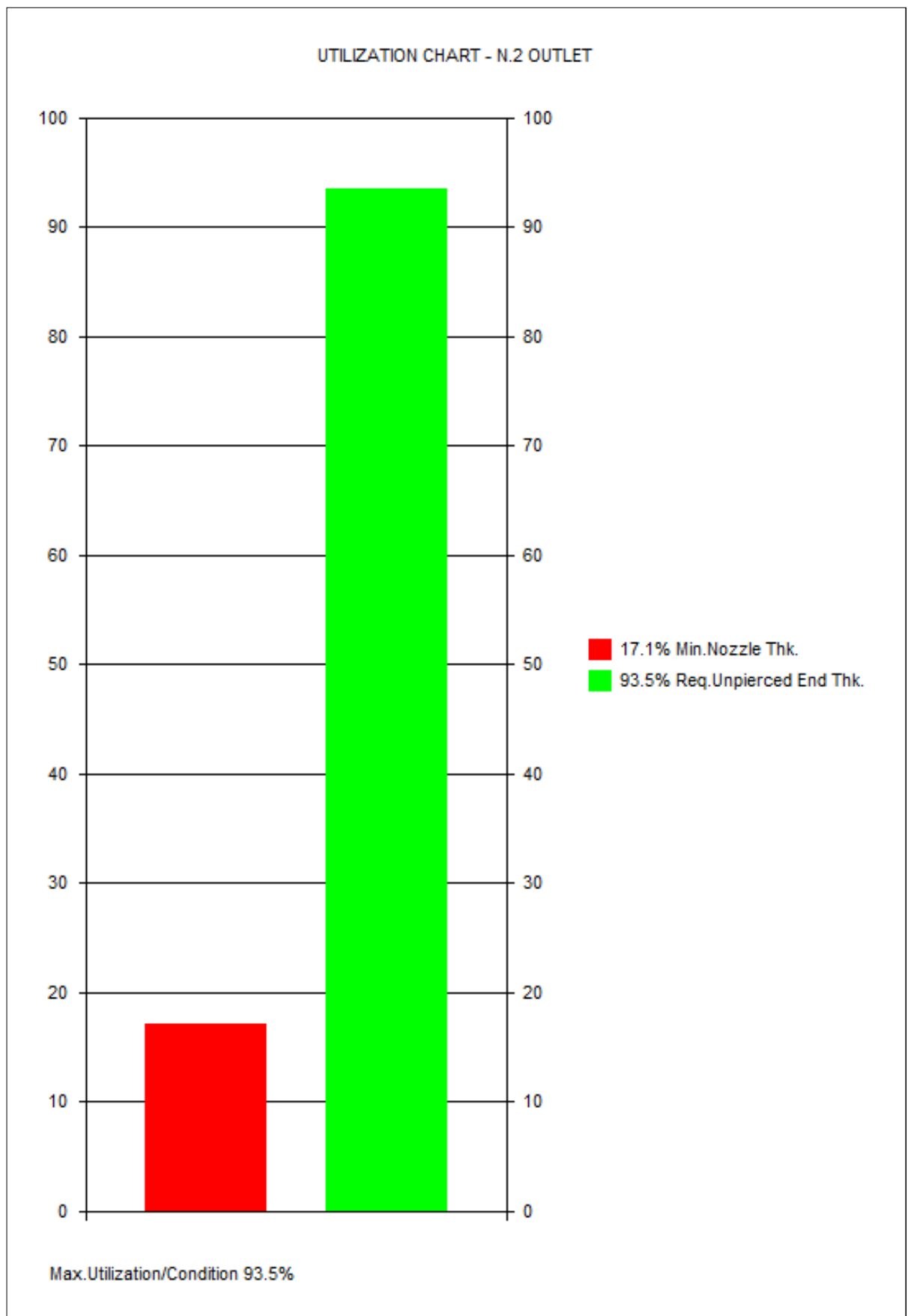
Vessel Tag No.:OS.F.33B.54.1

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N.2 Outlet

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N.3 Sae 3/8"

23 Feb. 2020 18:42 ConnID:E5.1

INPUT DATA

COMPONENT ATTACHMENT/LOCATION

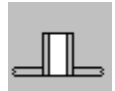
Attachment: E5.1 Bolted Flat End Cover Flange F.1
Connect this nozzle to the nozzle neck of another nozzle: NO



Off Center

Orientation & Location of Nozzle: Radial to End (Off Center)
Angle of Rotation of nozzle axis projected in the x-y plane:Phi 90.00 Degr.
Distance between Center of End and Center of Nozzle.:R 50.00 mm

GENERAL DESIGN DATA



Type of Opening: Nozzle Without Standard ASME or DIN/EN Flange Attachment
PRESSURE LOADING: Design Component for Internal Pressure Only
PROCESS CARD:
General Design Data : Temp= 100°C, P=3.3000 MPa, c=0.0 mm, Pext=0.0000 MPa
SPECIFIC DENSITY OF OPERATING LIQUID.....:SG 0.00
LIQUID HEAD.....:LH 0.00 mm
Apply a different corrosion allowance to nozzle neck than the shell thickness.: NO

SHELL DATA (E5.1)

Shell Type: Bolted Flat End
INSIDE DIAMETER OF SHELL/GASKET LOAD REACTION.....:Di 167.50 mm
NOMINAL WALL THICKNESS (uncorroded).....:en 18.00 mm
REQUIRED THICKNESS OF UNPIERCED END(corroded).....:eo 14.13 mm
EN 10028-2:2017, 1.0473 P355GH plate and strip, HT:N THK<=40mm 100'C
Rm=510 Rp=345 Rpt=314 fs=209.33 f20=212.5 ftest=328.57 E=206067(N/mm2) ro=7.85

NOZZLE MATERIAL DATA



Delivery Form: Seamless Pipe
EN 10217-2:2002/A1:05, 1.0345 P235GH welded tube, HT:N THK<=16mm 100'C
Rm=360 Rp=235 Rpt=198 fb=132 f20=150 ftest=223.81 E=206067(N/mm2) ro=7.85

NOZZLE DIMENSIONAL DATA



Attachment: Set On Nozzle
Application:
9.4.6.3 NOT a critical fatigue area, and calc.temp.is outside creep range.
OUTSIDE NOZZLE DIAMETER.....:deb 17.00 mm
NOMINAL NOZZLE THICKNESS (uncorroded).....:enb 5.0000 mm
Size of Flange and Nozzle:
Comment (Optional):
NEGATIVE TOLERANCE/THINNING ALLOWANCE.....: 10.00 %
NOZZLE STANDOUT MEASURED FROM VESSEL OD.....:ho 8.0000 mm

Company Name -

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N.3 Sae 3/8"

23 Feb. 2020 18:42 ConnID:E5.1

WELDING REQUIREMENTS TO EN 1708-1:2010

Comment(Optional):

Type of welded connection: Not Applicable

CALCULATION DATA**PRELIMINARY CALCULATIONS**

Shell Analysis Thickness eas

eas = en - c =18-0=

18.000 mm

Nozzle Analysis Thickness eab

eab = enb - cn - NegDev =5-0-0.5=

4.5000 mm

dib = deb - 2 * eab =17-2*4.5=

8.0000 mm

Min.Nozzle Thk.Based on Internal Pressure ebp

ebp = P * deb / (2 * fb * z + P)

=3.3*17/(2*132*1+3.3)=

0.2100 mm

Min.Nozzle Thk. ebp=0.21 <= eab=4.5[mm]**4.6%****OK**

Limit of Reinforcement Along Nozzle

Ibo = MIN(0.8 * Sqr((dib + eab) * eab), ho)

(10.6-8)

=MIN(0.8*Sqr((8+4.5)*4.5,)8)=

6.0000 mm

TOTAL AREA OF REINFORCEMENT AVAILABLE IN THE NOZZLE A

A = Ibo * (eab - ebp) =6*(4.5-0.21)=

25.74 mm²

A = MIN(A , A * fb / fs)

(10.6-7)

=MIN(25.74,25.74*132/209.33)=

16.23 mm²

deq = dib - 2 * A / eas (10.6-5) =8-2*16.23/18=

6.1965 mm**10.6 PIERCED CIRCULAR FLAT ENDS**

Calculation Coefficient for Opening Reinforcement Y1 and Y2

Y2 = SQR(G / (G - deq)) (10.6-4) =SQR(167.5/(167.5-6.2))= 1.0190

Required Minimum Thickness of End due to Opening emin

emin = Y2 * eo + c (10.6-2) =1.02*14.13+0=

14.40 mm

Req.Unpierced End Thk. emin=14.4 <= en=18[mm]**79.9%****OK**

Weight of Nozzle: .0118kg Pad: 0kg

CALCULATION SUMMARY**Min.Nozzle Thk. ebp=0.21 <= eab=4.5[mm]****4.6%****OK**

Limit of Reinforcement Along Nozzle

Ibo = MIN(0.8 * Sqr((dib + eab) * eab), ho)

(10.6-8)

=MIN(0.8*Sqr((8+4.5)*4.5,)8)=

6.0000 mm

Required Minimum Thickness of End due to Opening emin

emin = Y2 * eo + c (10.6-2) =1.02*14.13+0=

14.40 mm

Req.Unpierced End Thk. emin=14.4 <= en=18[mm]**79.9%****OK**Volume:0.00 m³ Weight:0 kg (SG= 7.85)

Company Name -

Client :GÜVEN SOGUTMA

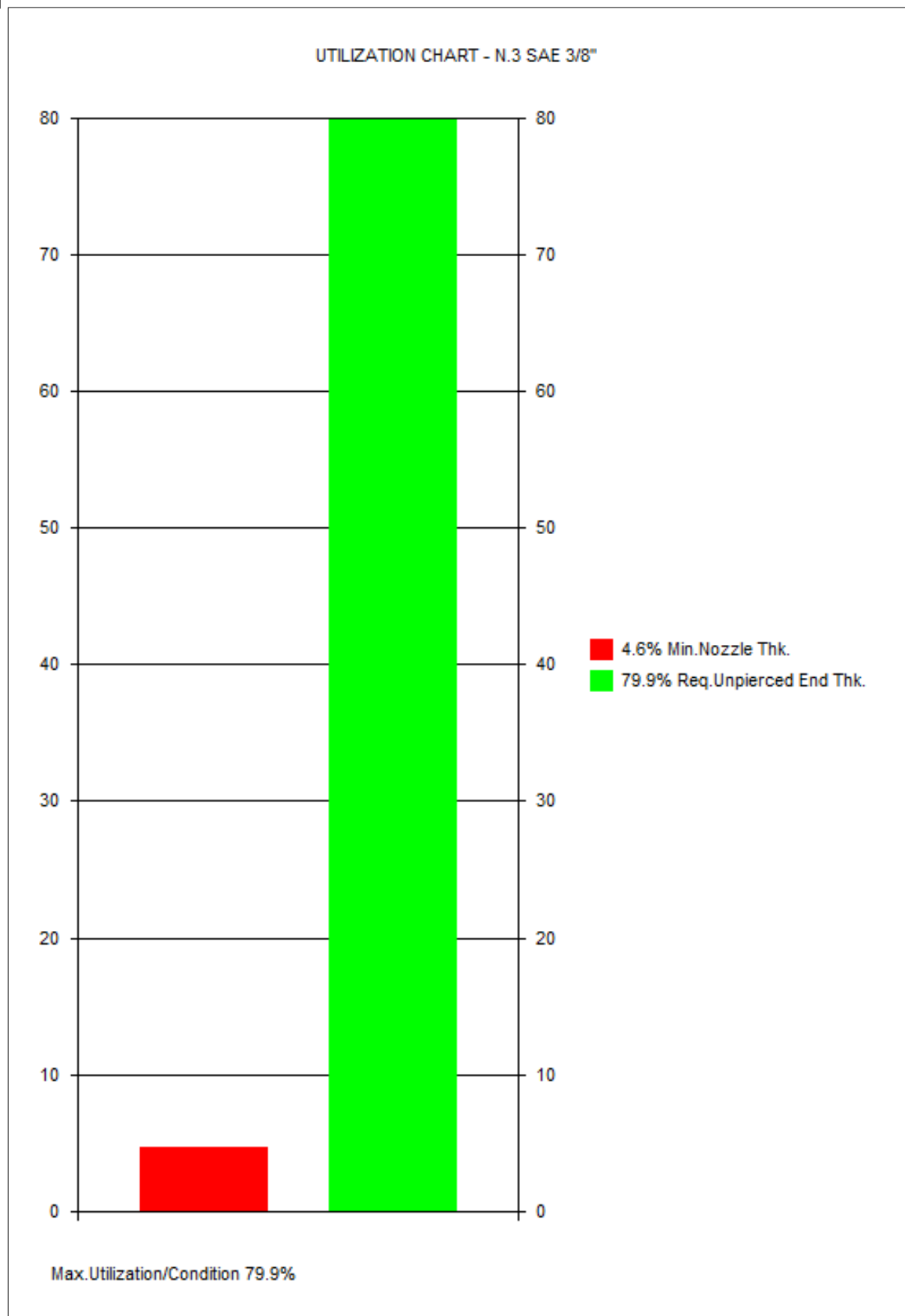
Vessel Tag No.:OS.F.33B.54.1

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EN13445:2014 Issue 5:2018+A5 - 9.5 ISOLATED OPENINGS IN SHELLS

N.3 Sae 3/8"

23 Feb. 2020 18:42 ConnID:E5.1



Company Name -

Client :GÜVEN SOGUTMA

Vessel Tag No.:OS.F.33B.54.1

Visual Vessel Design by Hexagon AB,Ver:19.0- Operator : Rev.:A

EN13445:2014 Issue 5:2018+A5 - 11.5 NARROW FACE GASKETED FLANGES

F.1 Shell Flange 23 Feb. 2020 18:40 ConnID:S1.1

INPUT DATA

COMPONENT ATTACHMENT/LOCATION

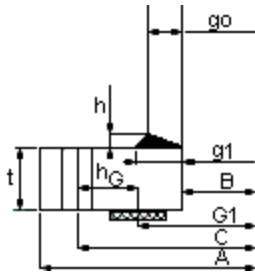
Attachment: S1.1 Cylindrical Shell Shell
Location: Along z-axis z1= 300
Flange Design Method: Section 11 - Taylor Forge

GENERAL DESIGN DATA

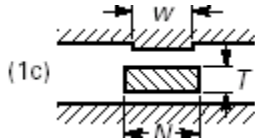
PROCESS CARD: General Design Data : Temp= 100°C, P=3.3000 MPa, c=0.0 mm
SPECIFIC DENSITY OF OPERATING LIQUID.....:SG 0.00
LIQUID HEAD.....:LH 0.00 mm
B: Pressure loading: Flange under internal pressure
EXTERNAL LOADS ON FLANGE (PD5500 ENQ 5500/123): NO
SPECIFY BOLT LOADS FROM 2nd./MATING FLANGE: NO

TYPE OF FLANGE AND GASKET FACING

A: Flange Standard: User Specified Flanges



C: Flange Type: RT Ring Type(Smooth or Stepped bore)



D: Flange Facing (Sketch/Description): 1c Tongue & Groove

SHELL/NOZZLE DATA

SHELL/NOZZLE SIZE & COMMENT: S1.1
EN 10216-3:2013, 1.0565 P355NH seamless tube, HT:N THK<=50mm 100'C
Rm=490 Rp=335 Rpt=294 fs=196 fs20=204.17 ftest=319.05 E=206067(N/mm2) ro=7.85
OUTSIDE DIAMETER OF SHELL/NOZZLE:Do 168.30 mm
WALL THICKNESS OF NOZZLE/SHELL(uncorroded).....:s1 3.0000 mm

FLANGE DATA

FLANGE HUB: Flange With Hub
REVERSE FLANGE: No (The bolts are located on the outside)
DESIGN METHOD: A) INTEGRAL FLANGE METHOD
FLANGE BORE: Stepped
INSIDE DIAMETER OF FLANGE corroded.....:B 162.50 mm
OUTSIDE DIAMETER OF FLANGE.....:A 218.00 mm
THICKNESS OF FLANGE(uncorroded).....:e 18.00 mm
THICKNESS OF FLANGE AT REDUCED SECTION.....:er 18.00 mm
CORROSION ALLOWANCE FOR FLANGE FACE.....:cf 0.00 mm
EN 10028-2:2017, 1.0473 P355GH plate and strip, HT:N THK<=40mm 100'C
Rm=510 Rp=345 Rpt=314 SFO=209.33 SFA=212.5 ftest=328.57 E=206067(N/mm2) ro=7.85

DATA FOR FLANGE HUB

LENGTH OF HUB.....:h 3.0000 mm
THICKNESS OF HUB AT BACK OF FLANGE corroded.....:g1 6.0000 mm
THICKNESS OF HUB AT SMALL END corroded.....:go 3.0000 mm
EN 10028-2:2017, 1.0473 P355GH plate and strip, HT:N THK<=16mm 100'C
Rm=510 Rp=355 Rpt=323 SHO=212.5 SHA=212.5 ftest=338.1 E=206067(N/mm2) ro=7.85

Company Name -

Client :GÜVEN SOGUTMA

Vessel Tag No.:OS.F.33B.54.1

Visual Vessel Design by Hexagon AB,Ver:19.0- Operator : Rev.:A

EN13445:2014 Issue 5:2018+A5 - 11.5 NARROW FACE GASKETED FLANGES

F.1 Shell Flange 23 Feb. 2020 18:40 ConnID:S1.1

BOLTING DATA

REDUCE SAFETY AGAINST ABUSE BY CAREFULLY CONTROLLING THE BOLTING-UP TORQUE: NO
BOLTING TORQUE CALCULATION: NO

NOMINAL BOLTING SIZE & COMMENT: M10x1.5 ;

EFFECTIVE BOLT AREA per bolt.....:Ae	58.00 mm ²
RECOMMENDED MINIMUM BOLT CENTER TO EDGE CLEARANCE...:Bce	14.00 mm
RECOMMENDED MINIMUM BOLT CENTER/RADIAL CLEARANCE....:Bcr	18.00 mm
DIAMETER OF BOLT HOLES IN FLANGE.....:d	12.00 mm
NUMBER OF BOLTS.....:n	10.00
BOLT-CIRCLE DIAMETER.....:C	193.00 mm

8.8 DIN 267 THK<=30mm 100'C

Rm=800 Rp=640 Rpt=590 Sb=196.67 Sa=200 ftest=300 (N/mm²)

NOTE: A PARTICULAR MATERIAL APPRAISAL(PMA) MAY BE REQUIRED FOR THIS MATERIAL.

GASKET DATA

Table H-1 Gasket factors m & y Facing:

Mineral Fiber 3.2 mm thick m=2.0 Y=11.0 2 1a,1b,1c,1d,4,5

OUTSIDE DIAMETER OF GASKET/RAISED FACE.....:Go 172.50 mm

GREATER VALUE OF INSIDE DIAMETER OF GASKET/FLANGE FACE:A1 162.50 mm

TEMA RGP-RCB-11.7 Include Additional Loads from Pass Partition Plate Gasket: NO

WELDING REQUIREMENTS TO EN 1708-1:2010

Comment(Optional):

Type of welded connection: Not Applicable

CALCULATION DATA

Large Diameter Stress Correction Factor K

k (D < 1000 mm) = 1 =1= 1.0000

GASKET DETAILS

b = MIN VALUE(2.52 * Sqr(bo), bo) = = 2.5000 mm

FLANGE LOADS

HD = 0.785 * B ^ 2 * p =0.785*162.5^2*3.3= 68.41 kN

H = 0.785 * G ^ 2 * p (11.5-5) =0.785*167.5^2*3.3= 72.68 kN

HG = (2 * PI * b * G * m) * p (11.5-6)

= (2*3.14*2.5*167.5*2)*3.3= 17.37 kN

HT = H - HD (11.5-11) =72679.72-68405.39= 4.2743 kN

MOMENT ARMS

hG = (C - G) / 2 (11.5-14) =(193-167.5)/2= 12.75 mm

hD = (C - B) / 2 (11.5-13) =(193-162.5)/2= 15.25 mm

hT = (2 * C - B - G) / 4 (11.5-15) =(2*193-162.5-167.5)/4= 14.00 mm

BOLT LOADS

Operating condition

Wop = H + HG (11.5-8) =72679.72+17365.15= 90.04 kN

Bolting up condition

Wamb = PI * b * G * y (11.5-7) =3.14*2.5*167.5*11= 14.47 kN

BOLTING AREA

Am1 = Wop / Sb =90044.87/196.67= 457.85 mm²

Am2 = Wamb / Sa =14470.96/200= 72.35 mm²

Required Bolting Area Am

Am = MAX(Am1 , Am2) =MAX(457.85,72.35)= 457.85 mm²

Available Bolting Area Ab

Ab (num.bolts*root area) = n * Ae =10*58= 580.00 mm²

Bolting Area Check Ab=580 >= Am=457.85[mm²]

78.9%

OK

W = 0.5 * (Ab + Am) * Sa (11.5-16) =0.5*(580+457.85)*200= 103.78 kN

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F.1 Shell Flange 23 Feb. 2020 18:40 ConnID:S1.1

FLANGE MOMENTS

$$Mop = HD * hD + HT * hT + HG * hG \quad (11.5-18)$$

$$=68405.39*15.25+4274.33*14+17365.15*12.75= \underline{1324.43 \text{ Nm}}$$

$$Mamb = W * hG \quad (11.5-17) =1.0378E05*12.75= \underline{1323.26 \text{ Nm}}$$

Bolt Spacing

$$Bs = C * PI / n =193*3.14/10= \underline{60.63 \text{ mm}}$$

Bolt Pitch Correction Factor

$$CF = \text{MAX}(\text{Sqr}(Bs / (2 * db + 6 * e / (m + 0.5))) , 1) \quad (11.5-20)$$

$$=\text{MAX}(\text{Sqr}(60.63/(2*10+6*18/(2+0.5))) , 1)= \underline{1.0000}$$

$$Mo = Mop * CF / B \quad (11.5-27) =1324.43*1/162.5= \underline{8.1503 \text{ Nm/mm}}$$

$$Ma = Mamb * CF / B \quad (11.5-26) =1323.26*1/162.5= \underline{8.1431 \text{ Nm/mm}}$$

SHAPE CONSTANTS

$$K = A / B \quad (11.5-21) =218/162.5= \underline{1.3415}$$

$$lo = \text{SQR}(B * go) \quad (11.5-22) =\text{SQR}(162.5*3)= \underline{22.08}$$

$$h/lo= 0.136 \quad K=A/B= 1.342 \quad g1/go= 2.000$$

VALUES FROM FIGURES 11.5-4 to 8

$$\text{BetaT} = 1.780 \quad \text{BetaZ} = 3.501 \quad \text{BetaY} = 6.764 \quad \text{BetaU} = 7.433$$

$$\text{BetaF} = 0.900 \quad \text{BetaV} = 0.410 \quad \text{phi} = 3.044$$

$$\text{lamda} = (e*\text{BetaF}+lo)/(\text{BetaT}*lo)+e^3*\text{BetaV}/(\text{BetaU}*lo*go^2)$$

$$=(18*0.8997+22.08)/(1.78*22.08)+18^3*0.41/(7.433*22.08*3^2)= \underline{2.5925}$$

OPERATING CONDITION

$$M = Mo =8.15= \underline{8.1503 \text{ Nm/mm}}$$

11.5.4.1 Flange Stresses with Flange Thickness e= 18 mm

Longitudinal Hub Stress

$$\text{SigH} = \text{phi} * M / (\text{lamda} * g1 ^ 2) \quad (11.5-32)$$

$$=3.04*8.15/(2.59*6^2)= \underline{265.82 \text{ N/mm}^2}$$

Radial Flange Stress

$$\text{Sigr} = (1.333 * e * \text{BetaF} + lo) * M / (\text{lamda} * e ^ 2 * lo) \quad (11.5-33)$$

$$=(1.333*18*0.8997+22.08)*8.15/(2.59*18^2*22.08)= \underline{19.19 \text{ N/mm}^2}$$

Tangential Flange Stress

$$\text{SigTeta} = \text{BetaY}*M/e^2-\text{Sigr}*(K^2+1)/(K^2-1) \quad (11.5-34)$$

$$=6.764*8.15/18^2-19.19*(1.34^2+1)/(1.34^2-1)= \underline{102.97 \text{ N/mm}^2}$$

11.5.4.2 Stress Limits

Hub Stress $k*\text{SigH}=265.82 \leq 1.5 * \text{MIN}(f;fH)=314.[\text{N/mm}^2]$ (11.5-90)	84.6%	OK
Radial Stress $k*\text{SigR}=19.19 \leq f=209.33[\text{N/mm}^2]$ (11.5-91)	9.1%	OK
Tangential Stress $k*\text{SigTeta}=102.97 \leq f=209.33[\text{N/mm}^2]$ (11.5-92)	49.1%	OK
Radial+Hub Stress $0.5*k*(\text{SigH}+\text{SigR})=142.5 \leq f=209.33[\text{N/mm}^2]$ (11.5-93)	68.0%	OK
Tangential+Hub Stress $0.5*k*(\text{SigH}+\text{SigTeta})=184.39 \leq f=209.33[\text{N/mm}^2]$ (11.5-94)	88.0%	OK

BOLTING UP CONDITION

$$M = Ma =8.14= \underline{8.1431 \text{ Nm/mm}}$$

11.5.4.1 Flange Stresses with Flange Thickness e= 18 mm

Longitudinal Hub Stress

$$\text{SigH} = \text{phi} * M / (\text{lamda} * g1 ^ 2) \quad (11.5-32)$$

$$=3.04*8.14/(2.59*6^2)= \underline{265.58 \text{ N/mm}^2}$$

Radial Flange Stress

$$\text{Sigr} = (1.333 * e * \text{BetaF} + lo) * M / (\text{lamda} * e ^ 2 * lo) \quad (11.5-33)$$

$$=(1.333*18*0.8997+22.08)*8.14/(2.59*18^2*22.08)= \underline{19.17 \text{ N/mm}^2}$$

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EN13445:2014 Issue 5:2018+A5 - 11.5 NARROW FACE GASKETED FLANGES

F.1 Shell Flange 23 Feb. 2020 18:40 ConnID:S1.1

Tangential Flange Stress

$$\text{SigTeta} = \text{BetaY} * \text{M} / \text{e}^2 - \text{Sigr} * (\text{K}^2 + 1) / (\text{K}^2 - 1) \quad (11.5-34)$$

$$= 6.764 * 8.14 / 18^2 - 19.17 * (1.34^2 + 1) / (1.34^2 - 1) = 102.88 \text{ N/mm}^2$$

11.5.4.2 Stress Limits

Hub Stress $k * \text{SigH} = 265.58 \leq 1.5 * \text{MIN}(f; f_H) = 318.75 [\text{N/mm}^2]$ (11.5-90)	83.3%	OK
Radial Stress $k * \text{SigR} = 19.17 \leq f = 212.5 [\text{N/mm}^2]$ (11.5-91)	9.0%	OK
Tangential Stress $k * \text{SigTeta} = 102.88 \leq f = 212.5 [\text{N/mm}^2]$ (11.5-92)	48.4%	OK
Radial+Hub Stress $0.5 * k * (\text{SigH} + \text{SigR}) = 142.38 \leq f = 212.5 [\text{N/mm}^2]$ (11.5-93)	67.0%	OK
Tangential+Hub Stress $0.5 * k * (\text{SigH} + \text{SigTeta}) = 184.23 \leq f = 212.5 [\text{N/mm}^2]$ (11.5-94)	86.6%	OK

EN13445-5;10.2.3.3 REQUIRED MIN.HYDROSTATIC TEST PRESSURE:Ptmin

NEW AT AMBIENT TEMP. FOR TEST GROUPS 1, 2 and 3

$$\text{Ptmin} = 1.25 * \text{Pd} * f_{20} / f = 1.25 * 3.3 * 212.5 / 209.33 = 4.1875 \text{ MPa}$$

$$\text{Ptmin} = 1.43 * \text{Pd} = 1.43 * 3.3 = 4.7190 \text{ MPa}$$

Test Pressure $\text{Ptmin} = 4.72 \leq \text{Pmax} = 5.887 [\text{MPa}]$	80.1%	OK
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PRESSURE AND TORQUE SUMMARY

Table PRESSURE AND TORQUE SUMMARY FOR F.1 :

Description	Temp(C)	P(MPa)	Limited By	Min.Req.Total Bolt Force(kN)
Design Pressure(corroded)	100	3.30	Tangential+Hub Stress	90.04
Max.Allow.Pressure(corroded)	100	3.75	Tangential+Hub Stress	102.29
Max.Allow.Pressure(corroded)	Ambient	3.80	Tangential+Hub Stress	103.79
Max.Allow.Test Pressure(corroded)	Ambient	5.89	Tangential+Hub Stress	160.64
Required Test Pressure	Ambient	4.19	Tangential+Hub Stress	114.26

The nominal Force and Torque values are based on the following bolting up method:

CALCULATION SUMMARY

BOLTING AREA

Bolting Area Check $\text{Ab} = 580 \geq \text{Am} = 457.85 [\text{mm}^2]$	78.9%	OK
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OPERATING CONDITION

11.5.4.1 Flange Stresses with Flange Thickness $e = 18 \text{ mm}$

Longitudinal Hub Stress

$$\text{SigH} = \text{phi} * \text{M} / (\text{lamda} * \text{gl}^2) \quad (11.5-32)$$

$$= 3.04 * 8.15 / (2.59 * 6^2) = 265.82 \text{ N/mm}^2$$

Radial Flange Stress

$$\text{Sigr} = (1.333 * e * \text{BetaF} + \text{lo}) * \text{M} / (\text{lamda} * e^2 * \text{lo}) \quad (11.5-33)$$

$$= (1.333 * 18 * 0.8997 + 22.08) * 8.15 / (2.59 * 18^2 * 22.08) = 19.19 \text{ N/mm}^2$$

Tangential Flange Stress

$$\text{SigTeta} = \text{BetaY} * \text{M} / \text{e}^2 - \text{Sigr} * (\text{K}^2 + 1) / (\text{K}^2 - 1) \quad (11.5-34)$$

$$= 6.764 * 8.15 / 18^2 - 19.19 * (1.34^2 + 1) / (1.34^2 - 1) = 102.97 \text{ N/mm}^2$$

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11.5.4.2 Stress Limits

Hub Stress $k \cdot \text{SigH} = 265.82 \leq 1.5 \cdot \text{MIN}(f; f_H) = 314$ [N/mm ²] (11.5-90)	84.6%	OK
Radial Stress $k \cdot \text{SigR} = 19.19 \leq f = 209.33$ [N/mm ²] (11.5-91)	9.1%	OK
Tangential Stress $k \cdot \text{SigTeta} = 102.97 \leq f = 209.33$ [N/mm ²] (11.5-92)	49.1%	OK
Radial+Hub Stress $0.5 \cdot k \cdot (\text{SigH} + \text{SigR}) = 142.5 \leq f = 209.33$ [N/mm ²] (11.5-93)	68.0%	OK
Tangential+Hub Stress $0.5 \cdot k \cdot (\text{SigH} + \text{SigTeta}) = 184.39 \leq f = 209.33$ [N/mm ²] (11.5-94)	88.0%	OK

BOLTING UP CONDITION**11.5.4.1 Flange Stresses with Flange Thickness $e = 18$ mm**

Longitudinal Hub Stress

$$\text{SigH} = \frac{\phi \cdot M}{(\lambda \cdot g_1 \cdot e^2)} \quad (11.5-32)$$

$$= \frac{3.04 \cdot 8.14}{(2.59 \cdot 18^2)} = 265.58 \text{ N/mm}^2$$

Radial Flange Stress

$$\text{SigR} = \frac{(1.333 \cdot e \cdot \text{BetaF} + l_0) \cdot M}{(\lambda \cdot e^2 \cdot l_0)} \quad (11.5-33)$$

$$= \frac{(1.333 \cdot 18 \cdot 0.8997 + 22.08) \cdot 8.14}{(2.59 \cdot 18^2 \cdot 22.08)} = 19.17 \text{ N/mm}^2$$

Tangential Flange Stress

$$\text{SigTeta} = \frac{\text{BetaY} \cdot M}{e^2 - \text{SigR}} \cdot \frac{(K^2 + 1)}{(K^2 - 1)} \quad (11.5-34)$$

$$= \frac{6.764 \cdot 8.14}{18^2 - 19.17} \cdot \frac{(1.34^2 + 1)}{(1.34^2 - 1)} = 102.88 \text{ N/mm}^2$$

11.5.4.2 Stress Limits

Hub Stress $k \cdot \text{SigH} = 265.58 \leq 1.5 \cdot \text{MIN}(f; f_H) = 318.75$ [N/mm ²] (11.5-90)	83.3%	OK
Radial Stress $k \cdot \text{SigR} = 19.17 \leq f = 212.5$ [N/mm ²] (11.5-91)	9.0%	OK
Tangential Stress $k \cdot \text{SigTeta} = 102.88 \leq f = 212.5$ [N/mm ²] (11.5-92)	48.4%	OK
Radial+Hub Stress $0.5 \cdot k \cdot (\text{SigH} + \text{SigR}) = 142.38 \leq f = 212.5$ [N/mm ²] (11.5-93)	67.0%	OK
Tangential+Hub Stress $0.5 \cdot k \cdot (\text{SigH} + \text{SigTeta}) = 184.23 \leq f = 212.5$ [N/mm ²] (11.5-94)	86.6%	OK

EN13445-5;10.2.3.3 REQUIRED MIN.HYDROSTATIC TEST PRESSURE:Ptmin

NEW AT AMBIENT TEMP. FOR TEST GROUPS 1, 2 and 3

$$\text{Ptmin} = 1.25 \cdot \text{Pd} \cdot \frac{f_{20}}{f} = 1.25 \cdot 3.3 \cdot \frac{212.5}{209.33} = 4.1875 \text{ MPa}$$

$$\text{Ptmin} = 1.43 \cdot \text{Pd} = 1.43 \cdot 3.3 = 4.7190 \text{ MPa}$$

Test Pressure $\text{Ptmin} = 4.72 \leq \text{Ptmax} = 5.887$ [MPa]	80.1%	OK
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Volume:0.0004345 m³ Weight:2 kg (SG= 7.85)

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