

# Company Name -

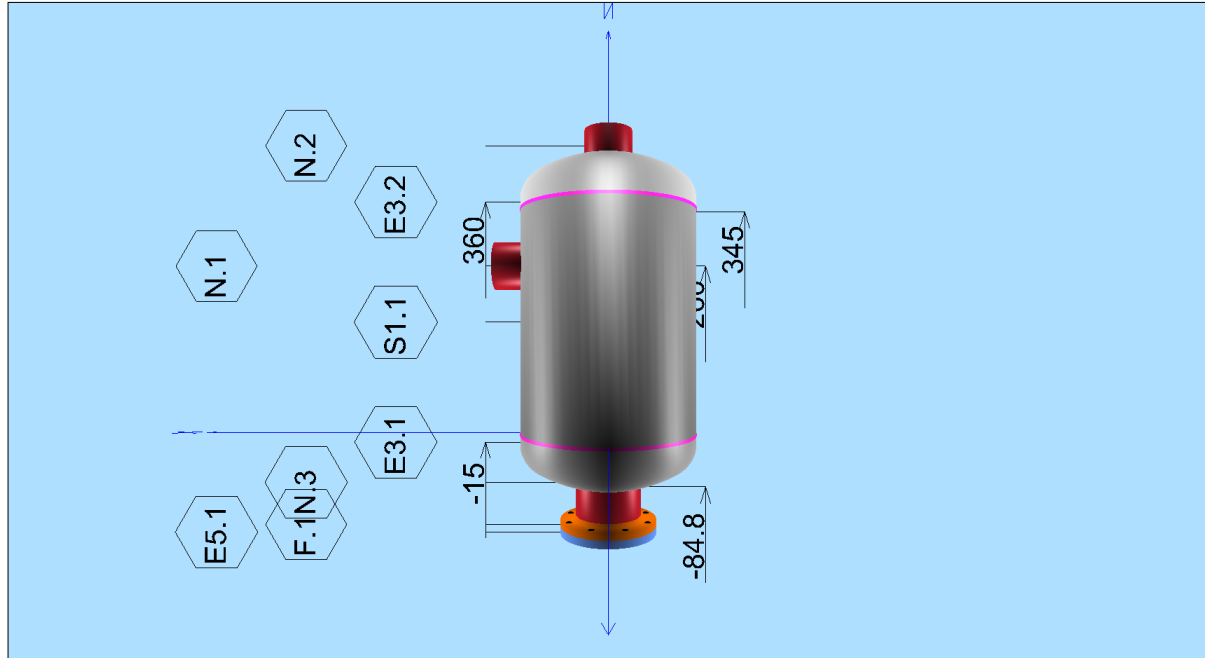
Client :GÜVEN SOGUTMA

Vessel Tag No.:OS.HF.33B.66.1

Visual Vessel Design by Hexagon PPM,Ver:20.0 Operator : Rev.:A

## (0) Drawing

3D View of Vessel (alter by using the Save User Specified View command)



## Design Data & Process Information

Description	Units	Design Data
Process Card		General Design Data
Design Code & Specifications		EN13445 TG = 3b
Internal Design Pressure (MPa)	MPa	3.3
External Design Pressure (MPa)	MPa	
Hydrotest Pressure (MPa)	MPa	
Maximum Design Temperature (°C)	°C	130
Minimum Design Temperature (°C)	°C	-20
Operating Temperature (°C)	°C	
Corrosion Allowance (mm)	mm	0.5
Content of Vessel		
Specific Density of Oper.Liq		
Normal Liquid Level NLL (mm)	mm	

## Test Pressure

### TEST PRESSURE OF VESSEL - NEW & COLD - VERTICAL

Design Pressure..... : 3.300 MPa

Design Temperature..... : 130.0 C

ID	Description	Pdesign	PtMax	PtMin	Wat.Head	PtTop	PtTopMax
E3.1	Torispherical End-Bottom Head	3.300	9.277	4.261	0.005	4.261	9.271
E3.2	Torispherical End-Upper Head	3.300	9.277	4.261	0.001	4.261	9.276
E5.1	Bolted Flat End-Cover Flange	3.300	7.082	4.261	0.006	4.261	7.076
F.1	RT - Flange-Ring Flange	3.300	7.197	NA	0.006	NA	7.191
N.1	Nozzle,Seamless Pipe-Inlet	3.300	6.558	NA	0.003	NA	6.554
N.2	Nozzle,Seamless Pipe-Outlet	3.300	7.726	NA	0.000	NA	7.726
N.3	Nozzle,Seamless Pipe-Float Shell	3.300	6.856	NA	0.006	NA	6.851
S1.1	Cylindrical Shell-Shell	3.300	10.164	4.156	0.005	4.156	10.159

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PtReq = MAX(MIN(PtTop), 1.43\*p)= 4.7190 MPa (EN13445-5, 10.2.3.3.1-1 & 2)

## HYDRO-TEST

REQUIRED TEST PRESSURE AT TOP OF VESSEL PtReq(Hydro Test) .....: 4.7190 MPa  
MAXIMUM TEST PRESSURE AT TOP OF VESSEL PtLim(Hydro Test) .....: 6.5542 MPa

## PNEUMATIC TEST

REQUIRED TEST PRESSURE AT TOP OF VESSEL PtReq(Pneumatic Test) ...: 4.7190 MPa  
MAXIMUM TEST PRESSURE AT TOP OF VESSEL PtLim(Pneumatic Test) ...: 6.5576 MPa

Note : Other components may limit Ptlim than the ones checked above.

## TEST PRESSURE OF VESSEL - NEW & COLD - HORIZONTAL

Design Pressure.....: 3.300 MPa

Design Temperature.....: 130.0 C

ID	Description	Pdesign	PtMax	PtMin	Wat.Head	PtTop	PtTopMax
E3.1	Torispherical End-Bottom Head	3.300	9.277	4.261	0.002	4.261	9.275
E3.2	Torispherical End-Upper Head	3.300	9.277	4.261	0.003	4.261	9.273
E5.1	Bolted Flat End-Cover Flange	3.300	7.082	4.261	0.002	4.261	7.080
F.1	RT - Flange-Ring Flange	3.300	7.197	NA	0.002	NA	7.195
N.1	Nozzle,Seamless Pipe-Inlet	3.300	6.558	NA	0.001	NA	6.556
N.2	Nozzle,Seamless Pipe-Outlet	3.300	7.726	NA	0.002	NA	7.724
N.3	Nozzle,Seamless Pipe-Float Shell	3.300	6.856	NA	0.002	NA	6.854
S1.1	Cylindrical Shell-Shell	3.300	10.164	4.156	0.003	4.156	10.160

PtReq = MAX(MIN(PtTop), 1.43\*p)= 4.7190 MPa (EN13445-5, 10.2.3.3.1-1 & 2)

## HYDRO-TEST

REQUIRED TEST PRESSURE AT TOP OF VESSEL PtReq(Hydro Test) .....: 4.7190 MPa  
MAXIMUM TEST PRESSURE AT TOP OF VESSEL PtLim(Hydro Test) .....: 6.5564 MPa

## PNEUMATIC TEST

REQUIRED TEST PRESSURE AT TOP OF VESSEL PtReq(Pneumatic Test) ...: 4.7190 MPa  
MAXIMUM TEST PRESSURE AT TOP OF VESSEL PtLim(Pneumatic Test) ...: 6.5576 MPa

Note : Other components may limit Ptlim than the ones checked above.

## NOMENCLATURE:

Pdesign- is the design pressure including liquid head at the part under consideration.

PtMax - is the maximum allowed test pressure determined at the part under consideration.

PtMin - is the required test pressure determined at the part under consideration.

Wat.Head - is the water head during hydrotesting at the part under consideration.

PtBot - is the required test pressure at bottom of the vessel, for the part under consideration.

PtTop - is the required test pressure at top of the vessel, for the part under consideration.

PtTopMax - is the maximum test pressure allowed at top of the vessel, for the part under consideration.

PtReq - is the required minimum test pressure (minimum value of PtTop) at top of vessel for the listed components.

PtLim - is the maximum allowed test pressure (minimum value for PtTopMax) at top of vessel for the listed components.

EN13445-5 10.2.3.3.8 Pressure of vessels under test shall be gradually increased to a value of approximately 50 % of the specified test pressure, thereafter the pressure shall be increased in stages of approximately 10 % of the specified test pressure until this is reached. The required test pressure shall be maintained for not less than 30 min. At no stage shall the vessel be approached for close examination until the pressure has been positively reduced by at least 10 % to a level lower than that previously attained. The pressure shall be maintained at the specified close examination level for a sufficient length of time to permit a visual inspection to be made of all surfaces and joints.

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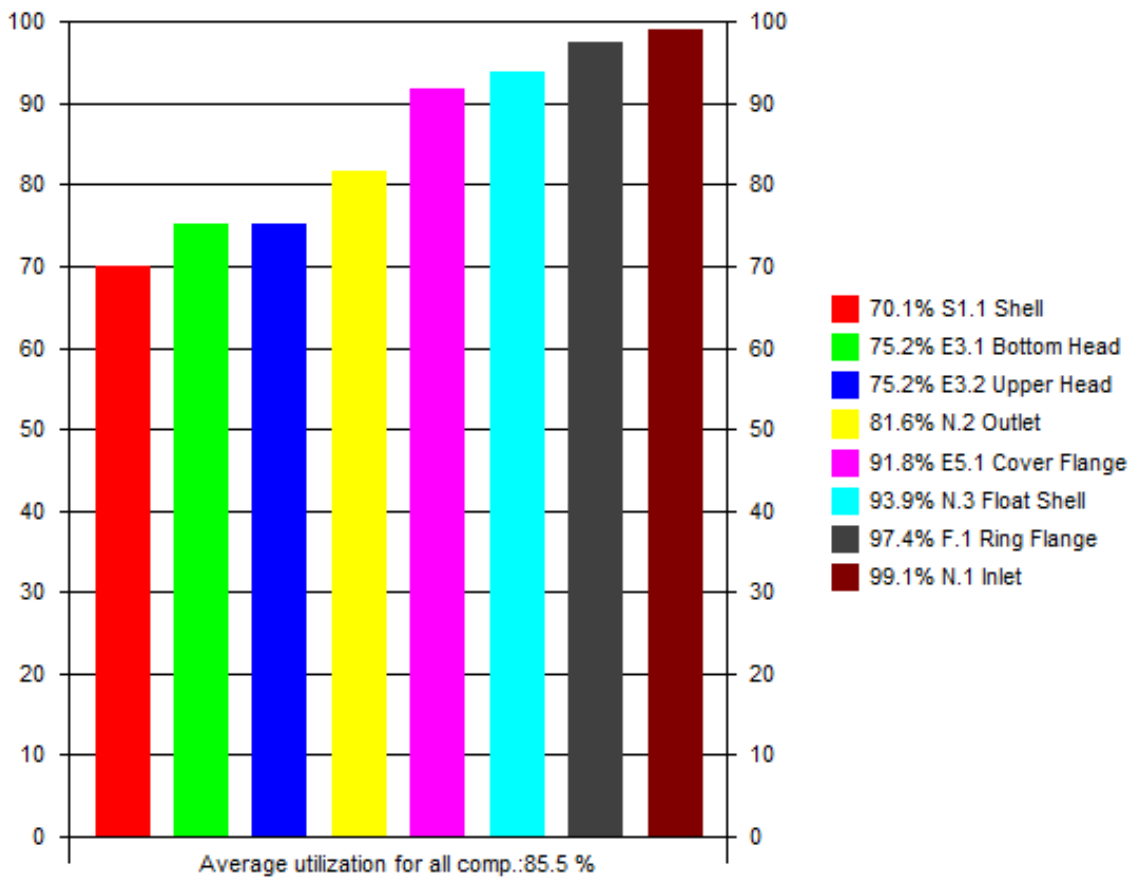
Visual Vessel Design by Hexagon PPM,Ver:20.0 Operator :

Rev.:A

## Utilization Chart

Utilization Chart

MPONENTS UTILIZATION CHART - Client :GÜVEN SOGUTMA Vessel Tag No.:OS.HF.33B.6



Maximum Utilization of 99.1% for Component N.1 Inlet - VVD by Hexagon PPM, Ver:20.0

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Vessel Tag No.:OS.HF.33B.66.1

Visual Vessel Design by Hexagon PPM,Ver:20.0 Operator : Rev.:A

EN13445:2014 Issue 5:2018+A5 - 7.4.2 CYLINDRICAL SHELL

S1.1 Shell

17 Dec. 2020 18:41

## INPUT DATA

### COMPONENT ATTACHMENT/LOCATION

### GENERAL DESIGN DATA

PRESSURE LOADING: Design Component for Internal Pressure Only

PROCESS CARD:

General Design Data : Temp= 100°C, P=3.3000 MPa, c=0.5 mm, Pext=0.0000 MPa

SPECIFIC DENSITY OF OPERATING LIQUID.....:SG 0.00

LIQUID HEAD.....:LH 0.00 mm

### SHELL DATA

CYLINDER FABRICATION: Welded Pipe

WELD JOINT COEFFICIENT: Testing Group 1 (z=1.0)

NEGATIVE TOLERANCE: Negative tolerance specified in % of nominal thickness

EN 10217-3:2002/A1:05, 1.0565 P355NH welded tube, HT:N THK<=20mm 100'C

Rm=490 Rp=355 Rpt=304 f=202.67 f20=204.17 ftest=338.1 E=206067(N/mm2) ro=7.85

OUTSIDE DIAMETER OF SHELL.....:De 273.00 mm

LENGTH OF CYLINDRICAL PART OF SHELL.....:Lcyl 345.00 mm

NOMINAL WALL THICKNESS (uncorroded).....:en 4.5000 mm

NEGATIVE TOLERANCE/THINNING ALLOWANCE.....: 10.00 %

Split shell into several shell courses and include welding information: NO

### WELDING REQUIREMENTS TO EN 1708-1:2010

Comment(Optional):

Type of welded connection: Not Applicable

## CALCULATION DATA

### 7.4.2 - CYLINDRICAL SHELLS UNDER INTERNAL PRESSURE

Required Minimum Shell Thickness Excl.Allow. emin :

$$emin = De * P / (2 * f * z + P) \quad (7.4-2)$$
$$= 273 * 3.3 / (2 * 202.67 * 1 + 3.3) = 2.2046 \text{ mm}$$

Required Minimum Shell Thickness Incl.Allow. :

$$emina = emin + c + NegDev = 2.2 + 0.5 + 0.45 = 3.1546 \text{ mm}$$

Analysis Thickness

$$ea = en - c - NegDev = 4.5 - 0.5 - 0.45 = 3.5500 \text{ mm}$$

»7.4.1 Cond.of Applicability  $emin/De=0.0081 \leq 0.16$ « » OK«

Internal Pressure $emina=3.15 \leq en=4.5$ [mm]	70.1%	OK
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### MAXIMUM ALLOWABLE WORKING PRESSURE MAWP :

Inside Diameter of Shell

$$Di = De - 2 * ea = 273 - 2 * 3.55 = 265.90 \text{ mm}$$

Mean Diameter of Shell

$$Dm = (De + Di) / 2 = (273 + 265.9) / 2 = 269.45 \text{ mm}$$

MAWP HOT & CORR. (Corroded condition at design temp.)

$$MAWPHC = 2 * f * z * ea / Dm = 2 * 202.67 * 1 * 3.55 / 269.45 = 5.3403 \text{ MPa}$$

MAWP NEW & COLD (Uncorroded condition at ambient temp.)

$$MAWPNC = 2 * f20 * z * (ea + c) / Dm$$
$$= 2 * 204.17 * 1 * (3.55 + 0.5) / 269.45 = 6.1376 \text{ MPa}$$

### MAX TEST PRESSURE (Uncorroded cond.at ambient temp.)

Ptmax = 2 \* ftest \* ztest \* (ea + c) / Dm

$$= 2 * 338.1 * 1 * (3.55 + 0.5) / 269.45 = 10.16 \text{ MPa}$$

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EN13445:2014 Issue 5:2018+A5 - 7.4.2 CYLINDRICAL SHELL

S1.1 Shell

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### EN13445-5;10.2.3.3 REQUIRED MIN.HYDROSTATIC TEST PRESSURE:Ptmin

NEW AT AMBIENT TEMP. FOR TEST GROUPS 1, 2 and 3

$$Ptmin = 1.25 * Pd * f_{20} / f = 1.25 * 3.3 * 204.17 / 202.67 = 4.1555 \text{ MPa}$$

$$Ptmin = 1.43 * Pd = 1.43 * 3.3 = 4.7190 \text{ MPa}$$

**Test Pressure Ptmin=4.72 <= Pmax=10.16[MPa]****46.4%****OK**

### MAXIMUM DIAMETER OF UNREINFORCED OPENING IN SHELL

Inside Radius of Shell

$$ris = Di / 2 \text{ (9.5-3)} = 265.9 / 2 = 132.95 \text{ mm}$$

Length of Shell Contributing to Reinforcement

$$Is = \text{Sqr}((2 * ris + ea) * ea) \text{ (9.5-2)}$$

$$= \text{Sqr}((2 * 132.95 + 3.55) * 3.55) = 30.93 \text{ mm}$$

Maximum Diameter of Unreinforced Opening in Shell Checked to Rules in Section 9

$$dmax1 = \text{MIN}(0.5 * Di, (ea * Is * (f - 0.5 * P) / (P - ris * Is)) / (0.5 * ris + 0.5 * ea)) \text{ (9.5-7,22,23)}$$

$$= \text{MIN}(0.5 * 265.9, (3.55 * 30.93 * (202.67 - 0.5 * 3.3) / (3.3 - 132.95 * 30.93)) / (0.5 * 132.95 + 0.5 * 3.55)) = 37.75 \text{ mm}$$

Maximum diameter of Opening Not Requiring Reinforcement Check

$$dmax2 = 0.15 * \text{Sqr}((2 * ris + ea) * ea) \text{ (9.5-18)}$$

$$= 0.15 * \text{Sqr}((2 * 132.95 + 3.55) * 3.55) = 4.6392 \text{ mm}$$

Maximum Diameter of Unreinforced Opening

$$dmax = \text{MAX}(dmax1, dmax2) = \text{MAX}(37.75, 4.64) = 37.75 \text{ mm}$$

## CALCULATION SUMMARY

### 7.4.2 - CYLINDRICAL SHELLS UNDER INTERNAL PRESSURE

Required Minimum Shell Thickness Excl.Allow. emin :

$$emin = De * P / (2 * f * z + P) \text{ (7.4-2)}$$

$$= 273 * 3.3 / (2 * 202.67 * 1 + 3.3) = 2.2046 \text{ mm}$$

Required Minimum Shell Thickness Incl.Allow. :

$$emina = emin + c + \text{NegDev} = 2.2 + 0.5 + 0.45 = 3.1546 \text{ mm}$$

**Internal Pressure emina=3.15 <= en=4.5[mm]****70.1%****OK**

### MAX TEST PRESSURE (Uncorroded cond.at ambient temp.)

$$P_{tmax} = 2 * f_{test} * z_{test} * (ea + c) / D_m$$

$$= 2 * 338.1 * 1 * (3.55 + 0.5) / 269.45 = 10.16 \text{ MPa}$$

### EN13445-5;10.2.3.3 REQUIRED MIN.HYDROSTATIC TEST PRESSURE:Ptmin

NEW AT AMBIENT TEMP. FOR TEST GROUPS 1, 2 and 3

$$Ptmin = 1.25 * Pd * f_{20} / f = 1.25 * 3.3 * 204.17 / 202.67 = 4.1555 \text{ MPa}$$

$$Ptmin = 1.43 * Pd = 1.43 * 3.3 = 4.7190 \text{ MPa}$$

**Test Pressure Ptmin=4.72 <= Pmax=10.16[MPa]****46.4%****OK**

### MAXIMUM DIAMETER OF UNREINFORCED OPENING IN SHELL

Maximum Diameter of Unreinforced Opening

$$dmax = \text{MAX}(dmax1, dmax2) = \text{MAX}(37.75, 4.64) = 37.75 \text{ mm}$$

Volume:0.0192 m3 Weight:10.3 kg (SG= 7.85 )

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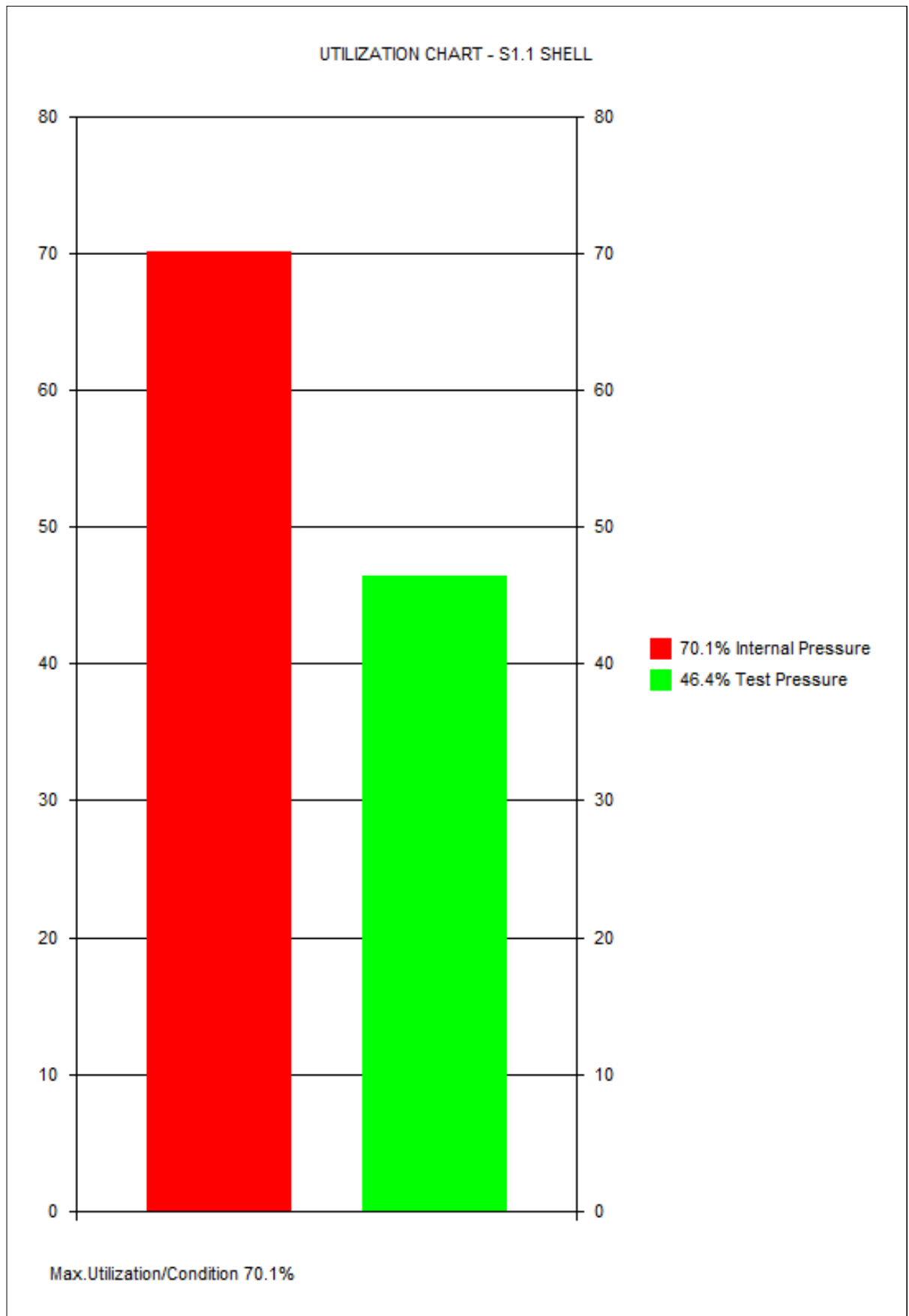
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EN13445:2014 Issue 5:2018+A5 - 7.4.2 CYLINDRICAL SHELL

S1.1 Shell

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EN13445:2014 Issue 5:2018+A5 - 7.5 DOMED ENDS

E3.1 Bottom Head 17 Aug. 2023 11:33 ConnID:S1.1

## INPUT DATA

### COMPONENT ATTACHMENT/LOCATION

Attachment: S1.1 Cylindrical Shell Shell  
Location: Along z-axis zo= 0

### GENERAL DESIGN DATA

PRESSURE LOADING: Design Component for Internal Pressure Only

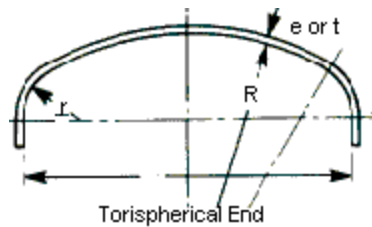
PROCESS CARD:

General Design Data : Temp= 130°C, P=3.3000 MPa, c=0.5 mm, Pext=0.0000 MPa

SPECIFIC DENSITY OF OPERATING LIQUID.....:SG 0.00

LIQUID HEAD.....:LH 0.00 mm

### DIMENSIONS OF END



Type of Torispherical End: Dished End KORBOGEN DIN 28013-28014/SMS 482

WELD JOINT COEFFICIENT: Unwelded Component(z=1.0)

OUTSIDE DIAMETER OF CYLINDRICAL FLANGE OF END.....:De 273.00 mm

LENGTH OF CYLINDRICAL FLANGE OF END.....:Lcyl 15.00 mm

NEGATIVE TOLERANCE/THINNING ALLOWANCE.....:th 0.3000 mm

NOMINAL THICKNESS OF HEAD/END (uncorroded).....:en 4.0000 mm

Include calculation of forming during fabrication to EN13445-4 Section 9.: NO

### MATERIAL DATA FOR END

EN 10028-2:2017, 1.0473 P355GH plate and strip, HT:N THK<=16mm 130'C

Rm=510 Rp=355 Rpt=308.6 f=205.73 f20=212.5 ftest=338.1 E=203868(N/mm2) ro=7.85

Material & Delivery Form: Cold Spun Seamless Austenitic Stainless Steel

### NOZZLES IN KNUCKLE REGION TO SECTION 7.7

Nozzles In Knuckle Region: NO

### WELDING REQUIREMENTS TO EN 1708-1:2010

Comment(Optional):

Type of welded connection: Not Applicable

## CALCULATION DATA

### 7.5.3 - TORISPHERICAL ENDS UNDER INTERNAL PRESSURE

#### 7.5.3.2 Required Minimum End Thickness

Required Thickness of End to Limit Membrane Stress in Central Part

$$e_s = P * R / (2 * f * z - 0.5 * P) \quad (7.5-1)$$

$$= 3.3 * 218.4 / (2 * 205.73 * 1 - 0.5 * 3.3) = 1.7587 \text{ mm}$$

$$f_b = R_{pt} / 1.5 * 1.6 \quad (7.5-5) = 308.6 / 1.5 * 1.6 = 329.17 \text{ N/mm}^2$$

Required Thickness of Knuckle to Avoid Plastic Buckling

$$e_b = (0.75 * R + 0.2 * D_i) * ((P / (111 * f_b)) * (D_i / r)^{0.825})^{(0.667)} \quad (7.5-3)$$

$$= (0.75 * 218.4 + 0.2 * 266) * ((3.3 / (111 * 329.17)) * (266 / 42.042)^{0.825})^{(0.667)}$$

$$= 1.2018 \text{ mm}$$

7.5.3.5 Formulas for Calculation of Factor Beta

$$Y = \text{MIN}(e_{min} / R, 0.04) \quad (7.5-9) = \text{MIN}(2.21 / 218.4, 0.04) = 0.0101$$

$$Z = \text{LOG}(1 / Y) \quad (7.5-10) = \text{LOG}(1 / 0.0101) = 1.9953$$

$$X = r / D_i \quad (7.5-11) = 42.042 / 268.58 = 0.1565$$

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EN13445:2014 Issue 5:2018+A5 - 7.5 DOMED ENDS

E3.1 Bottom Head 17 Aug. 2023 11:33 ConnID:S1.1

$$N = 1.006 - 1 / (6.2 + (90 * Y) ^ 4) \quad (7.5-12)$$

$$= 1.006 - 1 / (6.2 + (90 * 0.0101) ^ 4) = 0.8608$$

$$\text{Beta01} = N * (-0.1833 * Z^3 + 1.0383 * Z^2 - 1.2943 * Z + 0.837) \quad (7.5-15)$$

$$= 0.8608 * (-0.1833 * 2.^3 + 1.0383 * 2.^2 - 1.2943 * 2. + 0.837) = 0.8023$$

$$\text{Beta02} = \text{MAX}(0.5, 0.95 * (0.56 - 1.94 * Y - 82.5 * Y ^ 2)) \quad (7.5-17)$$

$$= \text{MAX}(0.5, 0.95 * (0.56 - 1.94 * 0.0101 - 82.5 * 0.0101^2)) = 0.5054$$

$$\text{beta} = 10 * ((0.2 - X) * \text{Beta01} + (X - 0.1) * \text{Beta02}) \quad (7.5-16)$$

$$= 10 * ((0.2 - 0.1565) * 0.8023 + (0.1565 - 0.1) * 0.5054) = 0.6344$$

Required Thickness of Knuckle to Avoid Axisymmetric Yielding

$$e_y = \text{beta} * P * (0.75 * R + 0.2 * D_i) / f \quad (7.5-2)$$

$$= 0.6344 * 3.3 * (0.75 * 218.4 + 0.2 * 268.58) / 205.73 = 2.2136 \text{ mm}$$

NOTE 3, since  $e_y(2.2) > 0.005 * D_i(1.3)$  it is NOT necessary to calculate/consider eb.

Required Minimum End Thickness Excl.Allow.  $e_{min}$  :

$$e_{min} = e_{min} = 2.21 = 2.2136 \text{ mm}$$

Required Minimum End Thickness Incl.Allow. :

$$e_{minA} = e_{min} + c + t_h = 2.21 + 0.5 + 0.3 = 3.0100 \text{ mm}$$

<b>Internal Pressure <math>e_{minA}=3.01 \leq e_n=4</math>[mm]</b>	<b>75.2%</b>	<b>OK</b>
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Analysis Thickness

$$e_a = e_n - c - t_h = 4 - 0.5 - 0.3 = 3.2000 \text{ mm}$$

Inside Diameter of Shell

$$D_i = D_e - 2 * (e_n - c) = 273 - 2 * (4 - 0.5) = 266.00 \text{ mm}$$

Mean Diameter of Shell

$$D_m = (D_e + D_i) / 2 = (273 + 266) / 2 = 269.50 \text{ mm}$$

### 7.5.3.4 - Required Minimum Thickness of Straight Cylindrical Flange

$$L_{lim} = 0.2 * \text{SQRT}(D_i * e_{min}) = 0.2 * \text{SQRT}(266 * 2.21) = 4.8531 \text{ mm}$$

Since  $L_{cyl} > L_{lim}$ , Required Thickness of Straight Cylindrical Flange to 7.4.2

Minimum Thickness of Straight Flange Excl. Allow.

$$e_{cyl} = P * D_i / (2 * f * z - P) \quad (7.4-1)$$

$$= 3.3 * 266 / (2 * 205.73 * 1 - 3.3) = 2.1506 \text{ mm}$$

Minimum Thickness of Straight Flange Incl.Corr. :

$$e_{cylA} = e_{cyl} + c = 2.15 + 0.5 = 2.6500 \text{ mm}$$

### 7.5.3.1 Conditions of Applicability - Torispherical Ends

»Geometry Check  $r=42.042 \leq 0.2 * D_i=53.2$ [mm] « » OK«

»Geometry Check  $r=42.042 \geq 0.06 * D_i=15.96$ [mm] « » OK«

»Geometry Check  $r=42.042 \geq 2 * e$ [mm] « » OK«

»Geometry Check  $e=2.21 \leq 0.08 * D_e=21.84$ [mm] « » OK«

»Geometry Check  $e_a=3.2 \geq 0.001 * D_e=0.273$ [mm] « » OK«

»Geometry Check  $R=218.4 \leq D_e=273$ [mm] « » OK«

### MAXIMUM ALLOWABLE WORKING PRESSURE MAWP :NEW & COLD

$$P_s = 2 * f * z * e_a / (R + 0.5 * e_a) \quad (7.5-6)$$

$$= 2 * 212.5 * 1 * 3.7 / (217.9 + 0.5 * 3.7) = 7.1559 \text{ MPa}$$

$$P_y = f * e_a / (\text{beta} * (0.75 * R + 0.2 * D_i)) \quad (7.5-7)$$

$$= 212.5 * 3.7 / (0.5925 * (0.75 * 217.9 + 0.2 * 266)) = 6.1262 \text{ MPa}$$

$$P_b = 111 * f_b * (e_a / (0.75 * R + 0.2 * D_i)) ^ {1.5} * (r / D_i) ^ {0.825} \quad (7.5-8)$$

$$= 111 * 378.67 * (3.7 / (0.75 * 217.9 + 0.2 * 266)) ^ {1.5} * (42.042 / 266) ^ {0.825} = 20.48 \text{ MPa}$$

$$P_{cyl} = 2 * e_a * f * z / (D_i + e_a)$$

$$= 2 * 3.7 * 212.5 * 1 / (266 + 3.7) = 5.8306 \text{ MPa}$$

$P_{max}$  (is the least of  $P_s$ ,  $P_y$ ,  $P_b$  and  $P_{cyl}$ ) =  $P_{max}$

$$= 5.83 = 5.8306 \text{ MPa}$$

### MAXIMUM ALLOWABLE WORKING PRESSURE MAWP :HOT & CORR

$$P_s = 2 * f * z * e_a / (R + 0.5 * e_a) \quad (7.5-6)$$

$$= 2 * 205.73 * 1 * 3.2 / (218.4 + 0.5 * 3.2) = 5.9849 \text{ MPa}$$

$$P_y = f * e_a / (\text{beta} * (0.75 * R + 0.2 * D_i)) \quad (7.5-7)$$

$$= 205.73 * 3.2 / (0.6009 * (0.75 * 218.4 + 0.2 * 266)) = 5.0490 \text{ MPa}$$



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EN13445:2014 Issue 5:2018+A5 - 7.5 DOMED ENDS

E3.1 Bottom Head 17 Aug. 2023 11:33 ConnID:S1.1

$$P_B = 111 * f_b * (e_a / (0.75 * R + 0.2 * D_i))^{1.5} * (r / D_i)^{0.825} \quad (7.5-8)$$
$$= 111 * 329.17 * (3.2 / (0.75 * 218.4 + 0.2 * 266))^{1.5} * (42.042 / 266)^{0.825} = 14.28 \text{ MPa}$$
$$P_{cyl} = 2 * e_a * f * z / (D_i + e_a)$$
$$= 2 * 3.2 * 205.73 * 1 / (266 + 3.2) = 4.8911 \text{ MPa}$$
$$P_{max} \text{ (is the least of } P_s, P_y, P_b \text{ and } P_{cyl}) = P_{max}$$
$$= 4.89 = \underline{\underline{4.8911 \text{ MPa}}}$$

## MAX TEST PRESSURE (Uncorroded cond.at ambient temp.)

$$P_s = 2 * f * z * e_a / (R + 0.5 * e_a) \quad (7.5-6)$$
$$= 2 * 338.1 * 3.7 / (217.9 + 0.5 * 3.7) = 11.39 \text{ MPa}$$
$$P_y = f * e_a / (\beta * (0.75 * R + 0.2 * D_i)) \quad (7.5-7)$$
$$= 338.1 * 3.7 / (0.5925 * (0.75 * 217.9 + 0.2 * 266)) = 9.7471 \text{ MPa}$$
$$P_B = 111 * f_b * (e_a / (0.75 * R + 0.2 * D_i))^{1.5} * (r / D_i)^{0.825} \quad (7.5-8)$$
$$= 111 * 540.95 * (3.7 / (0.75 * 217.9 + 0.2 * 266))^{1.5} * (42.042 / 266)^{0.825} = 29.26 \text{ MPa}$$
$$P_{cyl} = 2 * e_a * f * z / (D_i + e_a)$$
$$= 2 * 3.7 * 338.1 * 1 / (266 + 3.7) = 9.2768 \text{ MPa}$$
$$P_{max} \text{ (is the least of } P_s, P_y, P_b \text{ and } P_{cyl}) = P_{max}$$
$$= 9.28 = \underline{\underline{9.2768 \text{ MPa}}}$$

## EN13445-5;10.2.3.3 REQUIRED MIN.HYDROSTATIC TEST PRESSURE:Ptmin

NEW AT AMBIENT TEMP. FOR TEST GROUPS 1, 2 and 3

$$P_{tmin} = 1.25 * P_d * f_{20} / f = 1.25 * 3.3 * 212.5 / 205.73 = \underline{\underline{4.2607 \text{ MPa}}}$$

$$P_{tmin} = 1.43 * P_d = 1.43 * 3.3 = \underline{\underline{4.7190 \text{ MPa}}}$$

**Test Pressure Ptmin=4.72 <= Pmax=9.28[MPa]****50.8%****OK**

## Maximum diameter of Opening Not Requiring Reinforcement Check , dmax

$$r_{is} = R \quad (9.5-4) = 218.4 = 218.40 \text{ mm}$$
$$\text{Length of Shell Contributing to Reinforcement}$$
$$I_s = \text{Sqr}((2 * r_{is} + e_a) * e_a) \quad (9.5-2)$$
$$= \text{Sqr}((2 * 218.4 + 3.2) * 3.2) = 37.52 \text{ mm}$$
$$\text{Maximum Diameter of Unreinforced Opening in Shell Checked to Rules in Section 9}$$
$$d_{max1} = \text{MIN}(0.5 * D_i, (e_a * I_s * (f - 0.5 * P) / P - r_{is} * I_s) / (0.5 * r_{is} + 0.5 * e_a)) \quad (9.5-7, 22, 23)$$
$$= \text{MIN}(0.5 * 266, (3.2 * 37.52 * (205.73 - 0.5 * 3.3) / 3.3 - 218.4 * 37.52) / (0.5 * 218.4 + 0.5 * 3.2)) = \underline{\underline{0.00 \text{ mm}}}$$
$$\text{Maximum diameter of Opening Not Requiring Reinforcement Check}$$
$$d_{max2} = 0.15 * \text{Sqr}((2 * r_{is} + e_a) * e_a) \quad (9.5-18)$$
$$= 0.15 * \text{Sqr}((2 * 218.4 + 3.2) * 3.2) = \underline{\underline{5.6285 \text{ mm}}}$$
$$\text{Maximum Diameter of Unreinforced Opening}$$
$$d_{max} = \text{MAX}(d_{max1}, d_{max2}) = \text{MAX}(0, 5.63) = \underline{\underline{5.6285 \text{ mm}}}$$

## CALCULATION SUMMARY

### 7.5.3 - TORISPHERICAL ENDS UNDER INTERNAL PRESSURE

#### 7.5.3.2 Required Minimum End Thickness

Required Minimum End Thickness Excl.Allow.  $e_{min}$  :

$$e_{min} = e_{min} = 2.21 = \underline{\underline{2.2136 \text{ mm}}}$$

Required Minimum End Thickness Incl.Allow. :

$$e_{minA} = e_{min} + c + t_h = 2.21 + 0.5 + 0.3 = \underline{\underline{3.0100 \text{ mm}}}$$

**Internal Pressure  $e_{minA}=3.01 <= e_n=4[\text{mm}]$** **75.2%****OK**

Minimum Thickness of Straight Flange Incl.Corr. :

$$e_{cylA} = e_{cyl} + c = 2.15 + 0.5 = \underline{\underline{2.6500 \text{ mm}}}$$

## MAXIMUM ALLOWABLE WORKING PRESSURE MAWP :NEW & COLD

 $P_{max}$  (is the least of  $P_s, P_y, P_b$  and  $P_{cyl}$ ) =  $P_{max}$ 

$$= 5.83 = \underline{\underline{5.8306 \text{ MPa}}}$$

**Company Name -**

Client :GÜVEN SOGUTMA

Vessel Tag No.:OS.HF.33B.66.1

Visual Vessel Design by Hexagon PPM,Ver:20.0 Operator : Rev.:A

EN13445:2014 Issue 5:2018+A5 - 7.5 DOMED ENDS

E3.1 Bottom Head 17 Aug. 2023 11:33 ConnID:S1.1

**MAXIMUM ALLOWABLE WORKING PRESSURE MAWP :HOT & CORR**Pmax (is the least of Ps, Py, Pb and Pcyl) = Pmax  
=4.89=

4.8911 MPa

**MAX TEST PRESSURE (Uncorroded cond.at ambient temp.)**Pmax (is the least of Ps, Py, Pb and Pcyl) = Pmax  
=9.28=

9.2768 MPa

**EN13445-5;10.2.3.3 REQUIRED MIN.HYDROSTATIC TEST PRESSURE:Ptmin**

NEW AT AMBIENT TEMP. FOR TEST GROUPS 1, 2 and 3

Ptmin = 1.25 \* Pd \* f20 / f =1.25\*3.3\*212.5/205.73=

4.2607 MPa

Ptmin = 1.43 \* Pd =1.43\*3.3=

4.7190 MPa

**Test Pressure Ptmin=4.72 <= Pmax=9.28[MPa]****50.8%****OK****Maximum diameter of Opening Not Requiring Reinforcement Check , dmax**

Maximum Diameter of Unreinforced Opening

dmax = MAX( dmax1, dmax2) =MAX(0,5.63)=

5.6285 mm

Volume:0.0033 m3 Weight:2.9 kg (SG= 7.85 )

**Company Name -**

Client :GÜVEN SOGUTMA

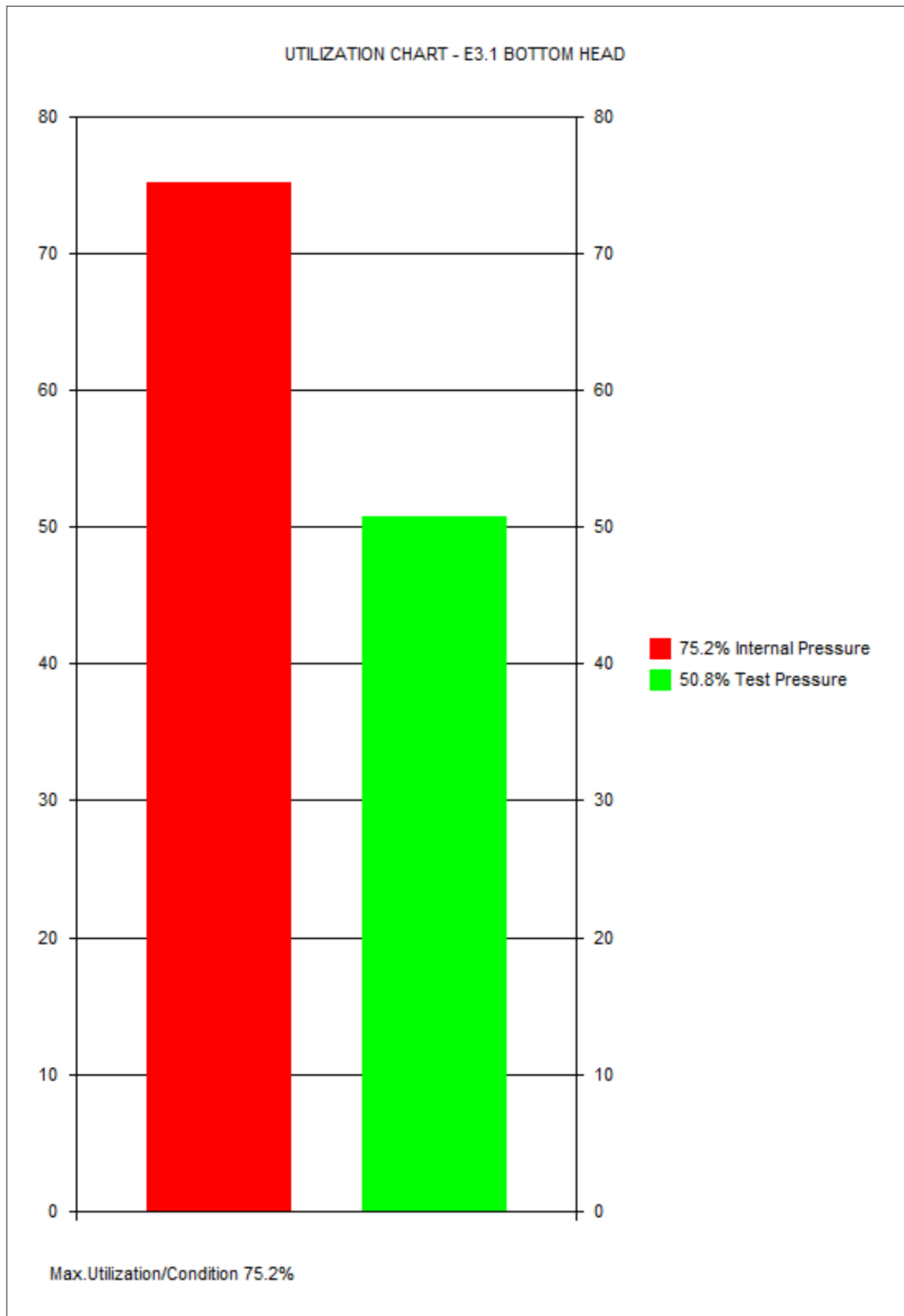
Vessel Tag No.:OS.HF.33B.66.1

Visual Vessel Design by Hexagon PPM,Ver:20.0 Operator : Rev.:A

EN13445:2014 Issue 5:2018+A5 - 7.5 DOMED ENDS

E3.1 Bottom Head

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Vessel Tag No.:OS.HF.33B.66.1

Visual Vessel Design by Hexagon PPM,Ver:20.0 Operator : Rev.:A

EN13445:2014 Issue 5:2018+A5 - 7.5 DOMED ENDS

E3.2 Upper Head 17 Aug. 2023 11:34 ConnID:S1.1

## INPUT DATA

### COMPONENT ATTACHMENT/LOCATION

Attachment: S1.1 Cylindrical Shell Shell  
Location: Along z-axis z1= 345

### GENERAL DESIGN DATA

PRESSURE LOADING: Design Component for Internal Pressure Only

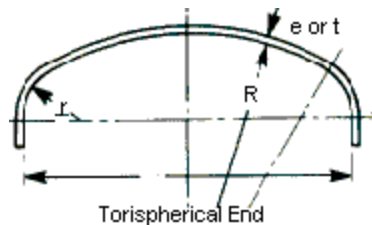
PROCESS CARD:

General Design Data : Temp= 130°C, P=3.3000 MPa, c=0.5 mm, Pext=0.0000 MPa

SPECIFIC DENSITY OF OPERATING LIQUID.....:SG 0.00

LIQUID HEAD.....:LH 0.00 mm

### DIMENSIONS OF END



Type of Torispherical End: Dished End KORBOGEN DIN 28013-28014/SMS 482

WELD JOINT COEFFICIENT: Unwelded Component(z=1.0)

OUTSIDE DIAMETER OF CYLINDRICAL FLANGE OF END.....:De 273.00 mm

LENGTH OF CYLINDRICAL FLANGE OF END.....:Lcyl 15.00 mm

NEGATIVE TOLERANCE/THINNING ALLOWANCE.....:th 0.3000 mm

NOMINAL THICKNESS OF HEAD/END (uncorroded).....:en 4.0000 mm

Include calculation of forming during fabrication to EN13445-4 Section 9.: NO

### MATERIAL DATA FOR END

EN 10028-2:2017, 1.0473 P355GH plate and strip, HT:N THK<=16mm 130'C

Rm=510 Rp=355 Rpt=308.6 f=205.73 f20=212.5 ftest=338.1 E=203868(N/mm2) ro=7.85

Material & Delivery Form: Cold Spun Seamless Austenitic Stainless Steel

### NOZZLES IN KNUCKLE REGION TO SECTION 7.7

Nozzles In Knuckle Region: NO

### WELDING REQUIREMENTS TO EN 1708-1:2010

Comment(Optional):

Type of welded connection: Not Applicable

## CALCULATION DATA

### 7.5.3 - TORISPHERICAL ENDS UNDER INTERNAL PRESSURE

#### 7.5.3.2 Required Minimum End Thickness

Required Thickness of End to Limit Membrane Stress in Central Part

$$e_s = P * R / (2 * f * z - 0.5 * P) \quad (7.5-1)$$

$$= 3.3 * 218.4 / (2 * 205.73 * 1 - 0.5 * 3.3) = 1.7587 \text{ mm}$$

$$f_b = R_{pt} / 1.5 * 1.6 \quad (7.5-5) = 308.6 / 1.5 * 1.6 = 329.17 \text{ N/mm}^2$$

Required Thickness of Knuckle to Avoid Plastic Buckling

$$e_b = (0.75 * R + 0.2 * D_i) * ((P / (111 * f_b)) * (D_i / r)^{0.825})^{(0.667)} \quad (7.5-3)$$

$$= (0.75 * 218.4 + 0.2 * 266) * ((3.3 / (111 * 329.17)) * (266 / 42.042)^{0.825})^{(0.667)}$$

$$= 1.2018 \text{ mm}$$

7.5.3.5 Formulas for Calculation of Factor Beta

$$Y = \text{MIN}(e_{min} / R, 0.04) \quad (7.5-9) = \text{MIN}(2.21 / 218.4, 0.04) = 0.0101$$

$$Z = \text{LOG}(1 / Y) \quad (7.5-10) = \text{LOG}(1 / 0.0101) = 1.9953$$

$$X = r / D_i \quad (7.5-11) = 42.042 / 268.58 = 0.1565$$

# Company Name -

Client :GÜVEN SOGUTMA

Vessel Tag No.:OS.HF.33B.66.1

Visual Vessel Design by Hexagon PPM,Ver:20.0 Operator : Rev.:A

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$$N = 1.006 - 1 / (6.2 + (90 * Y) ^ 4) \quad (7.5-12)$$

$$= 1.006 - 1 / (6.2 + (90 * 0.0101) ^ 4) = 0.8608$$

$$\text{Beta01} = N * (-0.1833 * Z^3 + 1.0383 * Z^2 - 1.2943 * Z + 0.837) \quad (7.5-15)$$

$$= 0.8608 * (-0.1833 * 2.^3 + 1.0383 * 2.^2 - 1.2943 * 2. + 0.837) = 0.8023$$

$$\text{Beta02} = \text{MAX}(0.5, 0.95 * (0.56 - 1.94 * Y - 82.5 * Y ^ 2)) \quad (7.5-17)$$

$$= \text{MAX}(0.5, 0.95 * (0.56 - 1.94 * 0.0101 - 82.5 * 0.0101^2)) = 0.5054$$

$$\text{beta} = 10 * ((0.2 - X) * \text{Beta01} + (X - 0.1) * \text{Beta02}) \quad (7.5-16)$$

$$= 10 * ((0.2 - 0.1565) * 0.8023 + (0.1565 - 0.1) * 0.5054) = 0.6344$$

Required Thickness of Knuckle to Avoid Axisymmetric Yielding

$$e_y = \text{beta} * P * (0.75 * R + 0.2 * D_i) / f \quad (7.5-2)$$

$$= 0.6344 * 3.3 * (0.75 * 218.4 + 0.2 * 268.58) / 205.73 = 2.2136 \text{ mm}$$

NOTE 3, since  $e_y(2.2) > 0.005 * D_i(1.3)$  it is NOT necessary to calculate/consider eb.

Required Minimum End Thickness Excl.Allow.  $e_{min}$  :

$$e_{min} = e_{min} = 2.21 = 2.2136 \text{ mm}$$

Required Minimum End Thickness Incl.Allow. :

$$e_{minA} = e_{min} + c + t_h = 2.21 + 0.5 + 0.3 = 3.0100 \text{ mm}$$

<b>Internal Pressure <math>e_{minA}=3.01 \leq e_n=4</math>[mm]</b>	<b>75.2%</b>	<b>OK</b>
--	--------------	-----------

Analysis Thickness

$$e_a = e_n - c - t_h = 4 - 0.5 - 0.3 = 3.2000 \text{ mm}$$

Inside Diameter of Shell

$$D_i = D_e - 2 * (e_n - c) = 273 - 2 * (4 - 0.5) = 266.00 \text{ mm}$$

Mean Diameter of Shell

$$D_m = (D_e + D_i) / 2 = (273 + 266) / 2 = 269.50 \text{ mm}$$

### 7.5.3.4 - Required Minimum Thickness of Straight Cylindrical Flange

$$L_{lim} = 0.2 * \text{SQRT}(D_i * e_{min}) = 0.2 * \text{SQRT}(266 * 2.21) = 4.8531 \text{ mm}$$

Since  $L_{cyl} > L_{lim}$ , Required Thickness of Straight Cylindrical Flange to 7.4.2

Minimum Thickness of Straight Flange Excl. Allow.

$$e_{cyl} = P * D_i / (2 * f * z - P) \quad (7.4-1)$$

$$= 3.3 * 266 / (2 * 205.73 * 1 - 3.3) = 2.1506 \text{ mm}$$

Minimum Thickness of Straight Flange Incl.Corr. :

$$e_{cylA} = e_{cyl} + c = 2.15 + 0.5 = 2.6500 \text{ mm}$$

### 7.5.3.1 Conditions of Applicability - Torispherical Ends

»Geometry Check  $r=42.042 \leq 0.2 * D_i=53.2$ [mm] « » OK«

»Geometry Check  $r=42.042 \geq 0.06 * D_i=15.96$ [mm] « » OK«

»Geometry Check  $r=42.042 \geq 2 * e$ [mm] « » OK«

»Geometry Check  $e=2.21 \leq 0.08 * D_e=21.84$ [mm] « » OK«

»Geometry Check  $e_a=3.2 \geq 0.001 * D_e=0.273$ [mm] « » OK«

»Geometry Check  $R=218.4 \leq D_e=273$ [mm] « » OK«

### MAXIMUM ALLOWABLE WORKING PRESSURE MAWP :NEW & COLD

$$P_s = 2 * f * z * e_a / (R + 0.5 * e_a) \quad (7.5-6)$$

$$= 2 * 212.5 * 1 * 3.7 / (217.9 + 0.5 * 3.7) = 7.1559 \text{ MPa}$$

$$P_y = f * e_a / (\text{beta} * (0.75 * R + 0.2 * D_i)) \quad (7.5-7)$$

$$= 212.5 * 3.7 / (0.5925 * (0.75 * 217.9 + 0.2 * 266)) = 6.1262 \text{ MPa}$$

$$P_b = 111 * f_b * (e_a / (0.75 * R + 0.2 * D_i)) ^ {1.5 * (r / D_i) ^ {0.825}} \quad (7.5-8)$$

$$= 111 * 378.67 * (3.7 / (0.75 * 217.9 + 0.2 * 266)) ^ {1.5 * (42.042 / 266) ^ {0.825}} = 20.48 \text{ MPa}$$

$$P_{cyl} = 2 * e_a * f * z / (D_i + e_a)$$

$$= 2 * 3.7 * 212.5 * 1 / (266 + 3.7) = 5.8306 \text{ MPa}$$

$P_{max}$  (is the least of  $P_s$ ,  $P_y$ ,  $P_b$  and  $P_{cyl}$ ) =  $P_{max}$

$$= 5.83 = 5.8306 \text{ MPa}$$

### MAXIMUM ALLOWABLE WORKING PRESSURE MAWP :HOT & CORR

$$P_s = 2 * f * z * e_a / (R + 0.5 * e_a) \quad (7.5-6)$$

$$= 2 * 205.73 * 1 * 3.2 / (218.4 + 0.5 * 3.2) = 5.9849 \text{ MPa}$$

$$P_y = f * e_a / (\text{beta} * (0.75 * R + 0.2 * D_i)) \quad (7.5-7)$$

$$= 205.73 * 3.2 / (0.6009 * (0.75 * 218.4 + 0.2 * 266)) = 5.0490 \text{ MPa}$$

# Company Name -

Client :GÜVEN SOGUTMA

Vessel Tag No.:OS.HF.33B.66.1

Visual Vessel Design by Hexagon PPM,Ver:20.0 Operator : Rev.:A

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$$P_b = 111 * f_b * (ea / (0.75 * R + 0.2 * Di))^{1.5} * (r / Di)^{0.825} \quad (7.5-8)$$
$$= 111 * 329.17 * (3.2 / (0.75 * 218.4 + 0.2 * 266))^{1.5} * (42.042 / 266)^{0.825} = 14.28 \text{ MPa}$$
$$P_{cyl} = 2 * ea * f * z / (Di + ea)$$
$$= 2 * 3.2 * 205.73 * 1 / (266 + 3.2) = 4.8911 \text{ MPa}$$
$$P_{max} \text{ (is the least of } P_s, P_y, P_b \text{ and } P_{cyl}) = P_{max}$$
$$= 4.89 = \underline{\underline{4.8911 \text{ MPa}}}$$

## MAX TEST PRESSURE (Uncorroded cond.at ambient temp.)

$$P_s = 2 * f * z * ea / (R + 0.5 * ea) \quad (7.5-6)$$
$$= 2 * 338.1 * 1 * 3.7 / (217.9 + 0.5 * 3.7) = 11.39 \text{ MPa}$$
$$P_y = f * ea / (\beta * (0.75 * R + 0.2 * Di)) \quad (7.5-7)$$
$$= 338.1 * 3.7 / (0.5925 * (0.75 * 217.9 + 0.2 * 266)) = 9.7471 \text{ MPa}$$
$$P_b = 111 * f_b * (ea / (0.75 * R + 0.2 * Di))^{1.5} * (r / Di)^{0.825} \quad (7.5-8)$$
$$= 111 * 540.95 * (3.7 / (0.75 * 217.9 + 0.2 * 266))^{1.5} * (42.042 / 266)^{0.825} = 29.26 \text{ MPa}$$
$$P_{cyl} = 2 * ea * f * z / (Di + ea)$$
$$= 2 * 3.7 * 338.1 * 1 / (266 + 3.7) = 9.2768 \text{ MPa}$$
$$P_{max} \text{ (is the least of } P_s, P_y, P_b \text{ and } P_{cyl}) = P_{max}$$
$$= 9.28 = \underline{\underline{9.2768 \text{ MPa}}}$$

## EN13445-5;10.2.3.3 REQUIRED MIN.HYDROSTATIC TEST PRESSURE:Ptmin

NEW AT AMBIENT TEMP. FOR TEST GROUPS 1, 2 and 3

$$P_{tmin} = 1.25 * P_d * f_{20} / f = 1.25 * 3.3 * 212.5 / 205.73 = \underline{\underline{4.2607 \text{ MPa}}}$$

$$P_{tmin} = 1.43 * P_d = 1.43 * 3.3 = \underline{\underline{4.7190 \text{ MPa}}}$$

**Test Pressure Ptmin=4.72 <= Pmax=9.28[MPa]****50.8%****OK**

## Maximum diameter of Opening Not Requiring Reinforcement Check , dmax

$$r_{is} = R \quad (9.5-4) = 218.4 = 218.40 \text{ mm}$$
$$\text{Length of Shell Contributing to Reinforcement}$$
$$I_s = \text{Sqr}((2 * r_{is} + ea) * ea) \quad (9.5-2)$$
$$= \text{Sqr}((2 * 218.4 + 3.2) * 3.2) = 37.52 \text{ mm}$$
$$\text{Maximum Diameter of Unreinforced Opening in Shell Checked to Rules in Section 9}$$
$$d_{max1} = \text{MIN}(0.5 * Di, (ea * I_s * (f - 0.5 * P) / P - r_{is} * I_s) / (0.5 * r_{is} + 0.5 * ea)) \quad (9.5-7, 22, 23)$$
$$= \text{MIN}(0.5 * 266, (3.2 * 37.52 * (205.73 - 0.5 * 3.3) / 3.3 - 218.4 * 37.52) / (0.5 * 218.4 + 0.5 * 3.2)) = \underline{\underline{0.00 \text{ mm}}}$$
$$\text{Maximum diameter of Opening Not Requiring Reinforcement Check}$$
$$d_{max2} = 0.15 * \text{Sqr}((2 * r_{is} + ea) * ea) \quad (9.5-18)$$
$$= 0.15 * \text{Sqr}((2 * 218.4 + 3.2) * 3.2) = \underline{\underline{5.6285 \text{ mm}}}$$
$$\text{Maximum Diameter of Unreinforced Opening}$$
$$d_{max} = \text{MAX}(d_{max1}, d_{max2}) = \text{MAX}(0, 5.63) = \underline{\underline{5.6285 \text{ mm}}}$$

## CALCULATION SUMMARY

### 7.5.3 - TORISPHERICAL ENDS UNDER INTERNAL PRESSURE

#### 7.5.3.2 Required Minimum End Thickness

$$\text{Required Minimum End Thickness Excl.Allow. } e_{min} :$$
$$e_{min} = e_{min} = 2.21 = \underline{\underline{2.2136 \text{ mm}}}$$

$$\text{Required Minimum End Thickness Incl.Allow. } :$$
$$e_{minA} = e_{min} + c + th = 2.21 + 0.5 + 0.3 = \underline{\underline{3.0100 \text{ mm}}}$$

**Internal Pressure emina=3.01 <= en=4[mm]****75.2%****OK**

Minimum Thickness of Straight Flange Incl.Corr. :

$$e_{cylA} = e_{cyl} + c = 2.15 + 0.5 = \underline{\underline{2.6500 \text{ mm}}}$$

## MAXIMUM ALLOWABLE WORKING PRESSURE MAWP :NEW & COLD

$$P_{max} \text{ (is the least of } P_s, P_y, P_b \text{ and } P_{cyl}) = P_{max}$$
$$= 5.83 = \underline{\underline{5.8306 \text{ MPa}}}$$

**Company Name -**

Client :GÜVEN SOGUTMA

Vessel Tag No.:OS.HF.33B.66.1

Visual Vessel Design by Hexagon PPM,Ver:20.0 Operator : Rev.:A

EN13445:2014 Issue 5:2018+A5 - 7.5 DOMED ENDS

E3.2 Upper Head 17 Aug. 2023 11:34 ConnID:S1.1

**MAXIMUM ALLOWABLE WORKING PRESSURE MAWP :HOT & CORR**Pmax (is the least of Ps, Py, Pb and Pcyl) = Pmax  
=4.89=4.8911 MPa**MAX TEST PRESSURE (Uncorroded cond.at ambient temp.)**Pmax (is the least of Ps, Py, Pb and Pcyl) = Pmax  
=9.28=9.2768 MPa**EN13445-5;10.2.3.3 REQUIRED MIN.HYDROSTATIC TEST PRESSURE:Ptmin**

NEW AT AMBIENT TEMP. FOR TEST GROUPS 1, 2 and 3

Ptmin = 1.25 \* Pd \* f20 / f =1.25\*3.3\*212.5/205.73=

4.2607 MPa

Ptmin = 1.43 \* Pd =1.43\*3.3=

4.7190 MPa**Test Pressure Ptmin=4.72 <= Pmax=9.28[MPa]****50.8%****OK****Maximum diameter of Opening Not Requiring Reinforcement Check , dmax**

Maximum Diameter of Unreinforced Opening

dmax = MAX( dmax1, dmax2) =MAX(0,5.63)=

5.6285 mm

Volume:0.0033 m3 Weight:2.9 kg (SG= 7.85 )

**Company Name -**

Client :GÜVEN SOGUTMA

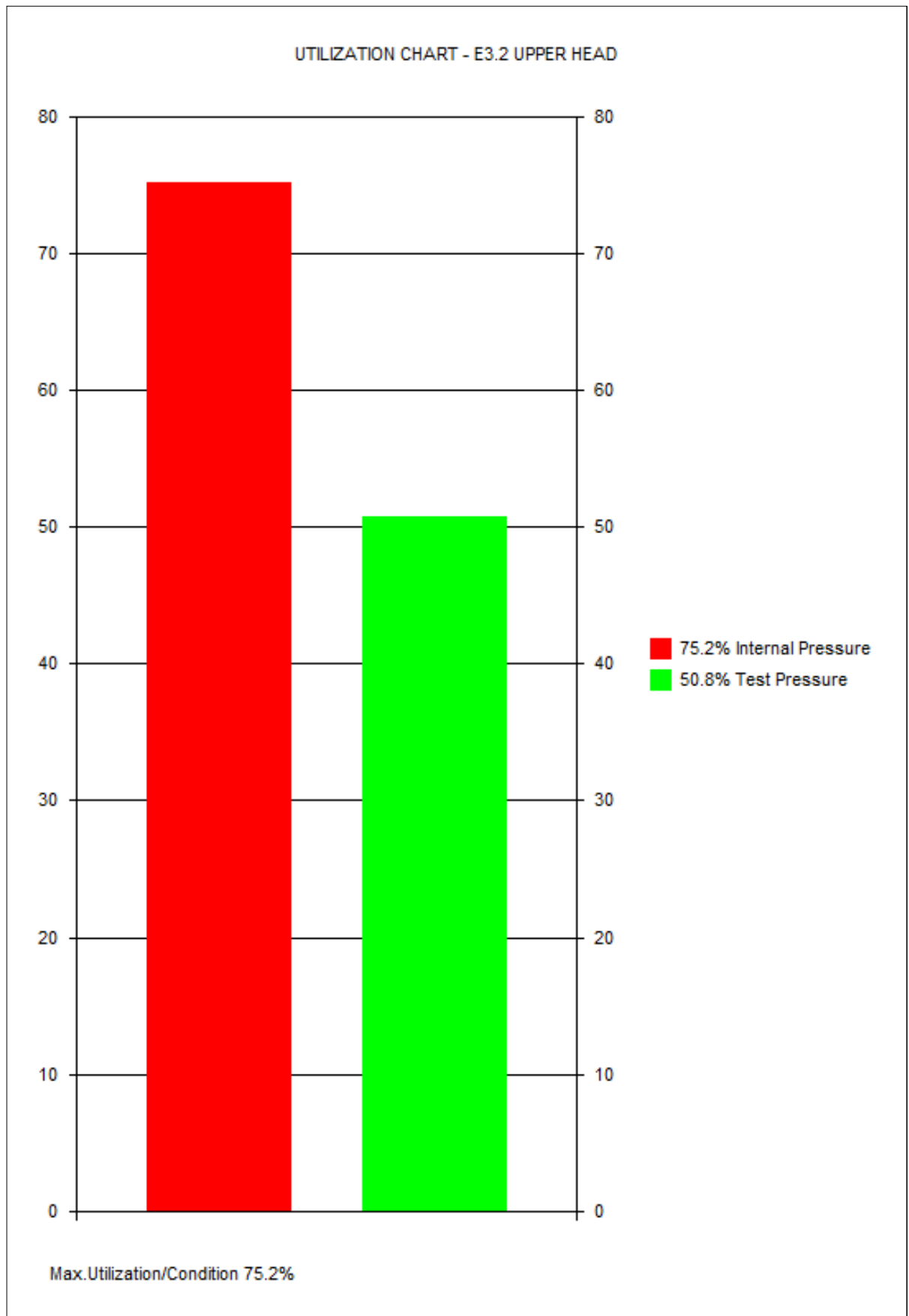
Vessel Tag No.:OS.HF.33B.66.1

Visual Vessel Design by Hexagon PPM,Ver:20.0 Operator : Rev.:A

EN13445:2014 Issue 5:2018+A5 - 7.5 DOMED ENDS

E3.2 Upper Head

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# Company Name -

Client :GÜVEN SOGUTMA

Vessel Tag No.:OS.HF.33B.66.1

Visual Vessel Design by Hexagon PPM,Ver:20.0 Operator : Rev.:A

EN13445:2014 Issue 5:2018+A5 - 10.5 BOLTED CIRCULAR FLAT END

E5.1 Cover Flange 17 Aug. 2023 11:34 ConnID:F.1

## INPUT DATA

### COMPONENT ATTACHMENT/LOCATION

Attachment: F.1 RT - Flange Ring Flange N.3  
Location: Along z-axis z1= -59.3

### GENERAL DESIGN DATA

PROCESS CARD: General Design Data : Temp= 130°C, P=3.3000 MPa, c=0.5 mm  
SPECIFIC DENSITY OF OPERATING LIQUID.....:SG 0.00  
LIQUID HEAD.....:LH 144.10 mm  
Check Deflection of Cover to TEMA RCB-9-21(multipass units): NO  
Shape of Cover: Circular  
Stayed Flat Plate to section 20.2: NO  
Circular flat ends with radial reinforcement ribs to section 21: NO

### DATA FOR MATING FLANGE (F.1)

TYPE OF BLIND FLANGE: Blind flange with gasket entirely within the bolt circle.  
OUTSIDE DIAMETER OF FLANGE.....:A 149.00 mm  
BOLT-CIRCLE DIAMETER.....:C 130.00 mm  
NUMBER OF BOLTS.....:n 8.0000  
DIAMETER OF BOLT HOLES IN FLANGE.....:d 10.00 mm  
FLANGE DESIGN BOLT LOAD FOR ASSEMBLY CONDITION.....:W 46.21 kN  
DIAMETER AT LOCATION OF GASKET LOAD REACTION.....:G 98.50 mm  
GASKET FACTOR.....:m 2.0000  
EFFECTIVE GASKET SEATING WIDTH.....:b 2.0000 mm

### DATA FOR BLIND FLANGE

NOMINAL THICKNESS OF HEAD/END (uncorroded).....:en 11.50 mm  
THICKNESS OF FLANGE(uncorroded).....:e 11.50 mm  
EN 10028-2:2017, 1.0473 P355GH plate and strip, HT:N THK<=16mm 130'C  
Rm=510 Rp=355 Rpt=308.6 f=205.73 f20=212.5 ftest=338.1 E=203868(N/mm2) ro=7.85

### WELDING REQUIREMENTS TO EN 1708-1:2010

Comment(Optional):  
Type of welded connection: Not Applicable

## CALCULATION DATA

### 10.5.2.1 MINIMUM THICKNESS OF BLIND FLANGE WITHIN GASKET e

Mean Bolt Pitch  
 $tB = \pi * C / n = 3.14 * 130 / 8 = 51.05 \text{ mm}$   
 $C_f = \text{MAX}(\text{Sqr}(tB / (2 * db + 6 * (eb - c) / (0.5 + m))), 1)$  (10.5-4)  
 $= \text{MAX}(\text{Sqr}(51.05 / (2 * 9 + 6 * (11.5 - 0.5) / (0.5 + 2))), 1) = 1.0723$   
Bolting Up Conditions  
 $eA = \text{Sqr}(C_f * 3 * (C - G) / (\pi * G) * (W / f20))$  (10.5-2)  
 $= \text{Sqr}(1.07 * 3 * (130 - 98.5) / (3.14 * 98.5) * (46.21 / 212.5)) = 8.4385 \text{ mm}$   
Operating Conditions  
 $eP = \text{Sqr}((0.31 * G^2 + 3 * C_f * (G / 4 + 2 * b * m) * (C - G)) * P / f)$  (10.5-3)  
 $= \text{Sqr}((0.31 * 98.5^2 + 3 * 1.07 * (98.5 / 4 + 2 * 2 * 2) * (130 - 98.5)) * 3.3 / 205.73) = 10.06 \text{ mm}$   
Minimum thickness excluding corrosion  $e_{min}$   
 $e_{min} = \text{Max}(eA, eP)$  (10.5-1) =  $\text{Max}(8.44, 10.06) = 10.06 \text{ mm}$   
Minimum thickness including allowance e  
 $e = e_{min} + c = 10.063 + 0.5 = 10.56 \text{ mm}$

End Thickness  $e_n = 11.5 \geq e = 10.563$ [mm]

91.8%

OK

### 10.5.2.2 MINIMUM THICKNESS OF FLANGED EXTENSION e1

$eP1 = \text{Sqr}(3 * C_f * (G / 4 + 2 * b * m) * (C - G) * P / f)$  (10.5-6)  
 $= \text{Sqr}(3 * 1.07 * (98.5 / 4 + 2 * 2 * 2) * (130 - 98.5) * 3.3 / 205.73) = 7.2821 \text{ mm}$   
 $e1 = \text{Max}(eA, eP1)$  (10.5-5) =  $\text{Max}(8.44, 7.28) = 8.4390 \text{ mm}$

# Company Name -

Client :GÜVEN SOGUTMA

Vessel Tag No.:OS.HF.33B.66.1

Visual Vessel Design by Hexagon PPM,Ver:20.0 Operator : Rev.:A

EN13445:2014 Issue 5:2018+A5 - 10.5 BOLTED CIRCULAR FLAT END

E5.1 Cover Flange 17 Aug. 2023 11:34 ConnID:F.1

Flanged Extension Thk. eb=11.5 >= e1=8.439[mm]

73.3%

OK

## PRESSURE CALCULATIONS

### MAXIMUM ALLOWABLE WORKING PRESSURE MAWP :NEW & COLD

$$P_{max1} = \frac{e_a^2 \cdot f}{(0.31 \cdot G^2 + 3 \cdot C_f \cdot (G/4 + 2 \cdot b \cdot m)) \cdot (C-G)}$$
$$= \frac{11.5^2 \cdot 212.5}{(0.31 \cdot 98.5^2 + 3 \cdot 1.07 \cdot (98.5/4 + 2 \cdot 2 \cdot 2)) \cdot (130 - 98.5)} = 4.4512 \text{ MPa}$$

$$P_{max2} = \frac{e_1^2 \cdot f}{(3 \cdot C_f \cdot (G/4 + 2 \cdot b \cdot m)) \cdot (C-G)}$$
$$= \frac{11.5^2 \cdot 212.5}{(3 \cdot 1.07 \cdot (98.5/4 + 2 \cdot 2 \cdot 2)) \cdot (130 - 98.5)} = 8.5008 \text{ MPa}$$

$$P_{max} = \text{MIN}(P_{max1}, P_{max2}) = \text{MIN}(4.45, 8.5) = 4.4512 \text{ MPa}$$

### MAXIMUM ALLOWABLE WORKING PRESSURE MAWP :HOT & CORR

$$P_{max1} = \frac{e_a^2 \cdot f}{(0.31 \cdot G^2 + 3 \cdot C_f \cdot (G/4 + 2 \cdot b \cdot m)) \cdot (C-G)}$$
$$= \frac{11^2 \cdot 205.73}{(0.31 \cdot 98.5^2 + 3 \cdot 1.07 \cdot (98.5/4 + 2 \cdot 2 \cdot 2)) \cdot (130 - 98.5)} = 3.9428 \text{ MPa}$$

$$P_{max2} = \frac{e_1^2 \cdot f}{(3 \cdot C_f \cdot (G/4 + 2 \cdot b \cdot m)) \cdot (C-G)}$$
$$= \frac{11^2 \cdot 205.73}{(3 \cdot 1.07 \cdot (98.5/4 + 2 \cdot 2 \cdot 2)) \cdot (130 - 98.5)} = 7.5299 \text{ MPa}$$

$$P_{max} = \text{MIN}(P_{max1}, P_{max2}) = \text{MIN}(3.94, 7.53) = 3.9428 \text{ MPa}$$

### MAX TEST PRESSURE (Uncorroded cond.at ambient temp.)

$$P_{max1} = \frac{e_a^2 \cdot f}{(0.31 \cdot G^2 + 3 \cdot C_f \cdot (G/4 + 2 \cdot b \cdot m)) \cdot (C-G)}$$
$$= \frac{11.5^2 \cdot 338.1}{(0.31 \cdot 98.5^2 + 3 \cdot 1.07 \cdot (98.5/4 + 2 \cdot 2 \cdot 2)) \cdot (130 - 98.5)} = 7.0821 \text{ MPa}$$

$$P_{max2} = \frac{e_1^2 \cdot f}{(3 \cdot C_f \cdot (G/4 + 2 \cdot b \cdot m)) \cdot (C-G)}$$
$$= \frac{11.5^2 \cdot 338.1}{(3 \cdot 1.07 \cdot (98.5/4 + 2 \cdot 2 \cdot 2)) \cdot (130 - 98.5)} = 13.53 \text{ MPa}$$

$$P_{max} = \text{MIN}(P_{max1}, P_{max2}) = \text{MIN}(7.08, 13.53) = 7.0821 \text{ MPa}$$

### EN13445-5;10.2.3.3 REQUIRED MIN.HYDROSTATIC TEST PRESSURE:Ptmin

NEW AT AMBIENT TEMP. FOR TEST GROUPS 1, 2 and 3

$$P_{tmin} = 1.25 \cdot P_d \cdot f_{20} / f = 1.25 \cdot 3.3 \cdot 212.5 / 205.73 = 4.2607 \text{ MPa}$$

$$P_{tmin} = 1.43 \cdot P_d = 1.43 \cdot 3.3 = 4.7190 \text{ MPa}$$

Test Pressure Ptmin=4.72 <= Pmax=7.08[MPa]

66.6%

OK

## CALCULATION SUMMARY

### 10.5.2.1 MINIMUM THICKNESS OF BLIND FLANGE WITHIN GASKET e

Minimum thickness excluding corrosion emin

$$e_{min} = \text{Max}(e_A, e_P) \text{ (10.5-1)} = \text{Max}(8.44, 10.06) = 10.06 \text{ mm}$$

Minimum thickness including allowance e

$$e = e_{min} + c = 10.063 + 0.5 = 10.56 \text{ mm}$$

End Thickness en=11.5 >= e=10.563[mm]

91.8%

OK

### 10.5.2.2 MINIMUM THICKNESS OF FLANGED EXTENSION e1

$$e_1 = \text{Max}(e_A, e_{P1}) \text{ (10.5-5)} = \text{Max}(8.44, 7.28) = 8.4390 \text{ mm}$$

Flanged Extension Thk. eb=11.5 >= e1=8.439[mm]

73.3%

OK

## PRESSURE CALCULATIONS

### MAXIMUM ALLOWABLE WORKING PRESSURE MAWP :NEW & COLD

$$P_{max} = \text{MIN}(P_{max1}, P_{max2}) = \text{MIN}(4.45, 8.5) = 4.4512 \text{ MPa}$$

**Company Name -**

Client :GÜVEN SOGUTMA Vessel Tag No.:OS.HF.33B.66.1

Visual Vessel Design by Hexagon PPM,Ver:20.0 Operator : Rev.:A

EN13445:2014 Issue 5:2018+A5 - 10.5 BOLTED CIRCULAR FLAT END

E5.1 Cover Flange 17 Aug. 2023 11:34 ConnID:F.1

**MAXIMUM ALLOWABLE WORKING PRESSURE MAWP :HOT & CORR**

$P_{max} = \text{MIN}( P_{max1} , P_{max2} ) = \text{MIN}(3.94, 7.53) =$  3.9428 MPa

**MAX TEST PRESSURE (Uncorroded cond.at ambient temp.)**

$P_{max} = \text{MIN}( P_{max1} , P_{max2} ) = \text{MIN}(7.08, 13.53) =$  7.0821 MPa

**EN13445-5;10.2.3.3 REQUIRED MIN.HYDROSTATIC TEST PRESSURE:Ptmin**

NEW AT AMBIENT TEMP. FOR TEST GROUPS 1, 2 and 3  
 $P_{tmin} = 1.25 * P_d * f_{20} / f = 1.25 * 3.3 * 212.5 / 205.73 =$  4.2607 MPa

$P_{tmin} = 1.43 * P_d = 1.43 * 3.3 =$  4.7190 MPa

<b>Test Pressure Ptmin=4.72 &lt;= Pmax=7.08[MPa]</b>	<b>66.6%</b>	<b>OK</b>
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Volume:0.00 m3 Weight:1 kg (SG= 7.85)

**Company Name -**

Client :GÜVEN SOGUTMA

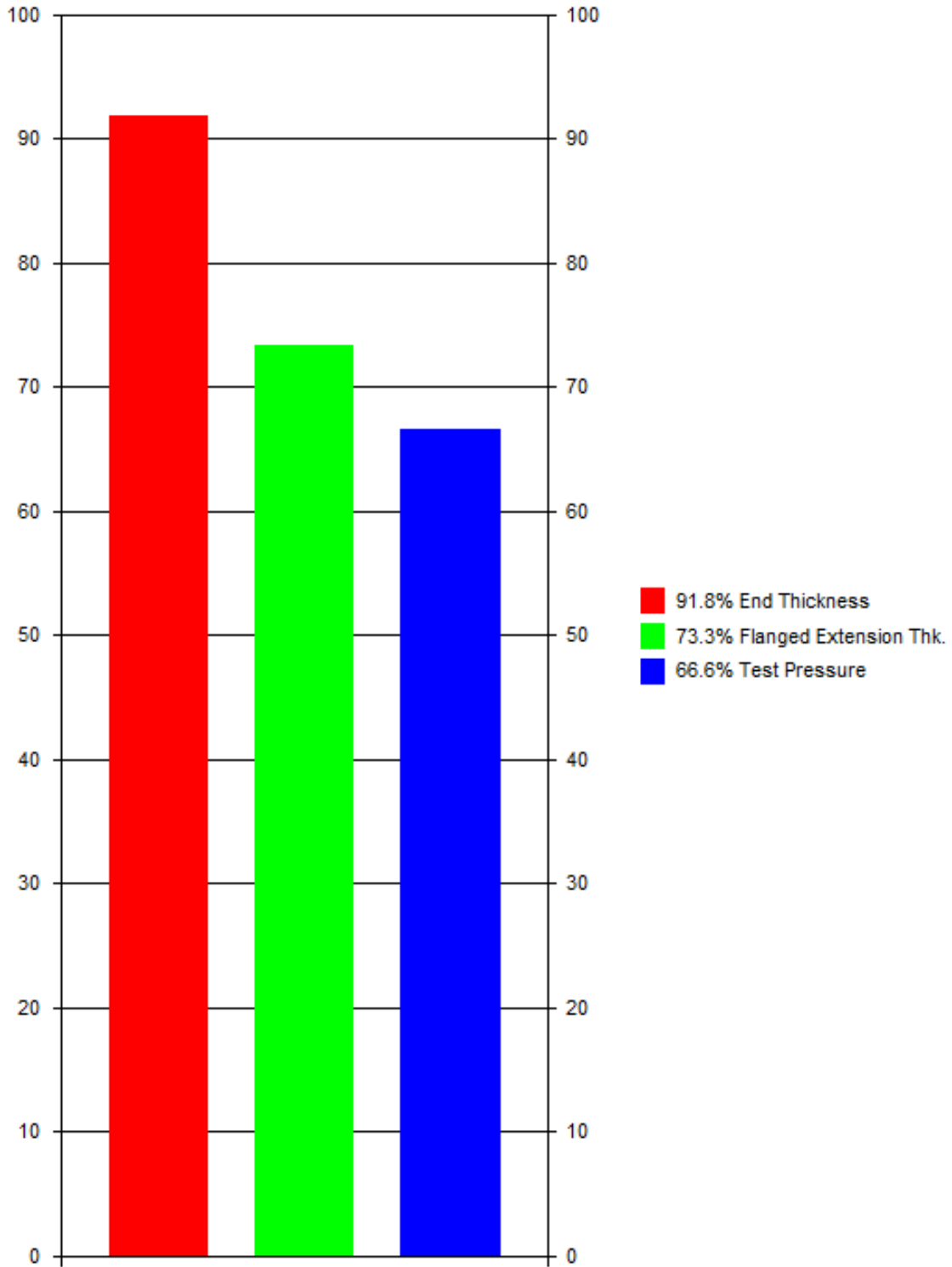
Vessel Tag No.:OS.HF.33B.66.1

Visual Vessel Design by Hexagon PPM,Ver:20.0 Operator : Rev.:A

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E5.1 Cover Flange 17 Aug. 2023 11:34 ConnID:F.1

UTILIZATION CHART - E5.1 COVER FLANGE



Max.Utilization/Condition 91.8%

# Company Name -

Client :GÜVEN SOGUTMA

Vessel Tag No.:OS.HF.33B.66.1

Visual Vessel Design by Hexagon PPM,Ver:20.0 Operator : Rev.:A

EN13445:2014 Issue 5:2018+A5 - 9.5 ISOLATED OPENINGS IN SHELLS

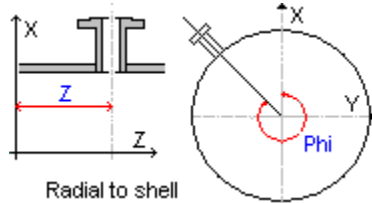
N.1 Inlet 17 Aug. 2023 11:35 ConnID:S1.1

## INPUT DATA

### COMPONENT ATTACHMENT/LOCATION

Attachment: S1.1 Cylindrical Shell Shell

Connect this nozzle to the nozzle neck of another nozzle: NO



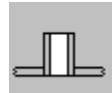
Radial to shell

Orientation & Location of Nozzle: Radial to Shell

z-location of nozzle along axis of attachment.....:z 260.00 mm

Angle of Rotation of nozzle axis projected in the x-y plane:Phi 0.00 Degr.

### GENERAL DESIGN DATA



Type of Opening: Nozzle Without Standard ASME or DIN/EN Flange Attachment

PRESSURE LOADING: Design Component for Internal Pressure Only

PROCESS CARD:

General Design Data : Temp= 130°C, P=3.3000 MPa, c=0.5 mm, Pext=0.0000 MPa

SPECIFIC DENSITY OF OPERATING LIQUID.....:SG 0.00

LIQUID HEAD.....:LH 0.00 mm

Apply a different corrosion allowance to nozzle neck than the shell thickness.: NO

Include Nozzle Load Calculation: NO

### SHELL DATA (S1.1)

Shell Type: Cylindrical Shell

OUTSIDE DIAMETER OF SHELL.....:De 273.00 mm

NOMINAL WALL THICKNESS (uncorroded).....:en 4.5000 mm

NEGATIVE TOLERANCE/THINNING ALLOWANCE.....:th 0.4500 mm

EN 10217-3:2019, 1.0565 P355NH welded tube, HT:N THK<=20mm 130'C

Rm=490 Rp=355 Rpt=292 fs=194.67 f20=204.17 ftest=338.1 E=203868(N/mm<sup>2</sup>) ro=7.85

### NOZZLE MATERIAL DATA



Delivery Form: Seamless Pipe

EN 10216-2:2013, 1.0425 P265GH seamless tube, HT:N THK<=16mm 130'C

Rm=410 Rp=265 Rpt=218.2 fb=145.47 f20=170.83 ftest=252.38 E=203868(N/mm<sup>2</sup>) ro=7.85

### NOZZLE DIMENSIONAL DATA

# Company Name -

Client :GÜVEN SOGUTMA

Vessel Tag No.:OS.HF.33B.66.1

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Attachment: Set In Flush Nozzle

Shape of Nozzle/Opening: Circular

Application:

9.4.6.3 NOT a critical fatigue area, and calc.temp.is outside creep range.

OUTSIDE NOZZLE DIAMETER.....:deb 74.50 mm

NOMINAL NOZZLE THICKNESS (uncorroded).....:enb 5.0000 mm

Size of Flange and Nozzle:

Comment (Optional):

NEGATIVE TOLERANCE/THINNING ALLOWANCE.....: 12.50 %

NOZZLE STANDOUT MEASURED FROM VESSEL OD.....:ho 40.00 mm

## WELDING DATA

Nozzle/Pad to Shell Welding Area: Exclude Area of Nozzle to Shell Weld

Nozzle Weld Intersect: Nozzle Does NOT Intersect with a Welded Shell Seam

ANGLE PhiC(OBLIQUE IN TRANSVERSE.CROSS SECT.)Fig.9.5-2:PhiC 0.00 Degr.

ANGLE PhiL(OBLIQUE IN LONG.CROSS SECT.)Fig.9.5-1.....:PhiL 0.00 Degr.

## DATA FOR REINFORCEMENT PAD



Type of Pad: No Pad

## LIMITS OF REINFORCEMENT

Reduction of Limits of Reinforcement: No Reduction Required

## WELDING REQUIREMENTS TO EN 1708-1:2010

Comment(Optional):

Type of welded connection: Not Applicable

## CALCULATION DATA

### PRELIMINARY CALCULATIONS

Shell Analysis Thickness eas = en - c - th =4.5-0.5-0.45= 3.5500 mm

Nozzle Analysis Thickness eab = enb - cn - NegDev =5-0.5-0.625= 3.8750 mm

Inside Radius of Curvature ris = De / 2 - eas (9.5-3) =273/2-3.55= 132.95 mm

dib = deb - 2 \* eab =74.5-2\*3.875= 66.75 mm

Min.Nozzle Thk.Based on Internal Pressure ebp

ebp = P \* deb / (2 \* fb \* z + P) =3.3\*74.5/(2\*145.47\*1+3.3)= 0.8400 mm

Allowable Stresses

fob = Min( fs, fb) (9.5-8) =Min(194.67,145.47)= 145.47 N/mm<sup>2</sup>

### GEOMETRIC LIMITATIONS

»Check Max.Diameter of Nozzle dib/(2\*ris)=0.251 <= 1.00=1[mm] «» OK«

Min.Nozzle Thk. ebp=0.84 <= eab=3.875[mm]

21.6%

OK

## 9.5.2.4.4 Nozzles normal to the shell, with or without reinforcement pads.

Calculation of Stress Loaded Areas Effective as Reinforcement

# Company Name -

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## Area of Shell Afs

Limit of Reinforcement Along Shell

$$\text{Iso} = \text{Sqr}((2 * \text{ris} + \text{eas}) * \text{eas})$$

$$= \text{Sqr}((2 * 132.95 + 3.55) * 3.55) =$$

30.93 mm

Set In Nozzle

$$\text{Afs} = \text{eas} * \text{Is} (9.5-79) = 3.55 * 30.93 =$$

109.79 mm<sup>2</sup>

## Area of Nozzle Afb

Limit of Reinforcement Along Nozzle (outside shell)

$$\text{Ibo} = \text{MIN}(\text{Sqr}((\text{deb} - \text{eb}) * \text{eb}), \text{ho})$$

(9.5-76)

$$= \text{MIN}(\text{Sqr}((74.5 - 3.875) * 3.875), 40) =$$

16.54 mm

Set In Nozzle

$$\text{Afb} = \text{eb} * (\text{Ibo} + \text{Ibi} + \text{eas}) (9.5-78) = 3.875 * (16.54 + 0 + 3.55) =$$

77.86 mm<sup>2</sup>

## Calculation of Pressure Loaded Areas

In the Nozzle Apb

$$\text{Apb} = 0.5 * \text{dib} * (\text{Ibo} + \text{eas}) (9.5-84) = 0.5 * 66.75 * (16.54 + 3.55) =$$

670.60 mm<sup>2</sup>

Cyl.Shell in the Longitudinal Section Aps

$$\text{ApsL} = \text{ris} * (\text{Is} + \text{a}) (9.5-94) = 132.95 * (30.93 + 37.25) =$$

9064.28 mm<sup>2</sup>

Cyl.Shell in the Transverse Cross Section Aps

$$\text{ApsT} = 0.5 * \text{ris}^2 * (\text{Is} + \text{a}) / (0.5 * \text{eas} + \text{ris})$$

(9.5-105)

$$= 0.5 * 132.95^2 * (30.93 + 37.25) / (0.5 * 3.55 + 132.95) =$$

4504.68 mm<sup>2</sup>

$$\text{Aps} = \text{MAX}(\text{ApsL}, \text{ApsT}) = \text{MAX}(9064.28, 4504.68) =$$

9064.28 mm<sup>2</sup>

## 9.5.2 Reinforcement Rules

### Pressure Area Required pA(req.)

$$\text{pAReqL} = P * (\text{ApsL} + \text{Apb}) (9.5-7) = 3.3 * (9064.28 + 670.6) =$$

32.13 kN

$$\text{pAReqT} = P * (\text{ApsT} + \text{Apb} + 0.5 * \text{Apphi})$$

(9.5-7)

$$= 3.3 * (4504.68 + 670.6 + 0.5 * 0) =$$

17.08 kN

$$\text{pAReq} = \text{MAX}(\text{pAReqL}, \text{pAReqT}) = \text{MAX}(32125.11, 17078.45) =$$

32.13 kN

### Pressure Area Available pA(aval.)

$$\text{pAAval} = (\text{Afs} + \text{Afw}) * (\text{fs} - 0.5 * P) + \text{Afp} * (\text{fop} - 0.5 * P) + \text{Afb} * (\text{fob} - 0.5 * P)$$

(9.5-7)

$$= (109.79 + 0) * (194.67 - 0.5 * 3.3) + 0 * (0 - 0.5 * 3.3) + 77.86 * (145.47 - 0.5 * 3.3) =$$

32.39 kN

**Nozzle Reinforcement pAAval=32.39 >= pAReq=32.13[kN]**

**99.1%**

**OK**

### Maximum Allowable Pressure Pmax

$$\text{Pmax} = (\text{Afs} + \text{Afw}) * \text{fs} + \text{Afb} * \text{fob} / ((\text{ApsL} + \text{Apb}) + 0.5 * (\text{Afs} + \text{Afw} + \text{Afb} + \text{Afp}))$$

(9.5-10)

$$= (109.79 + 0) * 194.67 + 77.86 * 145.47 / ((9064.28 + 670.6) + 0.5 * (109.79 + 0 + 77.86 + 0))$$

$$= 3.3270 \text{ MPa}$$

### Max.Allowable Test Pressure Ptmax

$$\text{Ptmax} = ==$$

6.5576 MPa

Weight of Nozzle: .4273kg

## CALCULATION SUMMARY

**Min.Nozzle Thk. ebp=0.84 <= eab=3.875[mm]**

**21.6%**

**OK**

### 9.5.2.4.4 Nozzles normal to the shell, with or without reinforcement pads.

Limit of Reinforcement Along Shell

$$\text{Iso} = \text{Sqr}((2 * \text{ris} + \text{eas}) * \text{eas})$$

$$= \text{Sqr}((2 * 132.95 + 3.55) * 3.55) =$$

30.93 mm

Limit of Reinforcement Along Nozzle (outside shell)

$$\text{Ibo} = \text{MIN}(\text{Sqr}((\text{deb} - \text{eb}) * \text{eb}), \text{ho})$$

(9.5-76)

$$= \text{MIN}(\text{Sqr}((74.5 - 3.875) * 3.875), 40) =$$

16.54 mm

**Company Name -**

Client :GÜVEN SOGUTMA

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**Pressure Area Required pA(req.)**

$$pAReqL = P * (ApsL + Apb) \quad (9.5-7) = 3.3 * (9064.28 + 670.6) = \underline{\underline{32.13 \text{ kN}}}$$

$$pAReqT = P * (ApsT + Apb + 0.5 * Apphi) \quad (9.5-7)$$

$$= 3.3 * (4504.68 + 670.6 + 0.5 * 0) = \underline{\underline{17.08 \text{ kN}}}$$

$$pAReq = \text{MAX}( pAReqL, pAReqT ) = \text{MAX}(32125.11, 17078.45) = \underline{\underline{32.13 \text{ kN}}}$$

**Pressure Area Available pA(aval.)**

$$pAAval = (Afs + Afw) * (fs - 0.5 * P) + Afp * (fop - 0.5 * P) + Afb * (fob - 0.5 * P) \quad (9.5-7)$$

$$= (109.79 + 0) * (194.67 - 0.5 * 3.3) + 0 * (0 - 0.5 * 3.3) + 77.86 * (145.47 - 0.5 * 3.3) = \underline{\underline{32.39 \text{ kN}}}$$

<b>Nozzle Reinforcement pAAval=32.39 &gt;= pAReq=32.13[kN]</b>	<b>99.1%</b>	<b>OK</b>
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**Maximum Allowable Pressure Pmax**

$$Pmax = (Afs + Afw) * fs + Afb * fob / ((ApsL + Apb) + 0.5 * (Afs + Afw + Afb + Afp)) \quad (9.5-10)$$

$$= (109.79 + 0) * 194.67 + 77.86 * 145.47 / ((9064.28 + 670.6) + 0.5 * (109.79 + 0 + 77.86 + 0))$$

$$= \underline{\underline{3.3270 \text{ MPa}}}$$

Volume:0.0001000 m3 Weight:0.4 kg (SG= 7.85)



**Company Name -**

Client :GÜVEN SOGUTMA

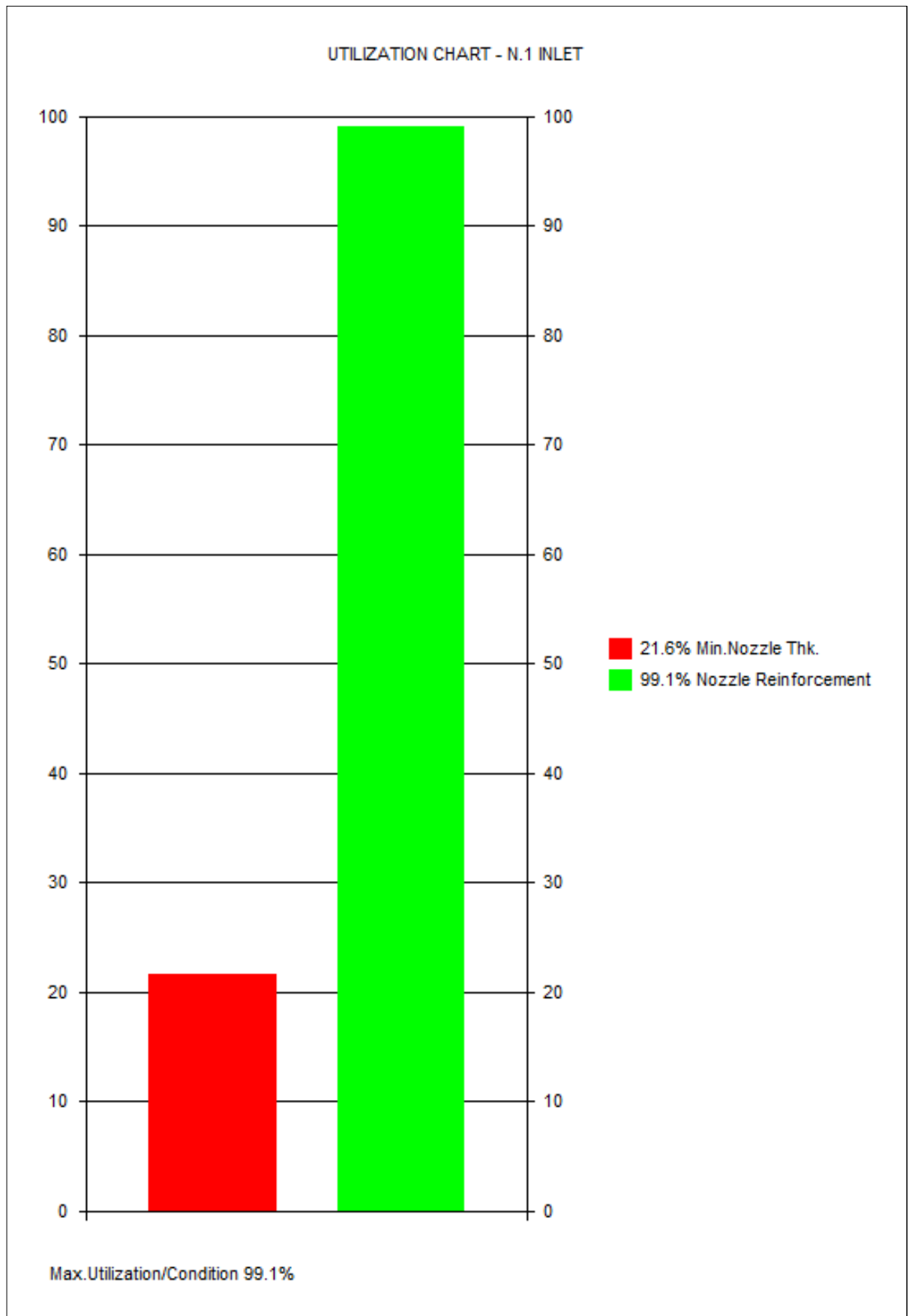
Vessel Tag No.:OS.HF.33B.66.1

Visual Vessel Design by Hexagon PPM,Ver:20.0 Operator : Rev.:A

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N.1 Inlet

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Vessel Tag No.:OS.HF.33B.66.1

Visual Vessel Design by Hexagon PPM,Ver:20.0 Operator : Rev.:A

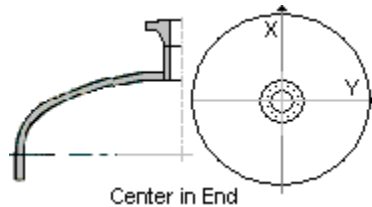
EN13445:2014 Issue 5:2018+A5 - 9.5 ISOLATED OPENINGS IN SHELLS

N.2 Outlet 17 Aug. 2023 11:35 ConnID:E3.2

## INPUT DATA

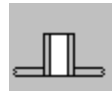
### COMPONENT ATTACHMENT/LOCATION

Attachment: E3.2 Torispherical End Upper Head S1.1  
Connect this nozzle to the nozzle neck of another nozzle: NO



Orientation & Location of Nozzle: Center in End

### GENERAL DESIGN DATA



Type of Opening: Nozzle Without Standard ASME or DIN/EN Flange Attachment  
PRESSURE LOADING: Design Component for Internal Pressure Only

PROCESS CARD:

General Design Data : Temp= 130°C, P=3.3000 MPa, c=0.5 mm, Pext=0.0000 MPa

SPECIFIC DENSITY OF OPERATING LIQUID.....:SG 0.00

LIQUID HEAD.....:LH 0.00 mm

Apply a different corrosion allowance to nozzle neck than the shell thickness.: NO

Include Nozzle Load Calculation: NO

### SHELL DATA (E3.2)

Shell Type: Torispherical End

OUTSIDE DIAMETER OF SHELL.....:De 273.00 mm

NOMINAL WALL THICKNESS (uncorroded).....:en 4.0000 mm

NEGATIVE TOLERANCE/THINNING ALLOWANCE.....:th 0.3000 mm

INSIDE SPHERICAL RADIUS (corroded).....:R 218.40 mm

EN 10028-2:2017, 1.0473 P355GH plate and strip, HT:N THK<=16mm 130'C

Rm=510 Rp=355 Rpt=308.6 fs=205.73 f20=212.5 ftest=338.1 E=203868(N/mm2) ro=7.85

### NOZZLE MATERIAL DATA

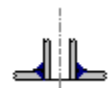


Delivery Form: Seamless Pipe

EN 10216-2:2013, 1.0425 P265GH seamless tube, HT:N THK<=16mm 130'C

Rm=410 Rp=265 Rpt=218.2 fb=145.47 f20=170.83 ftest=252.38 E=203868(N/mm2) ro=7.85

### NOZZLE DIMENSIONAL DATA



Attachment: Set In Flush Nozzle

Shape of Nozzle/Opening: Circular

Application:

9.4.6.3 NOT a critical fatigue area, and calc.temp.is outside creep range.

OUTSIDE NOZZLE DIAMETER.....:deb 74.50 mm

NOMINAL NOZZLE THICKNESS (uncorroded).....:enb 5.0000 mm

Size of Flange and Nozzle:

Comment (Optional):

NEGATIVE TOLERANCE/THINNING ALLOWANCE.....: 12.50 %

NOZZLE STANDOUT MEASURED FROM VESSEL OD.....:ho 40.00 mm

# Company Name -

Client :GÜVEN SOGUTMA

Vessel Tag No.:OS.HF.33B.66.1

Visual Vessel Design by Hexagon PPM,Ver:20.0 Operator : Rev.:A

EN13445:2014 Issue 5:2018+A5 - 9.5 ISOLATED OPENINGS IN SHELLS

N.2 Outlet 17 Aug. 2023 11:35 ConnID:E3.2

## WELDING DATA

Nozzle/Pad to Shell Welding Area: Exclude Area of Nozzle to Shell Weld  
Nozzle Weld Intersect: Nozzle Does NOT Intersect with a Welded Shell Seam  
ANGLE BETWN.BRANCH AXIS AND A LINE NORMAL TO MAIN BODY:Phi 0.00 Degr.

## DATA FOR REINFORCEMENT PAD



Type of Pad: No Pad

## LIMITS OF REINFORCEMENT

Reduction of Limits of Reinforcement: No Reduction Required

## WELDING REQUIREMENTS TO EN 1708-1:2010

Comment(Optional):

Type of welded connection: Not Applicable

## CALCULATION DATA

### PRELIMINARY CALCULATIONS

Shell Analysis Thickness eas 3.2000 mm  
 $eas = en - c - th = 4 - 0.5 - 0.3 =$   
Nozzle Analysis Thickness eab 3.8750 mm  
 $eab = enb - cn - NegDev = 5 - 0.5 - 0.625 =$   
 $ris = R (9.5 - 4) = 218.4 =$  218.40 mm  
 $dib = deb - 2 * eab = 74.5 - 2 * 3.875 =$  66.75 mm  
Min.Nozzle Thk.Based on Internal Pressure ebp  
 $ebp = P * deb / (2 * fb * z + P)$   
 $= 3.3 * 74.5 / (2 * 145.47 * 1 + 3.3) =$  0.8400 mm  
Allowable Stresses  
 $fob = Min( fs, fb ) (9.5 - 8) = Min(205.73, 145.47) =$  145.47 N/mm<sup>2</sup>

### GEOMETRIC LIMITATIONS

»Check Max.Diameter of Nozzle  $dib/De = 0.2445 \leq 0.60 = 0.6 [mm] (9.4.5.3) \llcorner \llcorner$  OK«

Min.Nozzle Thk. $ebp = 0.84 \leq eab = 3.875 [mm]$	21.6%	OK
--	-------	----

»Location in End to Fig.9.5-4  $L = 99.25 \geq De/10 = 27.3 [mm] \llcorner \llcorner$  OK«

## 9.5.2.4.4 Nozzles normal to the shell, with or without reinforcement pads.

### Calculation of Stress Loaded Areas Effective as Reinforcement

#### Area of Shell Afs

Limit of Reinforcement Along Shell  
 $Iso = Sqr(( 2 * ris + eas) * eas)$  37.52 mm  
 $= Sqr(( 2 * 218.4 + 3.2) * 3.2) =$   
Set In Nozzle  
 $Afs = eas * Iso (9.5-79) = 3.2 * 37.52 =$  120.07 mm<sup>2</sup>

#### Area of Nozzle Afb

Limit of Reinforcement Along Nozzle (outside shell)  
 $Ibo = MIN( Sqr(( deb - eb) * eb), ho)$  (9.5-76)  
 $= MIN(Sqr(( 74.5 - 3.875) * 3.875), 40) =$  16.54 mm  
Set In Nozzle  
 $Afb = eb * (Ibo + Ibi + eas) (9.5-78) = 3.875 * (16.54 + 0 + 3.2) =$  76.50 mm<sup>2</sup>

# Company Name -

Client :GÜVEN SOGUTMA

Vessel Tag No.:OS.HF.33B.66.1

Visual Vessel Design by Hexagon PPM,Ver:20.0 Operator : Rev.:A

EN13445:2014 Issue 5:2018+A5 - 9.5 ISOLATED OPENINGS IN SHELLS

N.2 Outlet

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## Calculation of Pressure Loaded Areas

In the Nozzle Apb

$$Apb = 0.5 * dib * (Ibo + eas) \quad (9.5-84) = 0.5 * 66.75 * (16.54 + 3.2) = 658.92 \text{ mm}^2$$

Spherical Shell/End on any Section Aps

$$Aps = 0.5 * ris^2 * (Is + a) / (0.5 * eas + ris) \quad (9.5-105) \\ = 0.5 * 218.4^2 * (37.52 + 37.43) / (0.5 * 3.2 + 218.4) = 8125.41 \text{ mm}^2$$

## 9.5.2 Reinforcement Rules

### Pressure Area Required pA(req.)

$$pAReq = P * (Aps + Apb + 0.5 * Apphi) \quad (9.5-7) \\ = 3.3 * (8125.41 + 658.92 + 0.5 * 0) = 28.99 \text{ kN}$$

### Pressure Area Available pA(aval.)

$$pAAval = (Afs + Afw) * (fs - 0.5 * P) + Afp * (fop - 0.5 * P) + Afb * (fob - 0.5 * P) \quad (9.5-7) \\ = (120.07 + 0) * (205.73 - 0.5 * 3.3) + 0 * (0 - 0.5 * 3.3) + 76.5 * (145.47 - 0.5 * 3.3) = 35.51 \text{ kN}$$

Nozzle Reinforcement pAAval=35.51 >= pAReq=28.99[kN]

81.6%

OK

### Maximum Allowable Pressure Pmax

$$Pmax = (Afs + Afw) * fs + Afb * fob / ((Aps + Apb + 0.5 * Apphi) + 0.5 * (Afs + Afw + Afb + Afp)) \quad (9.5-10) \\ = (120.07 + 0) * 205.73 + 76.5 * 145.47 / ((8125.41 + 658.92 + 0.5 * 0) + 0.5 * (120.07 + 0 + 76.5 + 0)) = 4.0339 \text{ MPa}$$

### Max.Allowable Test Pressure Ptmax

$$Ptmax = == 7.7263 \text{ MPa}$$

Weight of Nozzle: .4045kg

## CALCULATION SUMMARY

Min.Nozzle Thk. ebp=0.84 <= eab=3.875[mm]

21.6%

OK

### 9.5.2.4.4 Nozzles normal to the shell, with or without reinforcement pads.

Limit of Reinforcement Along Shell

$$Iso = \text{Sqr}((2 * ris + eas) * eas) \\ = \text{Sqr}((2 * 218.4 + 3.2) * 3.2) = 37.52 \text{ mm}$$

Limit of Reinforcement Along Nozzle (outside shell)

$$Ibo = \text{MIN}(\text{Sqr}((deb - eb) * eb), ho) \quad (9.5-76) \\ = \text{MIN}(\text{Sqr}((74.5 - 3.875) * 3.875), 40) = 16.54 \text{ mm}$$

### Pressure Area Required pA(req.)

$$pAReq = P * (Aps + Apb + 0.5 * Apphi) \quad (9.5-7) \\ = 3.3 * (8125.41 + 658.92 + 0.5 * 0) = 28.99 \text{ kN}$$

### Pressure Area Available pA(aval.)

$$pAAval = (Afs + Afw) * (fs - 0.5 * P) + Afp * (fop - 0.5 * P) + Afb * (fob - 0.5 * P) \quad (9.5-7) \\ = (120.07 + 0) * (205.73 - 0.5 * 3.3) + 0 * (0 - 0.5 * 3.3) + 76.5 * (145.47 - 0.5 * 3.3) = 35.51 \text{ kN}$$

Nozzle Reinforcement pAAval=35.51 >= pAReq=28.99[kN]

81.6%

OK

### Maximum Allowable Pressure Pmax

$$Pmax = (Afs + Afw) * fs + Afb * fob / ((Aps + Apb + 0.5 * Apphi) + 0.5 * (Afs + Afw + Afb + Afp)) \quad (9.5-10) \\ = (120.07 + 0) * 205.73 + 76.5 * 145.47 / ((8125.41 + 658.92 + 0.5 * 0) + 0.5 * (120.07 + 0 + 76.5 + 0)) = 4.0339 \text{ MPa}$$

**Company Name -**

Client :GÜVEN SOGUTMA

Vessel Tag No.:OS.HF.33B.66.1

Visual Vessel Design by Hexagon PPM,Ver:20.0 Operator : Rev.:A

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Volume:0.0001000 m3 Weight:0.4 kg (SG= 7.85 )

**Company Name -**

Client :GÜVEN SOGUTMA

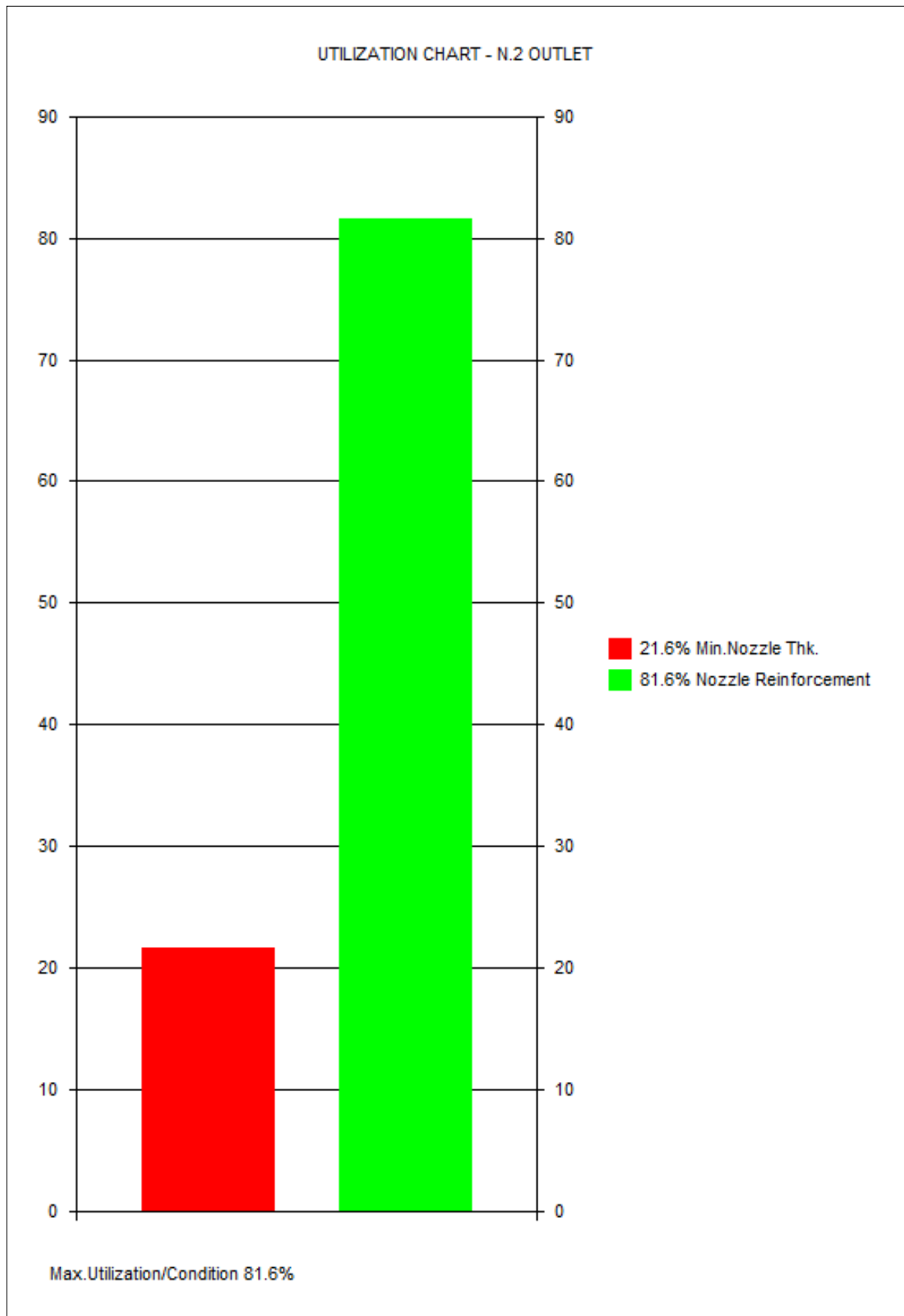
Vessel Tag No.:OS.HF.33B.66.1

Visual Vessel Design by Hexagon PPM,Ver:20.0 Operator : Rev.:A

EN13445:2014 Issue 5:2018+A5 - 9.5 ISOLATED OPENINGS IN SHELLS

N.2 Outlet

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# Company Name -

Client :GÜVEN SOGUTMA

Vessel Tag No.:OS.HF.33B.66.1

Visual Vessel Design by Hexagon PPM,Ver:20.0 Operator : Rev.:A

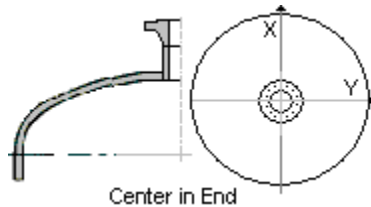
EN13445:2014 Issue 5:2018+A5 - 9.5 ISOLATED OPENINGS IN SHELLS

N.3 Float Shell 17 Aug. 2023 11:35 ConnID:E3.1

## INPUT DATA

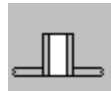
### COMPONENT ATTACHMENT/LOCATION

Attachment: E3.1 Torispherical End Bottom Head S1.1  
Connect this nozzle to the nozzle neck of another nozzle: NO



Orientation & Location of Nozzle: Center in End

### GENERAL DESIGN DATA



Type of Opening: Nozzle Without Standard ASME or DIN/EN Flange Attachment  
PRESSURE LOADING: Design Component for Internal Pressure Only

PROCESS CARD:

General Design Data : Temp= 130°C, P=3.3000 MPa, c=0.5 mm, Pext=0.0000 MPa

SPECIFIC DENSITY OF OPERATING LIQUID.....:SG 0.00

LIQUID HEAD.....:LH 84.84 mm

Apply a different corrosion allowance to nozzle neck than the shell thickness.: NO

Include Nozzle Load Calculation: NO

### SHELL DATA (E3.1)

Shell Type: Torispherical End

OUTSIDE DIAMETER OF SHELL.....:De 273.00 mm

NOMINAL WALL THICKNESS (uncorroded).....:en 4.0000 mm

NEGATIVE TOLERANCE/THINNING ALLOWANCE.....:th 0.3000 mm

INSIDE SPHERICAL RADIUS (corroded).....:R 218.40 mm

EN 10028-2:2017, 1.0473 P355GH plate and strip, HT:N THK<=16mm 130'C

Rm=510 Rp=355 Rpt=308.6 fs=205.73 f20=212.5 ftest=338.1 E=203868(N/mm2) ro=7.85

### NOZZLE MATERIAL DATA

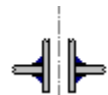


Delivery Form: Seamless Pipe

EN 10217-3:2019, 1.0565 P355NH welded tube, HT:N THK<=20mm 130'C

Rm=490 Rp=355 Rpt=292 fb=194.67 f20=204.17 ftest=338.1 E=203868(N/mm2) ro=7.85

### NOZZLE DIMENSIONAL DATA



Attachment: Protruding Nozzle

Shape of Nozzle/Opening: Circular

Application:

9.4.6.3 NOT a critical fatigue area, and calc.temp.is outside creep range.

OUTSIDE NOZZLE DIAMETER.....:deb 101.60 mm

NOMINAL NOZZLE THICKNESS (uncorroded).....:enb 3.0000 mm

Size of Flange and Nozzle:

Comment (Optional):

NEGATIVE TOLERANCE/THINNING ALLOWANCE.....: 10.00 %

NOZZLE STANDOUT MEASURED FROM VESSEL OD.....:ho 40.00 mm

# Company Name -

Client :GÜVEN SOGUTMA

Vessel Tag No.:OS.HF.33B.66.1

Visual Vessel Design by Hexagon PPM,Ver:20.0 Operator : Rev.:A

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N.3 Float Shell 17 Aug. 2023 11:35 ConnID:E3.1

PROTRUDING MEASURED FROM SHELL ris (corroded).....:Ibi 20.00 mm

## WELDING DATA

Nozzle/Pad to Shell Welding Area: User Specified Fillet Weld Throat Dimensions

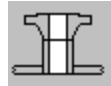
OUTWARD NOZZLE WELD, THROAT DIMENSION.....:mo 2.2000 mm

INWARD NOZZLE WELD, THROAT DIMENSION.....:mi 2.2000 mm

Nozzle Weld Intersect: Nozzle Does NOT Intersect with a Welded Shell Seam

ANGLE BETWN.BRANCH AXIS AND A LINE NORMAL TO MAIN BODY:Phi 0.00 Degr.

## DATA FOR REINFORCEMENT PAD



Type of Pad: No Pad

## LIMITS OF REINFORCEMENT

Reduction of Limits of Reinforcement: No Reduction Required

## WELDING REQUIREMENTS TO EN 1708-1:2010

Comment(Optional):

Type of welded connection: Not Applicable

## CALCULATION DATA

### PRELIMINARY CALCULATIONS

Shell Analysis Thickness eas

$eas = en - c - th = 4 - 0.5 - 0.3 = 3.2000$  mm

Nozzle Analysis Thickness eab

$eab = enb - cn - NegDev = 3 - 0.5 - 0.3 = 2.2000$  mm

$ris = R (9.5 - 4) = 218.4 = 218.40$  mm

$dib = deb - 2 * eab = 101.6 - 2 * 2.2 = 97.20$  mm

Min.Nozzle Thk.Based on Internal Pressure ebp

$ebp = P * deb / (2 * fb * z + P) = 3.3 * 101.6 / (2 * 194.67 * 1 + 3.3) = 0.8500$  mm

Allowable Stresses

$fob = \text{Min}( fs, fb ) (9.5 - 8) = \text{Min}(205.73, 194.67) = 194.67$  N/mm<sup>2</sup>

### GEOMETRIC LIMITATIONS

»Check Max.Diameter of Nozzle  $dib/De = 0.356 \leq 0.60 = 0.6$ [mm] (9.4.5.3)«» OK«

Min.Nozzle Thk. $ebp = 0.85 \leq eab = 2.2$ [mm]	38.6%	OK
--	-------	----

»Location in End to Fig.9.5-4  $L = 85.7 \geq De/10 = 27.3$ [mm] « » OK«

## 9.5.2.4.4 Nozzles normal to the shell, with or without reinforcement pads.

### Calculation of Stress Loaded Areas Effective as Reinforcement

#### Area of Shell Afs

Limit of Reinforcement Along Shell

$Iso = \text{Sqr}((2 * ris + eas) * eas) = \text{Sqr}((2 * 218.4 + 3.2) * 3.2) = 37.52$  mm

Set In Nozzle

$Afs = eas * Iso (9.5 - 79) = 3.2 * 37.52 = 120.07$  mm<sup>2</sup>

#### Area of Nozzle Afb

Limit of Reinforcement Along Nozzle (outside shell)

$Ibo = \text{MIN}( \text{Sqr}((deb - eb) * eb), ho ) (9.5 - 76) = \text{MIN}( \text{Sqr}((101.6 - 2.2) * 2.2), 40) = 14.79$  mm

Limit of Reinforcement Along Nozzle (inside shell)

$Ibi = \text{Min}( Ibi, 0.5 * Ibo ) = \text{Min}(20, 0.5 * 14.79) = 7.3939$  mm

Set In Nozzle



# Company Name -

Client :GÜVEN SOGUTMA

Vessel Tag No.:OS.HF.33B.66.1

Visual Vessel Design by Hexagon PPM,Ver:20.0 Operator : Rev.:A

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N.3 Float Shell 17 Aug. 2023 11:35 ConnID:E3.1

$$Afb = eb * (Ibo + Ibi + eas) (9.5-78) = 2.2 * (14.79 + 7.39 + 3.2) = 55.84 \text{ mm}^2$$

## Area of Welds Afw

$$Afw = mo^2 + (mi - c)^2 = 2.2^2 + (2.2 - 0.5)^2 = 7.7300 \text{ mm}^2$$

## Calculation of Pressure Loaded Areas

In the Nozzle Apb

$$Apb = 0.5 * dib * (Ibo + eas) (9.5-84) = 0.5 * 97.2 * (14.79 + 3.2) = 874.21 \text{ mm}^2$$

Spherical Shell/End on any Section Aps

$$Aps = 0.5 * ris^2 * (Is + a) / (0.5 * eas + ris) (9.5-105) \\ = 0.5 * 218.4^2 * (37.52 + 51.26) / (0.5 * 3.2 + 218.4) = 9624.91 \text{ mm}^2$$

## 9.5.2 Reinforcement Rules

### Pressure Area Required pA(req.)

$$pAReq = P * (Aps + Apb + 0.5 * Apphi) (9.5-7) \\ = 3.3 * (9624.91 + 874.21 + 0.5 * 0) = 34.65 \text{ kN}$$

### Pressure Area Available pA(aval.)

$$pAAval = (Afs + Afw) * (fs - 0.5 * P) + Afp * (fop - 0.5 * P) + Afb * (fob - 0.5 * P) (9.5-7) \\ = (120.07 + 7.73) * (205.73 - 0.5 * 3.3) + 0 * (0 - 0.5 * 3.3) + 55.84 * (194.67 - 0.5 * 3.3) \\ = 36.86 \text{ kN}$$

**Nozzle Reinforcement pAAval=36.86 >= pAReq=34.65[kN]****93.9%****OK**

### Maximum Allowable Pressure Pmax

$$Pmax = (Afs + Afw) * fs + Afb * fob / ((Aps + Apb + 0.5 * Apphi) + 0.5 * (Afs + Afw + Afb + Afp)) (9.5-10) \\ = (120.07 + 7.73) * 205.73 + 55.84 * 194.67 / ((9624.91 + 874.21 + 0.5 * 0) + 0.5 * (120.07 + 7.73 \\ + 55.84 + 0)) = 3.5090 \text{ MPa}$$

### Max.Allowable Test Pressure Ptmax

$$Ptmax = == 6.8565 \text{ MPa}$$

Weight of Nozzle: .5106kg

## CALCULATION SUMMARY

**Min.Nozzle Thk. ebp=0.85 <= eab=2.2[mm]****38.6%****OK**

### 9.5.2.4.4 Nozzles normal to the shell, with or without reinforcement pads.

Limit of Reinforcement Along Shell

$$Iso = Sqr((2 * ris + eas) * eas) \\ = Sqr((2 * 218.4 + 3.2) * 3.2) = 37.52 \text{ mm}$$

Limit of Reinforcement Along Nozzle (outside shell)

$$Ibo = MIN(Sqr((deb - eb) * eb), ho) (9.5-76) \\ = MIN(Sqr((101.6 - 2.2) * 2.2), 40) = 14.79 \text{ mm}$$

Limit of Reinforcement Along Nozzle (inside shell)

$$Ibi = Min(Ibi, 0.5 * Ibo) = Min(20, 0.5 * 14.79) = 7.3939 \text{ mm}$$

### Pressure Area Required pA(req.)

$$pAReq = P * (Aps + Apb + 0.5 * Apphi) (9.5-7) \\ = 3.3 * (9624.91 + 874.21 + 0.5 * 0) = 34.65 \text{ kN}$$

### Pressure Area Available pA(aval.)

$$pAAval = (Afs + Afw) * (fs - 0.5 * P) + Afp * (fop - 0.5 * P) + Afb * (fob - 0.5 * P) (9.5-7) \\ = (120.07 + 7.73) * (205.73 - 0.5 * 3.3) + 0 * (0 - 0.5 * 3.3) + 55.84 * (194.67 - 0.5 * 3.3) \\ = 36.86 \text{ kN}$$

**Nozzle Reinforcement pAAval=36.86 >= pAReq=34.65[kN]****93.9%****OK**

**Company Name -**

Client :GÜVEN SOGUTMA

Vessel Tag No.:OS.HF.33B.66.1

Visual Vessel Design by Hexagon PPM,Ver:20.0 Operator : Rev.:A

EN13445:2014 Issue 5:2018+A5 - 9.5 ISOLATED OPENINGS IN SHELLS

N.3 Float Shell 17 Aug. 2023 11:35 ConnID:E3.1

**Maximum Allowable Pressure Pmax**

$$P_{max} = (A_{fs}+A_{fw}) * f_s + A_{fb} * f_{ob} / ((A_{ps}+A_{pb}+0.5 * A_{phi}) + 0.5 * (A_{fs}+A_{fw}+A_{fb}+A_{fp})) (9.5-10)$$
$$= (120.07+7.73) * 205.73 + 55.84 * 194.67 / ((9624.91+874.21+0.5 * 0) + 0.5 * (120.07+7.73 + 55.84+0)) = \underline{\underline{3.5090 \text{ MPa}}}$$

Volume:0.0003000 m3 Weight:0.5 kg (SG= 7.85 )

**Company Name -**

Client :GÜVEN SOGUTMA

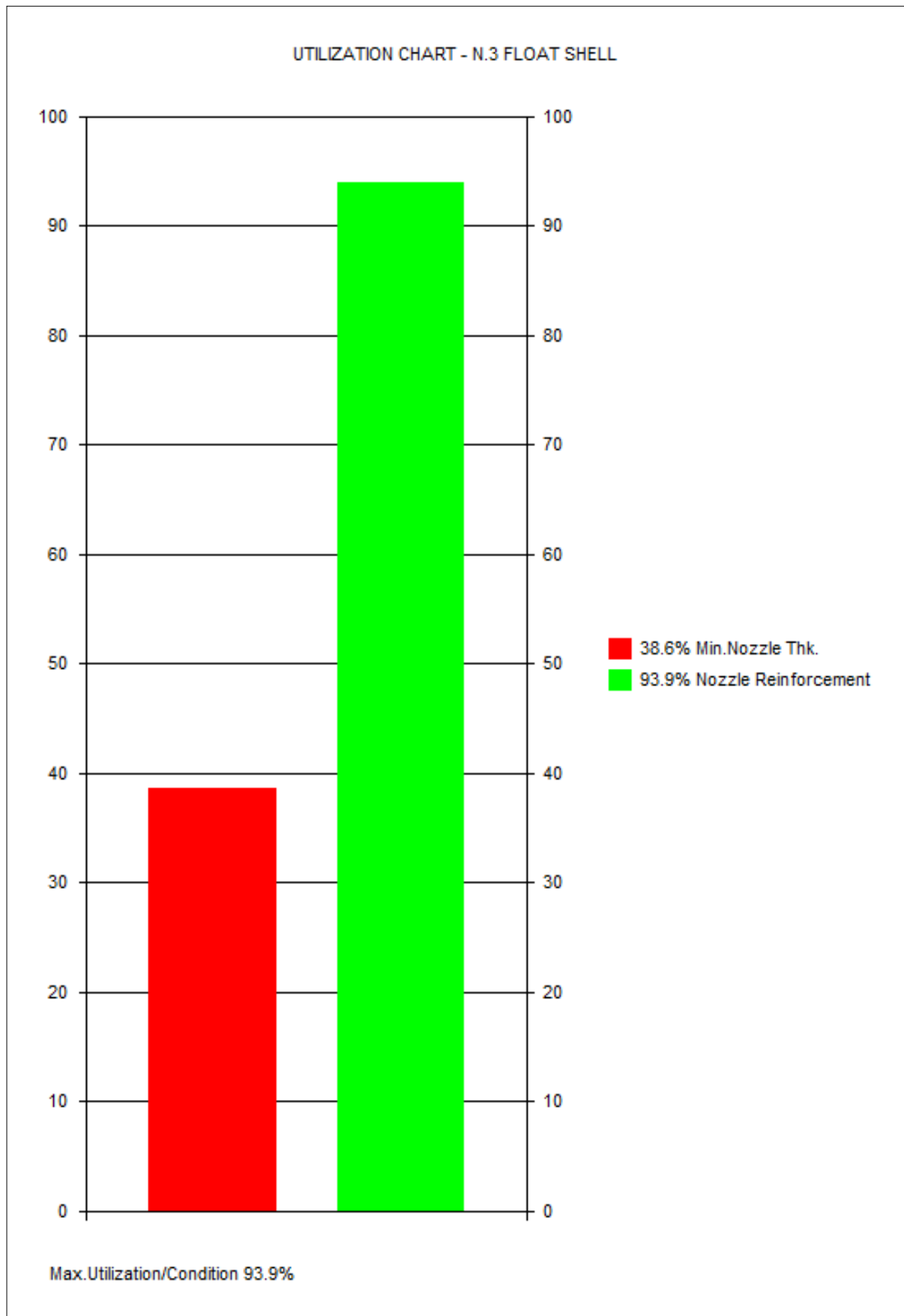
Vessel Tag No.:OS.HF.33B.66.1

Visual Vessel Design by Hexagon PPM,Ver:20.0 Operator : Rev.:A

EN13445:2014 Issue 5:2018+A5 - 9.5 ISOLATED OPENINGS IN SHELLS

N.3 Float Shell

17 Aug. 2023 11:35 ConnID:E3.1



# Company Name -

Client :GÜVEN SOGUTMA

Vessel Tag No.:OS.HF.33B.66.1

Visual Vessel Design by Hexagon PPM,Ver:20.0 Operator : Rev.:A

EN13445:2014 Issue 5:2018+A5 - 11.5 NARROW FACE GASKETED FLANGES

F.1 Ring Flange 17 Aug. 2023 11:35 ConnID:N.3

## INPUT DATA

### COMPONENT ATTACHMENT/LOCATION

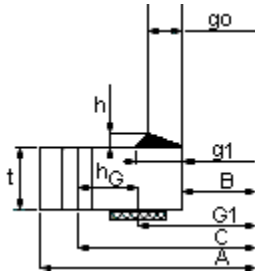
Attachment: N.3 Nozzle,Seamless Pipe Float Shell E3.1  
Location: Along z-axis z1= -42  
Flange Design Method: Section 11 - Taylor Forge

### GENERAL DESIGN DATA

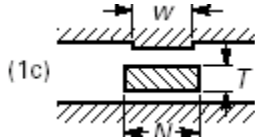
PROCESS CARD: General Design Data : Temp= 130°C, P=3.3000 MPa, c=0.5 mm  
SPECIFIC DENSITY OF OPERATING LIQUID.....:SG 0.00  
LIQUID HEAD.....:LH 126.84 mm  
B: Pressure loading: Flange under internal pressure  
EXTERNAL LOADS ON FLANGE (PD5500 ENQ 5500/123): NO  
SPECIFY BOLT LOADS FROM 2nd./MATING FLANGE: NO

### TYPE OF FLANGE AND GASKET FACING

A: Flange Standard: User Specified Flanges



C: Flange Type: RT Ring Type(Smooth or Stepped bore)



D: Flange Facing (Sketch/Description): 1c Tongue & Groove

### SHELL/NOZZLE DATA

SHELL/NOZZLE SIZE & COMMENT: N.3  
EN 10217-3:2019, 1.0565 P355NH welded tube, HT:N THK<=20mm 130'C  
Rm=490 Rp=355 Rpt=292 fs=194.67 fs20=204.17 ftest=338.1 E=203868(N/mm<sup>2</sup>) ro=7.85  
OUTSIDE DIAMETER OF SHELL/NOZZLE .....:Do 101.60 mm  
WALL THICKNESS OF NOZZLE/SHELL(uncorroded).....:s1 3.0000 mm

### FLANGE DATA

FLANGE HUB: Flange With Hub  
REVERSE FLANGE: No (The bolts are located on the outside)  
DESIGN METHOD: A) INTEGRAL FLANGE METHOD  
FLANGE BORE: Smooth  
OUTSIDE DIAMETER OF FLANGE.....:A 149.00 mm  
THICKNESS OF FLANGE(uncorroded).....:e 11.00 mm  
THICKNESS OF FLANGE AT REDUCED SECTION.....:er 11.00 mm  
CORROSION ALLOWANCE FOR FLANGE FACE.....:cf 0.00 mm  
EN 10028-2:2017, 1.0473 P355GH plate and strip, HT:N THK<=16mm 130'C  
Rm=510 Rp=355 Rpt=308.6 SFO=205.73 SFA=212.5 ftest=338.1 E=203868(N/mm<sup>2</sup>) ro=7.85

### DATA FOR FLANGE HUB

LENGTH OF HUB.....:h 6.0000 mm  
THICKNESS OF HUB AT BACK OF FLANGE corroded.....:g1 6.0000 mm  
THICKNESS OF HUB AT SMALL END corroded.....:go 3.0000 mm  
EN 10028-2:2017, 1.0473 P355GH plate and strip, HT:N THK<=16mm 130'C  
Rm=510 Rp=355 Rpt=308.6 SHO=205.73 SHA=212.5 ftest=338.1 E=203868(N/mm<sup>2</sup>) ro=7.85

# Company Name -

Client :GÜVEN SOGUTMA

Vessel Tag No.:OS.HF.33B.66.1

Visual Vessel Design by Hexagon PPM,Ver:20.0 Operator : Rev.:A

EN13445:2014 Issue 5:2018+A5 - 11.5 NARROW FACE GASKETED FLANGES

F.1 Ring Flange 17 Aug. 2023 11:35 ConnID:N.3

## BOLTING DATA

REDUCE SAFETY AGAINST ABUSE BY CAREFULLY CONTROLLING THE BOLTING-UP TORQUE: NO  
BOLTING TORQUE CALCULATION: NO

NOMINAL BOLTING SIZE & COMMENT: M8x1.5 ;

EFFECTIVE BOLT AREA per bolt.....:Ae	36.60 mm <sup>2</sup>
RECOMMENDED MINIMUM BOLT CENTER TO EDGE CLEARANCE...:Bce	12.00 mm
RECOMMENDED MINIMUM BOLT CENTER/RADIAL CLEARANCE....:Bcr	16.00 mm
DIAMETER OF BOLT HOLES IN FLANGE.....:d	10.00 mm
NUMBER OF BOLTS.....:n	8.0000
BOLT-CIRCLE DIAMETER.....:C	130.00 mm

8.8 DIN 267 THK<=30mm 130'C

Rm=800 Rp=640 Rpt=575 Sb=191.67 Sa=200 ftest=300 (N/mm<sup>2</sup>)

NOTE: A PARTICULAR MATERIAL APPRAISAL(PMA) MAY BE REQUIRED FOR THIS MATERIAL.

## GASKET DATA

Table H-1 Gasket factors m & y Facing:

Mineral Fiber 3.2 mm thick m=2.0 Y=11.0 2 1a,1b,1c,1d,4,5

OUTSIDE DIAMETER OF GASKET/RAISED FACE.....:Go 102.50 mm

GREATER VALUE OF INSIDE DIAMETER OF GASKET/FLANGE FACE:A1 94.50 mm

TEMA RGP-RCB-11.7 Include Additional Loads from Pass Partition Plate Gasket: NO

## WELDING REQUIREMENTS TO EN 1708-1:2010

Comment(Optional):

Type of welded connection: Not Applicable

## CALCULATION DATA

Large Diameter Stress Correction Factor K

k (D < 1000 mm) = 1 =1= 1.0000

## GASKET DETAILS

b = MIN VALUE(2.52 \* Sqr(bo), bo ) = = 2.0000 mm

## FLANGE LOADS

HD = 0.785 \* B ^ 2 \* p =0.785\*96.6^2\*3.3= 24.17 kN

H = 0.785 \* G ^ 2 \* p (11.5-5) =0.785\*98.5^2\*3.3= 25.13 kN

HG = (2 \* PI \* b \* G \* m) \* p (11.5-6) =(2\*3.14\*2\*98.5\*2)\*3.3= 8.1694 kN

HT = H - HD (11.5-11) =25133.68-24173.41= 0.9603 kN

## MOMENT ARMS

hG = (C - G) / 2 (11.5-14) =(130-98.5)/2= 15.75 mm

hD = (C - B - g1) / 2 (11.5-12) =(130-96.6-6)/2= 13.70 mm

hT = (2 \* C - B - G) / 4 (11.5-15) =(2\*130-96.6-98.5)/4= 16.23 mm

## BOLT LOADS

Operating condition

Wop = H + HG (11.5-8) =25133.68+8169.4= 33.30 kN

Bolting up condition

Wamb = PI \* b \* G \* y (11.5-7) =3.14\*2\*98.5\*11= 6.8078 kN

## BOLTING AREA

Am1 = Wop / Sb =33303.08/191.67= 173.75 mm<sup>2</sup>

Am2 = Wamb / Sa =6807.83/200= 34.04 mm<sup>2</sup>

Required Bolting Area Am

Am = MAX( Am1 , Am2) =MAX(173.75,34.04)= 173.75 mm<sup>2</sup>

Available Bolting Area Ab

Ab (num.bolts\*root area) = n \* Ae =8\*36.6= 292.80 mm<sup>2</sup>

**Bolting Area Check Ab=292.8 >= Am=173.75[mm<sup>2</sup>]**

**59.3%**

**OK**

W = 0.5 \* (Ab + Am) \* Sa (11.5-16) =0.5\*(292.8+173.75)\*200= 46.66 kN

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## FLANGE MOMENTS

$$Mop = HD * hD + HT * hT + HG * hG \quad (11.5-18)$$

$$=24173.41*13.7+960.27*16.225+8169.4*15.75= \quad 475.42 \text{ Nm}$$

$$Mamb = W * hG \quad (11.5-17) =46655.22*15.75= \quad 734.82 \text{ Nm}$$

Bolt Spacing

$$Bs = C * PI / n =130*3.14/8= \quad 51.05 \text{ mm}$$

Bolt Pitch Correction Factor

$$CF = MAX( Sqr( Bs / (2 * db + 6 * e / (m + 0.5))) , 1) \quad (11.5-20)$$

$$=MAX(Sqr(51.05/(2*8+6*11/(2+0.5))),1)= \quad 1.1000$$

$$Mo = Mop * CF / B \quad (11.5-27) =475.42*1.1/96.6= \quad 5.4137 \text{ Nm/mm}$$

$$Ma = Mamb * CF / B \quad (11.5-26) =734.82*1.1/96.6= \quad 8.3675 \text{ Nm/mm}$$

## SHAPE CONSTANTS

$$K = A / B \quad (11.5-21) =149/96.6= \quad 1.5424$$

$$lo = SQR( B * go) \quad (11.5-22) =SQR(96.6*3)= \quad 17.02$$

$$h/lo= 0.352 \quad K=A/B= 1.542 \quad g1/go= 2.000$$

VALUES FROM FIGURES 11.5-4 to 8

$$BetaT = 1.692 \quad BetaZ = 2.450 \quad BetaY = 4.654 \quad BetaU = 5.114$$

$$BetaF= 0.859 \quad BetaV = 0.278 \quad phi = 1.821$$

$$lamda = (e*BetaF+lo)/(BetaT*lo)+e^3*BetaV/(BetaU*lo*go^2)$$

$$=(11*0.8588+17.02)/(1.692*17.02)+11^3*0.2782/(5.114*17.02*3^2)= \quad 1.3916$$

## OPERATING CONDITION

$$M = Mo =5.41= \quad 5.4137 \text{ Nm/mm}$$

### 11.5.4.1 Flange Stresses with Flange Thickness e= 11 mm

Longitudinal Hub Stress

$$SigH = phi * M / (lamda * g1 ^ 2) \quad (11.5-32)$$

$$=1.82*5.41/(1.39*6^2)= \quad 196.74 \text{ N/mm}^2$$

Radial Flange Stress

$$Sigr = (1.333 * e * BetaF + lo) * M / (lamda * e ^ 2 * lo) \quad (11.5-33)$$

$$=(1.333*11*0.8588+17.02)*5.41/(1.39*11^2*17.02)= \quad 55.93 \text{ N/mm}^2$$

Tangential Flange Stress

$$SigTeta = BetaY*M/e^2-Sigr*(K^2+1)/(K^2-1) \quad (11.5-34)$$

$$=4.654*5.41/11^2-55.93*(1.54^2+1)/(1.54^2-1)= \quad 71.18 \text{ N/mm}^2$$

### 11.5.4.2 Stress Limits

Hub Stress $k*SigH=196.74 \leq 1.5 * MIN(f;fH)=308.59[N/mm^2]$ (11.5-90)	63.7%	OK
Radial Stress $k*SigR=55.93 \leq f=205.73[N/mm^2]$ (11.5-91)	27.1%	OK
Tangential Stress $k*SigTeta=71.18 \leq f=205.73[N/mm^2]$ (11.5-92)	34.5%	OK
Radial+Hub Stress $0.5*k*(SigH+SigR)=126.33 \leq f=205.73[N/mm^2]$ (11.5-93)	61.4%	OK
Tangential+Hub Stress $0.5*k*(SigH+SigTeta)=133.96 \leq f=205.73[N/mm^2]$ (11.5-94)	65.1%	OK

## BOLTING UP CONDITION

$$M = Ma =8.37= \quad 8.3675 \text{ Nm/mm}$$

### 11.5.4.1 Flange Stresses with Flange Thickness e= 11 mm

Longitudinal Hub Stress

$$SigH = phi * M / (lamda * g1 ^ 2) \quad (11.5-32)$$

$$=1.82*8.37/(1.39*6^2)= \quad 304.08 \text{ N/mm}^2$$

Radial Flange Stress

$$Sigr = (1.333 * e * BetaF + lo) * M / (lamda * e ^ 2 * lo) \quad (11.5-33)$$

$$=(1.333*11*0.8588+17.02)*8.37/(1.39*11^2*17.02)= \quad 86.45 \text{ N/mm}^2$$

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## Tangential Flange Stress

$$\text{SigTeta} = \text{BetaY} * \text{M} / \text{e}^2 - \text{Sigr} * (\text{K}^2 + 1) / (\text{K}^2 - 1) \quad (11.5-34)$$

$$= 4.654 * 8.37 / 11^2 - 86.45 * (1.54^2 + 1) / (1.54^2 - 1) = 110.02 \text{ N/mm}^2$$

## 11.5.4.2 Stress Limits

Hub Stress $k * \text{SigH} = 304.08 \leq 1.5 * \text{MIN}(f; f_H) = 318.75 [\text{N/mm}^2]$ (11.5-90)	95.3%	OK
Radial Stress $k * \text{SigR} = 86.45 \leq f = 212.5 [\text{N/mm}^2]$ (11.5-91)	40.6%	OK
Tangential Stress $k * \text{SigTeta} = 110.02 \leq f = 212.5 [\text{N/mm}^2]$ (11.5-92)	51.7%	OK
Radial+Hub Stress $0.5 * k * (\text{SigH} + \text{SigR}) = 195.26 \leq f = 212.5 [\text{N/mm}^2]$ (11.5-93)	91.8%	OK
Tangential+Hub Stress $0.5 * k * (\text{SigH} + \text{SigTeta}) = 207.05 \leq f = 212.5 [\text{N/mm}^2]$ (11.5-94)	97.4%	OK

## EN13445-5;10.2.3.3 REQUIRED MIN.HYDROSTATIC TEST PRESSURE:Ptmin

NEW AT AMBIENT TEMP. FOR TEST GROUPS 1, 2 and 3

$$\text{Ptmin} = 1.25 * \text{Pd} * f_{20} / f = 1.25 * 3.3 * 212.5 / 205.73 = 4.2607 \text{ MPa}$$

$$\text{Ptmin} = 1.43 * \text{Pd} = 1.43 * 3.3 = 4.7190 \text{ MPa}$$

Test Pressure  $\text{Ptmin} = 4.72 \leq \text{Pmax} = 7.197 [\text{MPa}]$  65.5% OK

## PRESSURE AND TORQUE SUMMARY

Table PRESSURE AND TORQUE SUMMARY FOR F.1 :

Description	Temp(C)	P(MPa)	Limited By	Min.Req.Total Bolt Force(kN)
Design Pressure(corroded)	130	3.30	Tangential+Hub Stress	33.3
Max.Allow.Pressure(corroded)	130	3.54	Tangential+Hub Stress	35.7
Max.Allow.Pressure(corroded)	Ambient	3.70	Tangential+Hub Stress	37.3
Max.Allow.Test Pressure(corroded)	Ambient	7.20	Tangential+Hub Stress	72.63
Required Test Pressure	Ambient	4.26	Tangential+Hub Stress	43

The nominal Force and Torque values are based on the following bolting up method:

## CALCULATION SUMMARY

### BOLTING AREA

Bolting Area Check  $\text{Ab} = 292.8 \geq \text{Am} = 173.75 [\text{mm}^2]$  59.3% OK

## OPERATING CONDITION

### 11.5.4.1 Flange Stresses with Flange Thickness $e = 11 \text{ mm}$

#### Longitudinal Hub Stress

$$\text{SigH} = \text{phi} * \text{M} / (\text{lamda} * \text{gl}^2) \quad (11.5-32)$$

$$= 1.82 * 5.41 / (1.39 * 6^2) = 196.74 \text{ N/mm}^2$$

#### Radial Flange Stress

$$\text{Sigr} = (1.333 * e * \text{BetaF} + \text{lo}) * \text{M} / (\text{lamda} * e^2 * \text{lo}) \quad (11.5-33)$$

$$= (1.333 * 11 * 0.8588 + 17.02) * 5.41 / (1.39 * 11^2 * 17.02) = 55.93 \text{ N/mm}^2$$

#### Tangential Flange Stress

$$\text{SigTeta} = \text{BetaY} * \text{M} / \text{e}^2 - \text{Sigr} * (\text{K}^2 + 1) / (\text{K}^2 - 1) \quad (11.5-34)$$

$$= 4.654 * 5.41 / 11^2 - 55.93 * (1.54^2 + 1) / (1.54^2 - 1) = 71.18 \text{ N/mm}^2$$

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**11.5.4.2 Stress Limits**

Hub Stress $k \cdot \text{SigH} = 196.74 \leq 1.5 \cdot \text{MIN}(f; f_H) = 308.59 [\text{N/mm}^2]$ (11.5-90)	63.7%	OK
Radial Stress $k \cdot \text{SigR} = 55.93 \leq f = 205.73 [\text{N/mm}^2]$ (11.5-91)	27.1%	OK
Tangential Stress $k \cdot \text{SigTeta} = 71.18 \leq f = 205.73 [\text{N/mm}^2]$ (11.5-92)	34.5%	OK
Radial+Hub Stress $0.5 \cdot k \cdot (\text{SigH} + \text{SigR}) = 126.33 \leq f = 205.73 [\text{N/mm}^2]$ (11.5-93)	61.4%	OK
Tangential+Hub Stress $0.5 \cdot k \cdot (\text{SigH} + \text{SigTeta}) = 133.96 \leq f = 205.73 [\text{N/mm}^2]$ (11.5-94)	65.1%	OK

**BOLTING UP CONDITION****11.5.4.1 Flange Stresses with Flange Thickness  $e = 11$  mm**

Longitudinal Hub Stress

$$\text{SigH} = \frac{\phi \cdot M}{(\lambda \cdot g_1 \cdot e^2)} \quad (11.5-32)$$

$$= 1.82 \cdot 8.37 / (1.39 \cdot 11^2) = 304.08 \text{ N/mm}^2$$

Radial Flange Stress

$$\text{SigR} = \frac{(1.333 \cdot e \cdot \text{BetaF} + l_0) \cdot M}{(\lambda \cdot e^2 \cdot l_0)} \quad (11.5-33)$$

$$= (1.333 \cdot 11 \cdot 0.8588 + 17.02) \cdot 8.37 / (1.39 \cdot 11^2 \cdot 17.02) = 86.45 \text{ N/mm}^2$$

Tangential Flange Stress

$$\text{SigTeta} = \frac{\text{BetaY} \cdot M}{e^2} - \text{SigR} \cdot \frac{(K^2 + 1)}{(K^2 - 1)} \quad (11.5-34)$$

$$= 4.654 \cdot 8.37 / 11^2 - 86.45 \cdot (1.54^2 + 1) / (1.54^2 - 1) = 110.02 \text{ N/mm}^2$$

**11.5.4.2 Stress Limits**

Hub Stress $k \cdot \text{SigH} = 304.08 \leq 1.5 \cdot \text{MIN}(f; f_H) = 318.75 [\text{N/mm}^2]$ (11.5-90)	95.3%	OK
Radial Stress $k \cdot \text{SigR} = 86.45 \leq f = 212.5 [\text{N/mm}^2]$ (11.5-91)	40.6%	OK
Tangential Stress $k \cdot \text{SigTeta} = 110.02 \leq f = 212.5 [\text{N/mm}^2]$ (11.5-92)	51.7%	OK
Radial+Hub Stress $0.5 \cdot k \cdot (\text{SigH} + \text{SigR}) = 195.26 \leq f = 212.5 [\text{N/mm}^2]$ (11.5-93)	91.8%	OK
Tangential+Hub Stress $0.5 \cdot k \cdot (\text{SigH} + \text{SigTeta}) = 207.05 \leq f = 212.5 [\text{N/mm}^2]$ (11.5-94)	97.4%	OK

**EN13445-5;10.2.3.3 REQUIRED MIN.HYDROSTATIC TEST PRESSURE:Ptmin**

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$$\text{Ptmin} = 1.25 \cdot \text{Pd} \cdot f_{20} / f = 1.25 \cdot 3.3 \cdot 212.5 / 205.73 = 4.2607 \text{ MPa}$$

$$\text{Ptmin} = 1.43 \cdot \text{Pd} = 1.43 \cdot 3.3 = 4.7190 \text{ MPa}$$

Test Pressure $\text{Ptmin} = 4.72 \leq \text{Ptmax} = 7.197 [\text{MPa}]$	65.5%	OK
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Warning: Invalid gasket location/dimension.

Volume:0.0001246 m3 Weight:0 kg (SG= 7.85 )



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